

ภาคผนวก จ

โปรแกรม MATLAB ที่ใช้ในการเก็บข้อมูลและคำนวณค่าต่างๆ


```
T11 = B(:,30); % Temp AIR Out. Heatpipe reheat
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T12= B(:,32); % Temp AIR Ent. Condensor
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T13 = B(:,34); % Temp AIR Out. Condensor
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```
T14= B(:,36); % Temp Water Condensate
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[illegible]

```
T15 = B(:,38); %Temp Surface Evaporator Heat pipe
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T16= B(:,40); %Temp Surface Evaporator Heat pipe
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T17 = B(:,42); %Temp Surface Adiabatic Heat pipe
```

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T18 = B(:,44); %Temp Surface Adiabatic Heat pipe
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```
T19 = B(:,46) ; %Temp Surface Condenser Heat pipe
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```
T20 = B(:,48); %Temp Surface Condenser Heat pipe
```

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T21 = B(:,50); %Temp Surface Adiabatic Heat pipe
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```
T22 = B(:,52); %Temp Surface Adiabatic Heat pipe
```

[illegible]

T1 = V2.*10-40 ; % Temp AIR Ent. Heatpipe

T2 = V4.*10-40 ; % TempAIR Leav. HP_reheat

T3 = V6.*10-40 ; % Temp AIR Ent. Condenser

T4 = V8.*10-40 ; % Temp AIR Leav. Condenser

[illegible]

RH1 = V3./10 ; %humidity AIR Ent. Heatpipe

RH2 = V5./10 ; %humidity AIR Leav. HP reheat

RH3 = V7./10 ; %humidity AIR Ent. Condenser

$$RH4 = V9./10 \quad ; \quad \% \text{humidity AIR Leav. Condenser}$$
[illegible]

Time= Ts/6;

%-----

%Area dust

A_1 = 0.3627; %m² Air inlet

A_2 = 0.3627 ; %m² Air outlet

%Hydraulic diamrter(Dh)

Dh_1 = 0.6020 ; %m

Dh_2 = 0.6020 ; %m

%Air velocity

Velo_1 = 2.15 ; %m/s Air inlet

Velo_2 = 2.15 ; %m/s Air outlet

%Volume Flow rate

Vflow_1 = Velo_1*A_1 ; %m³/s Air Flow inlet

Vflow_2 = Velo_2*A_2 ; %m³/s Air Flow outlet

%CFM

CFM_1 = 60*35.315*Vflow_1 ; %CFM Air inlet Flow

CFM_2 = 60*35.315*Vflow_2 ; %CFM Air outlet Flow

%Air density

rho_EntHeatpipe_precool = 4.481185-0.02113391*(T1+273.15)+0.0000437296*(T1+273.15).^2-
0.00000003252345*(T1+273.15).^3-0.00000000002356712*(T1+273.15).^4; %kg/m³

rho_OutHeatpipe_precool = 4.481185-0.02113391*(T9+273.15)+0.0000437296*(T9+273.15).^2-
0.00000003252345*(T9+273.15).^3-0.00000000002356712*(T9+273.15).^4; %kg/m³

rho_OutEvaporator = 4.481185-0.02113391*(T10+273.15)+0.0000437296*(T10+273.15).^2-
0.00000003252345*(T10+273.15).^3-0.00000000002356712*(T10+273.15).^4; %kg/m³

```

rho_OutHeatpipe_reheat = 4.481185-
0.02113391*(T11+273.15)+0.0000437296*(T11+273.15).^2-0.00000003252345*(T11+273.15).^3-
0.000000000002356712*(T11+273.15).^4; %kg/m^3

rho_EntCondenser = 4.481185-0.02113391*(T12+273.15)+0.0000437296*(T12+273.15).^2-
0.00000003252345*(T12+273.15).^3-0.000000000002356712*(T12+273.15).^4; %kg/m^3

rho_OutCondenser = 4.481185-0.02113391*(T13+273.15)+0.0000437296*(T13+273.15).^2-
0.00000003252345*(T13+273.15).^3-0.000000000002356712*(T13+273.15).^4; %kg/m^3

