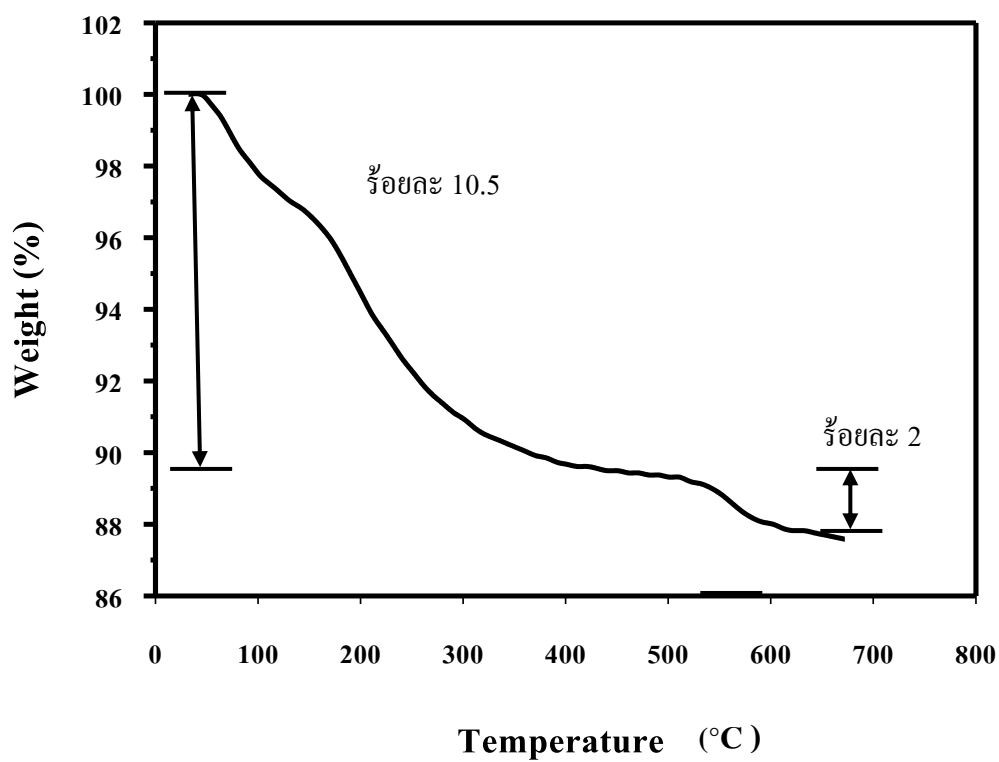


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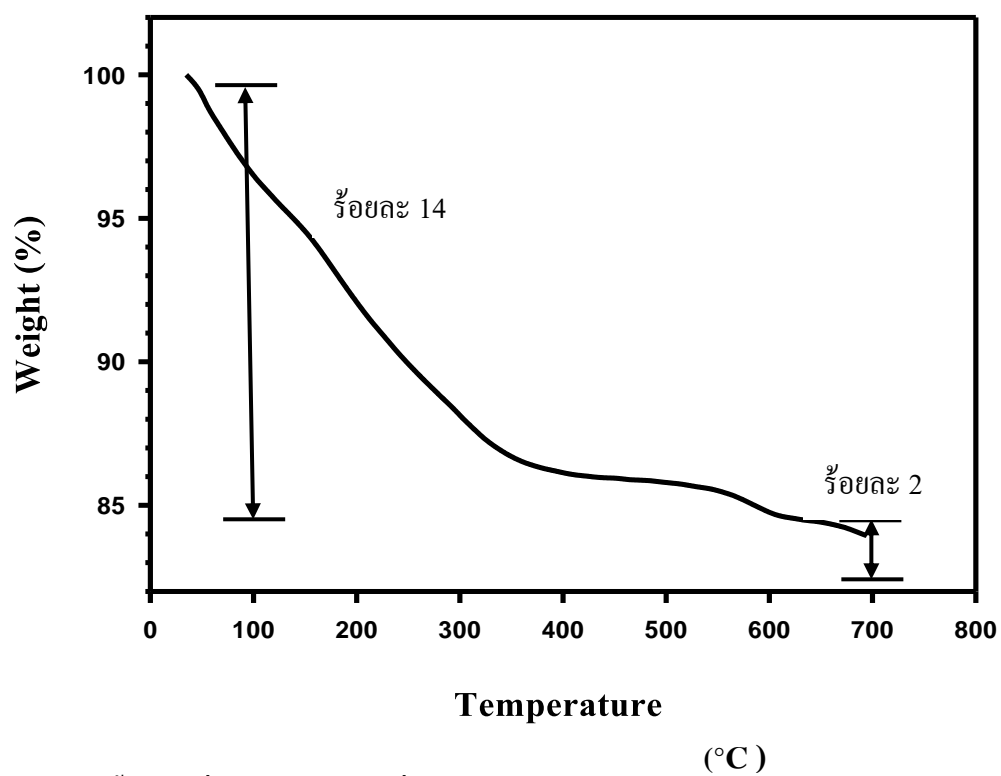
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ข้อมูลการทดลอง

