



**PREPARATION METHOD AND CHARACTERIZATION OF Au MODIFIED  
TiO<sub>2</sub> FOR PHOTOCATALYTIC H<sub>2</sub> PRODUCTION WITH SIMULATED  
SOLAR ENERGY**

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วิธีการเตรียมและคุณลักษณะของไททานเนียมไดออกไซด์ที่ดัดแปลงด้วยทองสำหรับการผลิต  
ไฮโดรเจนด้วยกระบวนการเร่งปฏิกิริยาด้วยแสงโดยใช้พลังงานแสงอาทิตย์จำลอง

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Photocatalytic H<sub>2</sub> production over TiO<sub>2</sub> prepared by solvothermal, sol-gel, and flame spray pyrolysis methods with Au modification were tested under simulated solar light irradiation. Due to the most suitable balance among these properties: nanocrystallite size, crystallinity, specific surface area, pore size and pore size distribution in mesoporous range, of the TiO<sub>2</sub> prepared by solvothermal method, it exhibited the highest photocatalytic H<sub>2</sub> production efficiency as compared to the TiO<sub>2</sub> prepared by the other methods and the commercial TiO<sub>2</sub> (Degussa P-25). Moreover, the prepared parameters of the solvothermal method: solvent type, solvothermal temperature, Ti concentration and calcination temperature significantly affected the properties of TiO<sub>2</sub> based photocatalyst. In addition, Au cocatalyst modified method affected photocatalytic H<sub>2</sub> production. Photodeposition and doping methods provided the Au modified TiO<sub>2</sub> with the same photocatalytic activity. The best Au modified TiO<sub>2</sub> exhibited the H<sub>2</sub> production rate of 13,786 μmol.h<sup>-1</sup>. g<sub>cat</sub><sup>-1</sup>.

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53404207 : สาขาวิชาวิศวกรรมเคมี

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น้ำหนักตัวเร่งปฏิกิริยา

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## TABLE OF CONTENTS

		Page
English Abstract.....		d
Thai Abstract.....		e
Acknowledgments.....		f
List of Tables .....		i
List of figures .....		j
Chapter		
1	Introduction .....	1
	Objective of the research .....	3
	Scope of the research .....	3
2	Literature reviews .....	5
	TiO <sub>2</sub> preparation by solvothermal method.....	5
	TiO <sub>2</sub> preparation by flame spray pyrolysis method.....	7
	Using Au cocatalyst in photocatalytic H <sub>2</sub> production .....	9
	Metal cocatalyst photodeposition .....	12
	Metal cocatalyst doping.....	14
3	Theory .....	16
	Basic principle of photocatalytic H <sub>2</sub> production.....	16
	Evaluation of photocatalytic H <sub>2</sub> production .....	19
	Techniques to enhance photocatalytic H <sub>2</sub> production .....	21
	Crystal structure and properties of TiO <sub>2</sub> .....	23
	Flame spray pyrolysis .....	28
	Solvothermal method.....	32
4	Experiments .....	36
	Chemicals .....	36
	TiO <sub>2</sub> based photocatalyst preparation.....	37
	Preparation by sol gel method .....	37
	Preparation by solvothermal method .....	38
	Preparation by flame spray pyrolysis method.....	41