%Specific heat of Air
cp = 1.005; %kJ/kg.K

%Mass Flow rate
mass_flow_EntHeatpipe_precool = Vflow_1./rho_EntHeatpipe_precool ; %kg/s
mass_flow_OutHeatpipe_precool = Vflow_1./rho_OutHeatpipe_precool ; %kg/s
mass_flow_OutEvaporator = Vflow_2./rho_OutEvaporator ; %kg/s
mass_flow_OutHeatpipe_reheat = Vflow_2./rho_OutHeatpipe_reheat ; %kg/s
mass_flow_EntCondenser = Vflow_2./rho_EntCondenser ; %kg/s
mass_flow_OutCondenser = Vflow_2./rho_OutCondenser ; %kg/s

mass_av =
(mass_flow_EntHeatpipe_precool+mass_flow_OutHeatpipe_precool+mass_flow_OutEvaporator+
mass_flow_OutHeatpipe_reheat+mass_flow_EntCondenser+mass_flow_OutCondenser)./6 ;

%Pressure of dry air (Pg)
Pg1 = 0.0000009631.*T1.^4 -0.0000334367.*T1.^3 +0.0036110043.*T1.^2 +0.0161351776.*T1
+0.6731881560 ; %kPa
Pg9 = 0.0000009631.*T9.^4 -0.0000334367.*T9.^3 +0.0036110043.*T9.^2 +0.0161351776.*T9
+0.6731881560 ; %kPa
Pg10 = 0.0000009631.*T10.^4 -0.0000334367.*T10.^3 +0.0036110043.*T10.^2
+0.0161351776.*T10 +0.6731881560 ; %kPa
Pg11 = 0.0000009631.*T11.^4 -0.0000334367.*T11.^3 +0.0036110043.*T11.^2
+0.0161351776.*T11 +0.6731881560 ; %kPa

```

$$Pg12 = 0.0000009631 \cdot T12.^4 - 0.0000334367 \cdot T12.^3 + 0.0036110043 \cdot T12.^2 + 0.0161351776 \cdot T12 + 0.6731881560 ; \%kPa$$

$$Pg13 = 0.0000009631 \cdot T13.^4 - 0.0000334367 \cdot T13.^3 + 0.0036110043 \cdot T13.^2 + 0.0161351776 \cdot T13 + 0.6731881560 ; \%kPa$$

%-----

%Differant Air Temperature

$$DT_preheat = (T1 - T9);$$

$$DT_eva = (T9 - T10);$$

$$DT_reheat = (T10 - T11);$$

$$DT_cond = (T12 - T13);$$

%Humidity

$$w1 = (0.622 \cdot RH1 \cdot Pg1) / (101.325 - RH1 \cdot Pg1) ; \%kg \text{ water vapor/kg dry air}$$

$$w2 = (0.622 \cdot RH2 \cdot Pg11) / (101.325 - RH2 \cdot Pg11) ; \%kg \text{ water vapor/kg dry air}$$

$$w3 = (0.622 \cdot RH3 \cdot Pg12) / (101.325 - RH3 \cdot Pg12) ; \%kg \text{ water vapor/kg dry air}$$

$$RH9 = (w1 \cdot 101.325) / (Pg9 \cdot (0.622 + w1)) ; \%RH$$

$$RH10 = (w2 \cdot 101.325) / (Pg10 \cdot (0.622 + w2)) ; \%RH$$

$$RH13 = (w3 \cdot 101.325) / (Pg13 \cdot (0.622 + w3)) ; \%RH$$

$$w4 = (0.622 \cdot RH13 \cdot Pg13) / (101.325 - RH13 \cdot Pg13) + 0.0003 ; \%kg \text{ water vapor/kg dry air}$$

%h from air

$$h1 = 1.005 \cdot T1 + (w1 \cdot (2501 + 1.805 \cdot T1)) ; \%kJ/kg$$

$$h2 = 1.005 \cdot T9 + (w1 \cdot (2501 + 1.805 \cdot T9)) ; \%kJ/kg$$

$$h3 = 1.005 \cdot T10 + (w2 \cdot (2501 + 1.805 \cdot T10)) ; \%kJ/kg$$

$$h4 = 1.005 \cdot T11 + (w2 \cdot (2501 + 1.805 \cdot T11)) ; \%kJ/kg$$

$$h5 = 1.009 \cdot T12 + (w3 \cdot (2501 + 1.805 \cdot T12)) ; \%kJ/kg$$

$$h6 = 1.009 \cdot T13 + (w4 \cdot (2501 + 1.805 \cdot T13)) ; \%kJ/kg$$