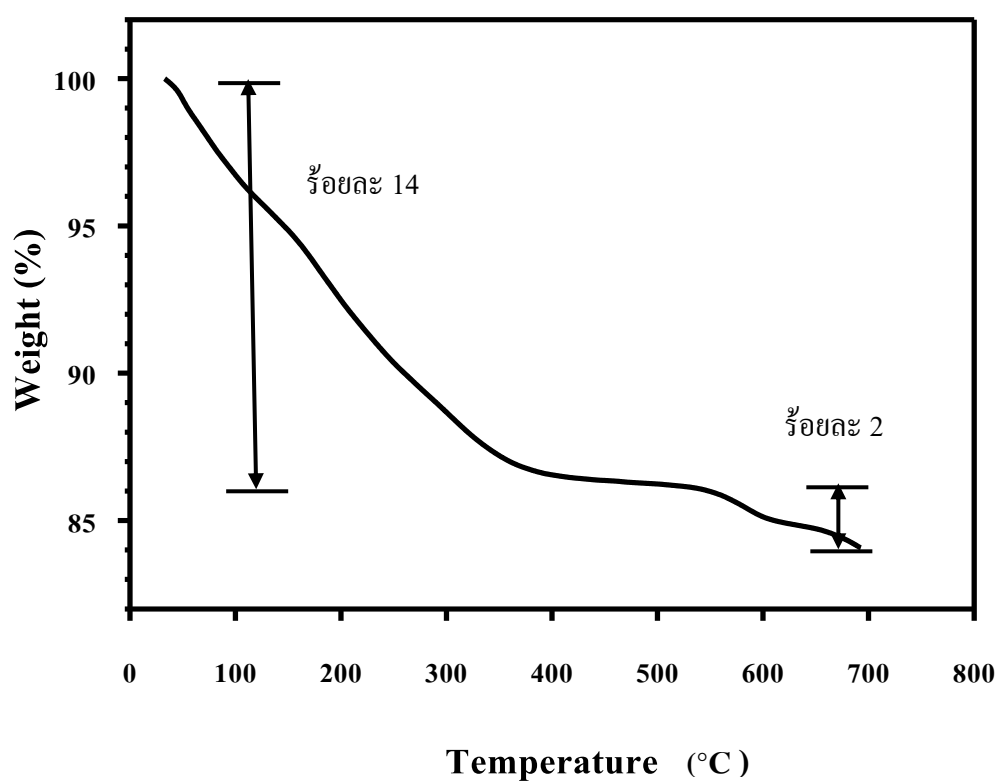
1. ผลการวิเคราะห์การดูดซับสารที่ผิวของตัวเร่งปฏิกิริยา โดยใช้เครื่อง TGA (Thermal gravimetric analysis)