Chapter		Page
4	Au cocatalyst modification	41
	Modification by impregnation .....	41
	Modification by photodeposition .....	41
	Modification by doping .....	42
	Photocatalyst characterization .....	43
	X-ray diffraction (XRD) .....	43
	N <sub>2</sub> physisorption .....	43
	Transmission electron microscopy (TEM) .....	44
	Inductively coupled plasma (ICP) .....	44
	UV-vis diffuse reflectance spectra (UV-vis DRS) .....	44
	H <sub>2</sub> chemisorption .....	45
	Photoluminescence spectroscopy .....	45
	Photocatalytic H <sub>2</sub> production testing .....	46
5	Results and Discussion.....	48
	Photocatalyst characterization .....	48
	Effect of TiO <sub>2</sub> preparation method .....	48
	Effect of solvent type in TiO <sub>2</sub> preparation by solvothermal.....	55
	Effect of temperature in TiO <sub>2</sub> preparation by solvothermal.....	60
	Effect of Ti concentration in TiO <sub>2</sub> preparation by solvothermal	65
	Effect of calcined temperature.....	68
	Effect of Au modified TiO <sub>2</sub> method .....	71
	Photocatalytic H <sub>2</sub> production.....	77
	Effect of TiO <sub>2</sub> preparation method .....	77
	Effect of solvent type in TiO <sub>2</sub> preparation by solvothermal.....	78
	Effect of temperature in TiO <sub>2</sub> preparation by solvothermal .....	79
	Effect of Ti concentration in TiO <sub>2</sub> preparation by solvothermal	80
	Effect of calcined temperature.....	81
	Effect of Au modified TiO <sub>2</sub> method .....	82
6	Conclusions and Recommendations.....	84

Chapter	Page
Bibliography .....	85
Appendix.....	94
Appexdix A Calculation for Photocatalyst preparation.....	95
Appexdix B Calculation of the crystallite size .....	98
Appexdix C Calculation for total H <sub>2</sub> chemisorption and dispersion	101
Appexdix D Calculation of H <sub>2</sub> production rate .....	103
Appexdix E International proceeding .....	105
Biography.....	107

## LIST OF TABLES

Table	Page
2.1 TiO <sub>2</sub> particles synthesis by solvothermal method .....	6
2.2 TiO <sub>2</sub> particles synthesis by flame spray pyrolysis method .....	9
2.3 Band gap and cut-off wavelength absorption of Au/TiO <sub>2</sub> photocatalyst .....	11
3.1 Some bulk properties of the three main polymorphs of TiO <sub>2</sub> (anatase, rutile, and brookite) .....	25
4.1 The details of chemicals used in the photocatalyst preparation .....	36
4.2 The Condition of studied parameter in TiO <sub>2</sub> prepared by solvothermal ....	40
4.3 The operating conditions of TCD gas chromatograph for the photocatalytic H <sub>2</sub> production testing .....	45
5.1 Physical properties of TiO <sub>2</sub> prepared by SG, ST and FSP .....	49
5.2 Physical properties of TiO <sub>2</sub> prepared by ST with different solvent .....	57
5.3 Physical properties of TiO <sub>2</sub> prepared by ST with different solvothermal temperature .....	62
5.4 Physical properties of TiO <sub>2</sub> prepared by ST with different Ti concentration .....	66
5.5 Physical properties of TiO <sub>2</sub> prepared by ST with different calcined temperature.....	69
5.6 Physical properties of Au modified TiO <sub>2</sub> by IMP, PD and DP .....	72
A.1 Chemical Properties .....	96

## LIST OF FIGURES

Figures	Page
2.1 Mechanism for the generation and growth of TiO <sub>2</sub> nanoparticles in the FSP .....	8
2.2 Mechanism of the photocatalytic activity of Au/TiO <sub>2</sub> .....	11
2.3 Light absorption properties of Au/TiO <sub>2</sub> photocatalysts .....	12
2.4 TEM image of Ag particles (a) and Au particles (b) on TiO <sub>2</sub> by photodeposition method .....	13
2.5 TEM image of the 1wt.% Au-loaded mesoporous SrTiO <sub>3</sub> photocatalyst.....	15
3.1 The principle of photocatalytic H <sub>2</sub> production in the presence of electron donor reagent .....	17
3.2 Schematic diagram of photocatalytic H <sub>2</sub> production in the presence of reducing .....	18
3.3 Schematic diagram of photocatalyst surface modification by the addition of cocatalyst .....	21
3.4 Crystalline structure of: (A) anatase, (B) brookite and (C) rutile .....	24
3.5 Schematic diagram showing the potentials for various redox processes occurring on the TiO <sub>2</sub> surface at pH 7 .....	28
3.6 Comparison of conventional wet-phase and flame methods for the synthesis of Pt/Al <sub>2</sub> O <sub>3</sub> catalyst .....	30
3.7 Schematic of configurations used for the synthesis of catalysts by FSP ....	30
3.8 The formation of different particle configurations via the gas-to-particle mechanism for single and multi-component systems in FSP process	31
3.9 Schematic of the main parameters influencing properties of flame synthesized materials .....	32
3.10 Main factors governing solvothermal processes .....	33
3.11 Expected mechanism for the synthesis of particles using the solvothermal method .....	35
4.1 Schematic of the TiO <sub>2</sub> based photocatalyst synthesis procedure by sol-gel method .....	38