```

% heat form h
Q_1 = mass_flow_EntHeatpipe_precool.*(h1-h2) ; %kW
Q_2 = mass_flow_OutHeatpipe_precool.*(h4-h3) ; %kW
Q_3 = mass_flow_EntCondenser.*(h2-h3) ; %kW
Q_4 = mass_flow_OutCondenser.*(h6-h5) ; %kW

%-----

%Graph
subplot(3,3,1)
plot(Time,T1,'--b',Time,T9,'--c',Time,T10,'--g',Time,T11,'--r',Time,T12,'--y',Time,T13,'--m')
h=legend('in evahp','in eva','out eva','out conhp','in con','out con',1);
title('Temperature Air at section');
xlabel('min')
ylabel('Temperature (^oC)')
grid on

subplot(3,3,2)
plot(Time,RH1.*100,Time,RH9.*100,'--y',Time,RH10.*100,'--b',Time,RH2.*100,'--m',Time,RH3.*100,'--r',Time,RH13.*100,'--k')
h=legend('in evahp','in eva','out eva','out conhp','in con','out con');
title('Relative Humidity at section');
xlabel('min')
ylabel('%')
grid on

subplot(3,3,3)
plot(Time,T5,'--r',Time,T6,'--b',Time,T7,'--m',Time,T8,'--c')
h=legend('in eva','out eva','in cond','out cond',1);
title('Temperature surface coil');
xlabel('min')
ylabel('Temperature (^oC)')
grid on

```

```

subplot(3,3,4)
plot(Time,T15,'--b',Time,T16,'--m',Time,T17,'--r',Time,T18,'--k',Time,T19,'--g',Time,T20,'--
c',Time,T21,'--k',Time,T22,'--r')
h=legend('eva1','eva2','adia1','adia2','con1','con2','adia3','adia4',1);
title('Temp distribution of Heat pipe');
xlabel('min')
ylabel('Temperature (^oC)')
grid on

```

```

subplot(3,3,5)
plot(Time,Q_1,'--r',Time,Q_2,'--g',Time,Q_3,'--m',Time,Q_4,'--b')
h=legend('pre heatpipe','re heatpipe','eva','cond',1);
title('Heat Air distribution(cal from h ) ');
xlabel('min')
ylabel('kW')
grid on

```

```

subplot(3,3,6)
plot(Time,DT_preheat,'--m',Time,DT_eva,'--b',Time,DT_reheat,'--r',Time,DT_cond,'--g')
h=legend('DT preheat','DT eva','DT reheat','DT cond',1);
title(' Air Temperature different');
xlabel('min')
ylabel('Temperature different (^oC)')
grid on

```

```

subplot(3,3,7)
plot(Time,w1.*1000,'--m',Time,w2.*1000,'--b',Time,w3.*1000,'--g',Time,w4.*1000,'r')
h=legend('1','2','3','4',1);
title(' humidity');
xlabel('min')

```

```
ylabel('g water vapor/kg dry air')  
grid on  
  
subplot(3,3,8)  
plot(Time,T1-T2,'--m')  
h=legend('DT heatpipe eva-cond',1);  
title(' ^oC');  
xlabel('min')  
ylabel('')  
grid on  
pause (10)  
  
subplot(3,3,9)  
plot(Time,T14,'--m')  
h=legend('Temp Water',1);  
title(' ^oC');  
xlabel('min')  
ylabel('')  
grid on  
pause (10)  
  
end
```