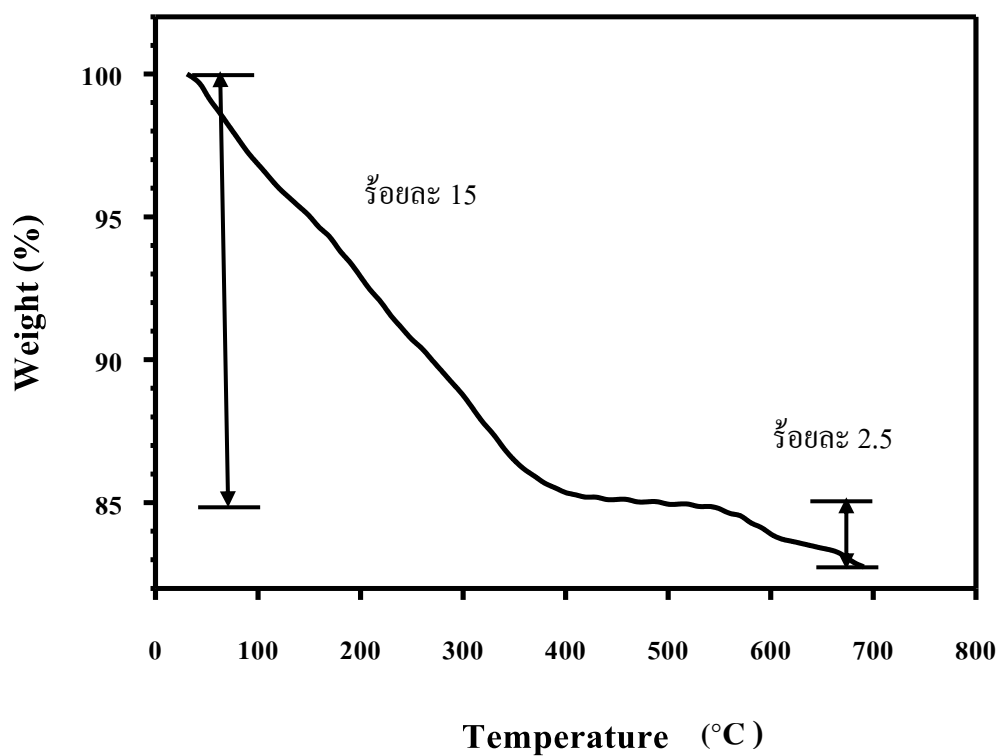
ภาพที่ 29 ปริมาณน้ำหนักที่หายไปของสารที่ผิวตัวเร่งปฏิกิริยา Fe-Ce-Zn (Fresh)



ภาพที่ 30 ปริมาณน้ำหนักที่หายไปของสารที่ผิวตัวเร่งปฏิกิริยา Fe-Ce-Zn ช่วง 5 นาทีแรกของปฏิกิริยาการดูดซับของตัวเร่งปฏิกิริยา



ภาพที่ 31 ปริมาณน้ำหนักที่หายไปของสารที่ผิวตัวเร่งปฏิกิริยา Fe-Ce-Zn ช่วง 5 นาทีแรกของการทำปฏิกิริยาโฟโตเฟนตอน



ภาพที่ 32 ปริมาณน้ำหนักที่หายไปของสารที่ผิวตัวเร่งปฏิกิริยา Fe-Ce-Zn ช่วงเริ่มต้นปฏิกิริยาจนกระทั่งสิ้นสุดปฏิกิริยา 120 นาที ของการทำปฏิกิริยาโฟโตเฟนตอน