Figures	Page
4.2 Schematic of the TiO <sub>2</sub> based photocatalyst synthesis procedure by solvothermal method .....	39
4.3 Autoclave used to synthesis TiO <sub>2</sub> .....	40
4.4 Schematic of synthesis procedure of Au photodeposition over TiO <sub>2</sub> .....	42
4.5 The photocatalytic hydrogen production system used in this study .....	46
5.1 XRD pattern of TiO <sub>2</sub> based photocatalysts prepared by flame spray pyrolysis (FSP), sol-gel (SG) and solvothermal (ST) .....	48
5.2 TEM image of TiO <sub>2</sub> preparation by SG .....	50
5.3 TEM image of TiO <sub>2</sub> preparation by ST .....	51
5.4 TEM image of TiO <sub>2</sub> preparation by FSP .....	51
5.5 N <sub>2</sub> adsorption/desorption isotherms of TiO <sub>2</sub> preparation by SG, ST and FSP .....	53
5.6 Pore size distributions of TiO <sub>2</sub> preparation by SG, ST and FSP .....	54
5.7 XRD pattern of TiO <sub>2</sub> based photocatalysts prepared by ST with using different solvent .....	55
5.8 N <sub>2</sub> adsorption/desorption isotherms of TiO <sub>2</sub> preparation by ST with using –OH compound solvent .....	58
5.9 N <sub>2</sub> adsorption/desorption isotherms of TiO <sub>2</sub> preparation by ST with using without –OH compound solvent .....	58
5.10 Pore size distributions of TiO <sub>2</sub> preparation by ST with using –OH compound solvent .....	59
5.11 Pore size distributions of TiO <sub>2</sub> preparation by ST with using without –OH compound solvent .....	59
5.12 XRD patterns of TiO <sub>2</sub> based photocatalysts prepared by ST at 250 °C and 300 °C in CHX (a), HT (b) and TE (c) solvent .....	60
5.13 N <sub>2</sub> adsorption/desorption isotherms (a) and pore size distribution (b) of TiO <sub>2</sub> prepared by ST in CHX at 250 and 300 °C .....	63
5.14 N <sub>2</sub> adsorption/desorption isotherms (a) and pore size distribution (b) of TiO <sub>2</sub> prepared by ST in HT at 250 and 300 °C .....	64

