

Piriya Itsariwan 2014: Mass Transfer Correlation in a Reactor for H<sub>2</sub>S Removal and Degradation of Iron EDTA Complex Solution. Master of Engineering (Chemical Engineering), Major Field: Chemical Engineering, Department of Chemical Engineering. Thesis Advisor: Associate Professor Sunun Limtrakul, D.Sc. 122 pages.

The H<sub>2</sub>S removal process via iron chelate solution consists of two steps; the removal reaction step in the riser and the solvent regeneration reaction step in the downcomer. An auto-circulating reactor is appropriate for H<sub>2</sub>S removal due to the advantage of combining the two reaction step in a single reactor. Reactor analysis and design require kinetic and mass transfer information. The intrinsic kinetics were obtained from experimental data in a stirred cell type of reactor. The intrinsic kinetic rates are  $-r_1 = 16.70C_{H_2S}C_{Fe^{3+}}$  and  $-r_2 = 0.166C_{O_2}C_{Fe^{2+}}^2$  for removal and regeneration reactions, respectively, in S.I. units. These data were then used to measure the interfacial areas and the mass transfer coefficients of the liquid phase in an auto-circulating reactor for both removal (riser) and regeneration (downer) conditions. The correlations of interfacial areas in the riser and downcomer are  $a_{rs}D_{rs} = 0.02 Re_{rs}^{0.99} Re_{dn}^{0.03}$  and  $a_{dn}D_{dn} = 0.11 Re_{rs}^{0.03} Re_{dn}^{0.65}$ , respectively. Furthermore the correlations of the liquid phase mass transfer coefficients of H<sub>2</sub>S in the riser and O<sub>2</sub> in the downcomer are  $Sh_{rs} = 3.49 Re_{rs}^{1.01} Re_{dn}^{0.08}$  and  $Sh_{dn} = 5.07 Re_{rs}^{0.11} Re_{dn}^{0.81}$ , respectively. The data and the correlations reported here would be useful for design and scale-up of this type of reactor. Moreover, the effect of types of buffer solution on the degradation of Fe-EDTA solution was investigated. The results show that Fe-EDTA complex solution is partially degraded to  $\mu$ -oxo dimer, [Fe(III)-EDTA-O-Fe(III)-EDTA]<sup>4-</sup> and other Fe-EDTA complex such as Fe(III)-NTA, Fe(III)-ED3A and Fe(III)-IDA in the removal and regeneration steps. The degradation of Fe-EDTA solution in the system using sodium citrate as a buffer solution is minimum comparing to using tris-(hydroxymethyl) aminomethane, and sodium hydroxide.

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Thesis Advisor's signature