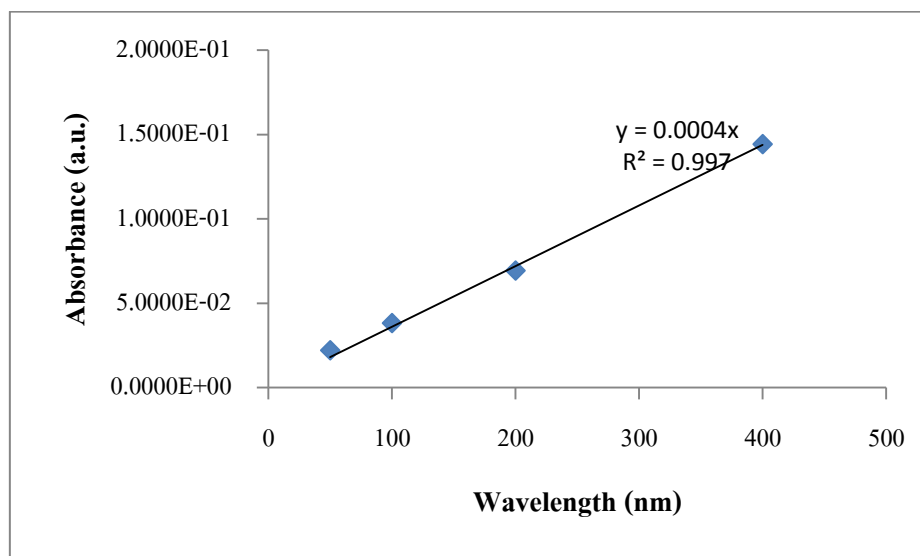
ภาคผนวก ข

ตัวอย่างการคำนวณ

## 1. วิเคราะห์ประสิทธิภาพในการลดค่า COD

$$\text{ร้อยละการสลาย COD} = \frac{\text{COD เริ่มต้น} - \text{COD ณ เวลานั้นๆ}}{\text{COD เริ่มต้น}}$$

## 2. ทำกราฟมาตรฐาน (Standard or Calibration Curve) และหาค่า COD ของตัวอย่างจากกราฟมาตรฐาน



ภาพที่ 33 กราฟมาตรฐานในการหาค่า COD



ภาคผนวก ก

การเผยแพร่ผลงานวิทยานิพนธ์



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ICEAS 1397

**Treatment of wastewater from pulp processing using UV/Fe-Ce/H<sub>2</sub>O<sub>2</sub>**

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**ABSTRACT**

Treatment of wastewater from pulp processing by photo-Fenton reaction over Fe-Ce bimetal catalysts is used to decompose the contaminants in waste water such as Lignin which is difficult to treat. The purpose of this research is to remove COD and colour in wastewater from pulping process. The reactions were carried out in batch reactor for 120 minutes under UV lights. The effects of some operating parameters such as catalyst concentrations in the range of 50-600 ppm, hydrogen peroxide concentrations in the range of 1000-15000 ppm, and the pH range were investigated. It has been found that 66.67% of COD has been removed in 5 min by using Fe-Ce bimetal catalyst and H<sub>2</sub>O<sub>2</sub> concentrations of 450 ppm and 10000 ppm, respectively.

Key Words : Decolourization, wastewater treatment, lignin removal, photo-Fenton

**1.Introduction**

Effluents from the pulping process contain a large number of toxic compounds and may also be harmful to environments if it is discharged into receiving waters directly [1]. The release of pulping process into natural waters can cause necessary environmental problems, for example: colour and toxic problems. The problem of lignin is a strong colour in the effluent and it is very difficult to decompose by biomass. Nowadays, the contaminants in pulping process effluents are non-biodegradable. Thus, the conventional biological treatment processes are not adequate for treatment.

Advanced oxidation processes (AOPs) have been successful in decomposing organic compounds in wastewater. The composition of UV radiation and H<sub>2</sub>O<sub>2</sub> with Fe (II) or Fe (III), that called photo-Fenton system, is the promising process based on this concept, where iron salts serve as photocatalysis and H<sub>2</sub>O<sub>2</sub> as oxidizing agent, the hydroxyl radicals must be generated by photochemical reactions. It is a good combination of oxidation and photochemical reaction for wastewater treatment [2]. The presence of Fe ions may cause some problem in the effluent. Thus the solid catalyst such as Fe-Ce bimetal catalyst becomes interesting to use as the catalyst in this treatment.

The objective of this study is to investigate the performance of advanced oxidation methods and their combinations for COD and colour removals from pulping process effluent. UV/Fe-Ce/H<sub>2</sub>O<sub>2</sub> treatment was employed at different operating parameter of pH (3-11), Fe-Ce bimetal doses (50-600 ppm) and H<sub>2</sub>O<sub>2</sub> doses (1000-15000 ppm) for the

treating pulp and paper wastewater.

## 2. Research Methodology

### 2.1 Catalyst preparation and Characterizations

The Fe-Ce bimetal catalyst was prepared by co-precipitation method [3]. The combination of 0.08 mol/L  $\text{Ce}(\text{SO}_4)_2 \cdot 4\text{H}_2\text{O}$ , 0.2 mol/L  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  and 0.1 mol/L  $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$  were dissolved mixing in water of 2 L, then gentle stirring, the pH was raised to around 10, 6 mol/L NaOH solution added to adjust. Continue stirring 30 min until the pH at 10. After 10 h of aging at room temperature, the suspension was washed with distilled water and finally dried at 100 °C for 10 h. Fe-Ce oxide hydrate catalyst used in the experiment. Catalysts characterization was carried out by BET and XRD in order to observe surface area and material structure, respectively.