Figures	Page
5.15	N <sub>2</sub> adsorption/desorption isotherms (a) and pore size distribution (b) of TiO <sub>2</sub> prepared by ST in TE at 250 and 300 °C ..... 64
5.16	XRD patterns of TiO <sub>2</sub> based photocatalysts prepared by ST with different TIPT concentration ..... 65
5.17	N <sub>2</sub> adsorption/desorption isotherms of TiO <sub>2</sub> prepared by ST in HT with different amount of TIPT ..... 67
5.18	Pore size distribution of TiO <sub>2</sub> prepared by ST in HT with different amount of TIPT ..... 67
5.19	XRD patterns of TiO <sub>2</sub> based photocatalysts prepared by ST with different calcined temperature ..... 68
5.20	N <sub>2</sub> adsorption/desorption isotherms of TiO <sub>2</sub> prepared by ST in HT with different calcined temperature ..... 70
5.21	Pore size distribution of TiO <sub>2</sub> prepared by ST in HT with different calcined temperature ..... 70
5.22	XRD patterns of Au modified TiO <sub>2</sub> by PD, DP and IMP..... 71
5.23	N <sub>2</sub> adsorption/desorption isotherms of Au modified TiO <sub>2</sub> by IMP, PD and DP ..... 73
5.24	Pore size distribution of Au modified TiO <sub>2</sub> by IMP, PD and DP ..... 73
5.25	UV-vis DRS of Au modified TiO <sub>2</sub> by IMP, PD and DP ..... 75
5.26	The PL emission spectra of Au modified TiO <sub>2</sub> by IMP, PD and DP..... 76
5.27	Effect of preparation method of TiO <sub>2</sub> particles on photocatalytic H <sub>2</sub> production rate..... 77
5.28	Effect of solvent type of TiO <sub>2</sub> preparation by ST on photocatalytic H <sub>2</sub> production rate..... 78
5.29	Effect of temperature in TiO <sub>2</sub> preparation by ST on photocatalytic H <sub>2</sub> production rate..... 80
5.30	Effect of TIPT concentration TiO <sub>2</sub> preparation by ST on photocatalytic H <sub>2</sub> production rate..... 81
5.31	Effect of calcined temperature on photocatalytic H <sub>2</sub> production rate..... 82
5.32	Effect of Au modified method on photocatalytic H <sub>2</sub> production rate..... 83

Figures		Page
B.1	Derivation of Bragg's Law for X-ray diffraction .....	99
B.2	The determining of the FWHM value of XRD line broadening .....	100
D.1	Calibration curve of amount of H <sub>2</sub> .....	104

## CHAPTER 1

### INTRODUCTION

Photocatalytic H<sub>2</sub> production from organic wastes reforming using colloidal semiconductors under sun light irradiation has received much attention because this technology can be not only the direct H<sub>2</sub> production but also the solution of environmental problem reduction. If the large scale hydrogen production from this technology is successfully achieved, the world will benefit from this hydrogen in the terms of energy and superior environment [1 - 8].

TiO<sub>2</sub> is an ideal based photocatalyst for photocatalytic H<sub>2</sub> production due to its suitable-potential level of the band structure, high chemical resistance, high photostability, non-toxicity and relatively low cost [9 - 14]. Particularly, nanoparticle is essential in the activity enhancement of the photocatalyst because it provides high surface area, low particle weight and fast charge-transference decreasing electron-hole recombination. Moreover, nanosize tends to increase the light-absorption, reduce the light-scattering, and well disperse in the liquid media [8, 15, 16]. Two recent methods to prepare nanoparticle are solvothermal [17 - 28] and flame spray pyrolysis methods [29 - 36] due to the good properties of the received nanoparticle as high specific surface area, high crystallinity and size homogeneity, which are considered as an important properties of the photocatalytic activity [5, 6, 27, 37]. However, different methods or different conditions can affect crystal structure, crystal defect, phase composition, surface morphology, surface chemical, etc. and hence photocatalytic activity [4, 6, 15]. So the first purpose of this work is to study the effect of preparation method on characteristic of TiO<sub>2</sub> to find out the suitable TiO<sub>2</sub> based photocatalyst for photocatalytic H<sub>2</sub> production. The studied method are solvothermal and flame spray pyrolysis methods comparing to sol-gel method, which is the most preparation technique for TiO<sub>2</sub> in the present.

The second purpose is due to the following mention. TiO<sub>2</sub> is well known that it has wide band gap about 3.2 eV [6], which only UV light can be utilized for H<sub>2</sub> production. Since the UV light only accounts for about 3% of solar radiation while the visible light contributes about 44% [4], the inability to utilize visible light of TiO<sub>2</sub>

limits the efficiency of the solar photocatalytic H<sub>2</sub> production over TiO<sub>2</sub> based photocatalyst. So far, modification of TiO<sub>2</sub> for visible-driven photocatalysts is limited and H<sub>2</sub> production rate is still low under visible light [38 - 58], which is not satisfactory for practical application. Hence, it is needed to develop TiO<sub>2</sub> photocatalysts that exhibited high photocatalytic activity under visible light.

Recently, the use of gold metal as cocatalyst is an effective way to reduce the band gap energy of the wide band gap photocatalysts [33, 34, 35, 59] as it shows a characteristic surface plasmon band in the visible region due to the collective excitation of electrons in the gold nanoparticles and it can strongly attach to the based photocatalyst surface [60, 61]. Moreover, it remarkably enhances photoactivity for H<sub>2</sub> production [62, 63], providing H<sub>2</sub> evolution sites of photocatalyst with decreasing the activation energy for gas evolution and extending for lifetime of excited electron-hole by its role is electron trap because of high electronegativity (EN) and high electron affinity (EA) [63]. Besides, it is a noble metal that does not undergo corrosion under photocatalytic conditions [64] and does not promote the backward reaction between H<sub>2</sub> and O<sub>2</sub> to produce water on the gold cocatalyst when compared to platinum cocatalyst [62]. The photodeposited gold metal onto the based photocatalyst surface [65 - 68] and gold doping [30, 33, 63, 69] are interesting in TiO<sub>2</sub> modification more than impregnation method since it provides highly uniform, well dispersion, small size of nanometal and strong interaction between metal and based photocatalyst, resulting in the photocatalytic activity enhancement. However, the different modification methods bring to different characteristic of cocatalyst metal that influence photocatalytic activity, such as electrochemical properties of cocatalyst, nanometal size, amount of H<sub>2</sub> active site, interaction between the activesite and H<sub>2</sub> molecule and interaction between cocatalyst metal and based photocatalyst [65, 67]. Thereby, the second purpose of this work is to investigate the suitable modification method of gold cocatalyst on TiO<sub>2</sub> based photocatalyst.

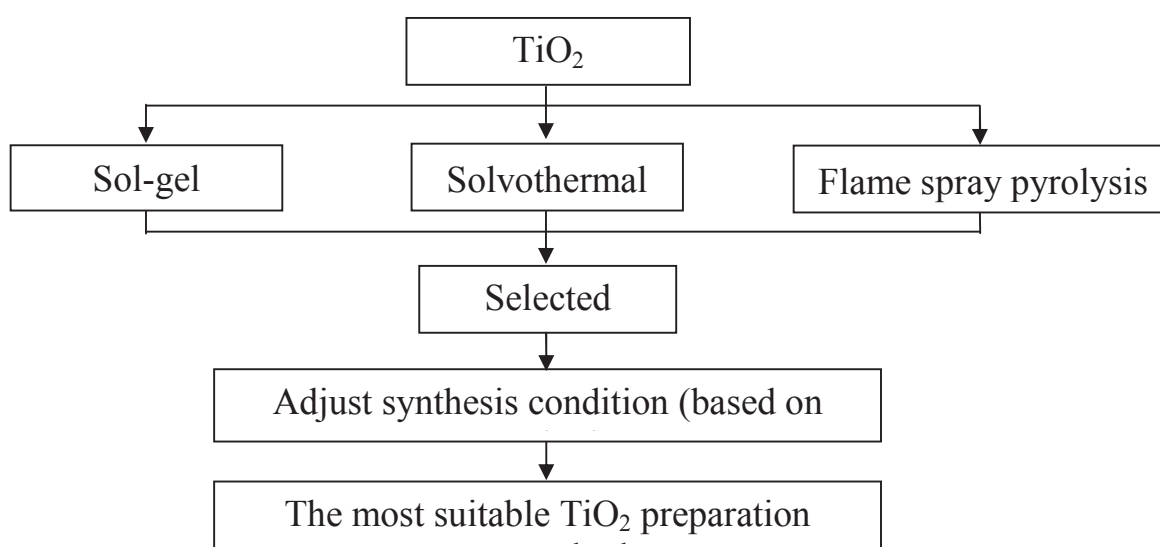
## Objectives of the Research

The purpose of this work are (1) to investigate the suitable preparation method for TiO<sub>2</sub> based photocatalysts that provided the good photocatalytic activity in H<sub>2</sub> production with simulated solar energy, and (2) to investigate the suitable Au cocatalyst modification method on TiO<sub>2</sub> base photocatalysts for photocatalytic activity enhancement.