### 2.2 Photo-reactor and analytical methods

The reactions were carried out in batch photo-reactor. The photo-reactor was equipped with two UV lamps. 500 ml of real wastewater was added to a 1 L reactor. The desired amount of Fe-Ce catalyst, hydrogen peroxide and pH adjusting agent were added into the reactor. The mixture was continuous stirring with constant rate. The samples were sampling along the reaction. The COD concentrations of all samples were analyzed by closed reflux method.

## 3. Results and discussion

### 3.1 Effects of initial $\text{H}_2\text{O}_2$ dose

A set of the experiments were carried out with variable  $\text{H}_2\text{O}_2$  concentrations between 1000 and 15000 ppm and Fe-Ce bimetal concentration was kept constant of 450 ppm in the presence of UV light. Fig. 1 describes variation of COD removals with the  $\text{H}_2\text{O}_2$  concentration. Percentage of COD removal slightly decreased with  $\text{H}_2\text{O}_2$  concentration up to 10000 ppm due to the excess of  $\text{H}_2\text{O}_2$  may react with iron ion. Maximum COD removal efficiency (66.67%) obtained with the addition of 10000 ppm and 450 ppm of Fe-Ce catalyst.

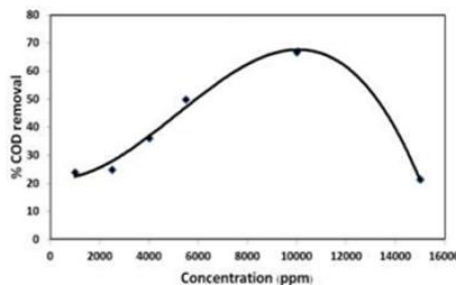


Fig.1. Variations of percent COD removals with initial  $\text{H}_2\text{O}_2$  concentration in UV/ $\text{H}_2\text{O}_2$ /Fe-Ce treatment at 450 ppm Fe-Ce catalysts, at 5 min.

### 3.2 Effect of initial Fe-Ce bimetal dose

A set of experiments with UV/H<sub>2</sub>O<sub>2</sub>/Fe-Ce were carried out with variable Fe-Ce bimetal concentration. Fig. 2 describes variation of COD removals with the Fe-Ce catalysts dose at a constant initial H<sub>2</sub>O<sub>2</sub> of 10000 ppm and Fe-Ce doses of between 50-600 ppm for 120 min. After addition of Fe-Ce bimetal catalysts and turning on the UV lamp, a fast decrease in COD was observed within 5 min. Percentage of COD removals increased with Fe-Ce bimetal concentration up to 450 ppm due to the excess of catalyst. Thus, it was non-energetic hydroxyl radicals in the decomposition of organic matter.

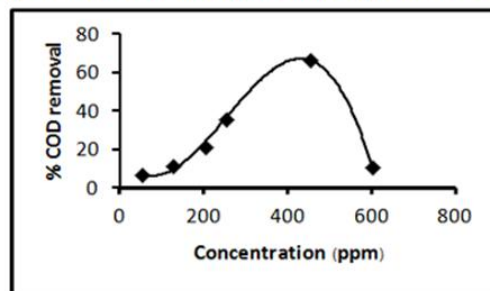


Fig.1. Variations of percent COD removals with initial Fe-Ce bimetal concentration in UV/H<sub>2</sub>O<sub>2</sub>/Fe-Ce treatment at 10000 ppm H<sub>2</sub>O<sub>2</sub> catalysts, at 5 min.

#### 4. Conclusions

COD and colour removals from a pulp and paper mill effluent were investigated by using UV/Fe-Ce/H<sub>2</sub>O<sub>2</sub> processes. The effect of the amount of the initial hydrogen peroxide and Fe-Ce catalysts concentrations on the treatment processes were investigated and the best suitable operating conditions were determined.

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