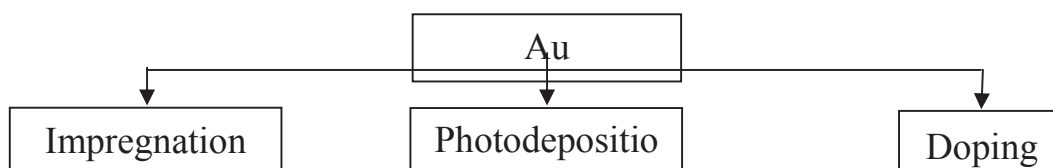
## Scope of the Research

### 1 Photocatalyst preparation

- Step 1, TiO<sub>2</sub> based photocatalyst is prepared by sol-gel, solvothermal and flame spray pyrolysis methods.



- Step 2, TiO<sub>2</sub> from step 1 is modified with Au cocatalyst by impregnation, photodeposition and doping methods.



## *2 Photocatalyst characterization*

2.1 The bulk crystal structure and chemical phase composition is determined by X-ray diffraction (XRD)

2.2 The crystallite size is observed using transmission electron microscopy (TEM).

2.3 The surface area of photocatalyst, average pore size diameter and pore size distribution are determined by physisorption of nitrogen using the BET method.

2.4 Diffuse reflection spectra are measured using UV-vis spectrophotometer to estimate bandgaps of photocatalysts.

2.5 The relative amounts of  $Ti^{3+}$  surface defects of the  $TiO_2$  based photocatalyst samples are determined by electron spin resonance spectroscopy (ESR).

2.6 The actual amounts of Au cocatalysts are determined by inductively coupled plasma (ICP).

2.7 The relative amounts of active gold metals on the  $TiO_2$  based photocatalyst samples are calculated from  $H_2$  chemisorption.

## *3 Photocatalytic $H_2$ production testing*

Reaction testing of Au modified  $TiO_2$  photocatalyst is made to investigate the photocatalytic activity for  $H_2$  production from formic acid aqueous solution under solar simulation.

## CHAPTER 2

### LITERATURE REVIEWS

#### 2.1 TiO<sub>2</sub> preparation by solvothermal method

The solvothermal method employ chemical reactions in several organic media such as Ethanol [21,74], Buthanol[19], Ethylene glycol [19,27,72], 1,4-butandiol [17-19,22], Glycerol [19] and toluene [22,23] under self produced pressures at low temperatures (usually under 300 °C). Generally, the solvothermal treatment could be useful to control grain size, particle morphology, crystalline phase, and surface chemistry by regulating the solution composition, reaction temperature, pressure, solvent properties, additives, and ageing time. So far, there are several conditions to synthesized TiO<sub>2</sub> for photocatalytic application of TiO<sub>2</sub> as shown in Table 2.1. On the other hand, in case of reaction in 1,4-butanediol, irregular aggregates of nanometer particles are observed for all reaction holding period investigated. It was concluded that nanocrystalline anatase titania prepared in 1,4-butanediol crystallized directly from the solution. On the other hand, for the reaction in toluene, crystalline anatase titania was obtained from solid state transformation of precipitated amorphous product. This difference in morphology suggests that the colloidal stability of the precipitate in toluene is different from that in 1,4-butanediol. The results can be explained by the difference in the dielectric constant of the organic solvents, which affect the colloidal stability and morphology of the product. Moreover, M. Kang [17] found that the solvothermal TiO<sub>2</sub> have a higher the surface charge and the activation energies for desorption of water molecules more than sol-gel method, which were adsorbed on and in particles. From this result, it could be suggested that solvothermal TiO<sub>2</sub> particles were more stable in water (well dispersed in water) and very hydrophilic property.

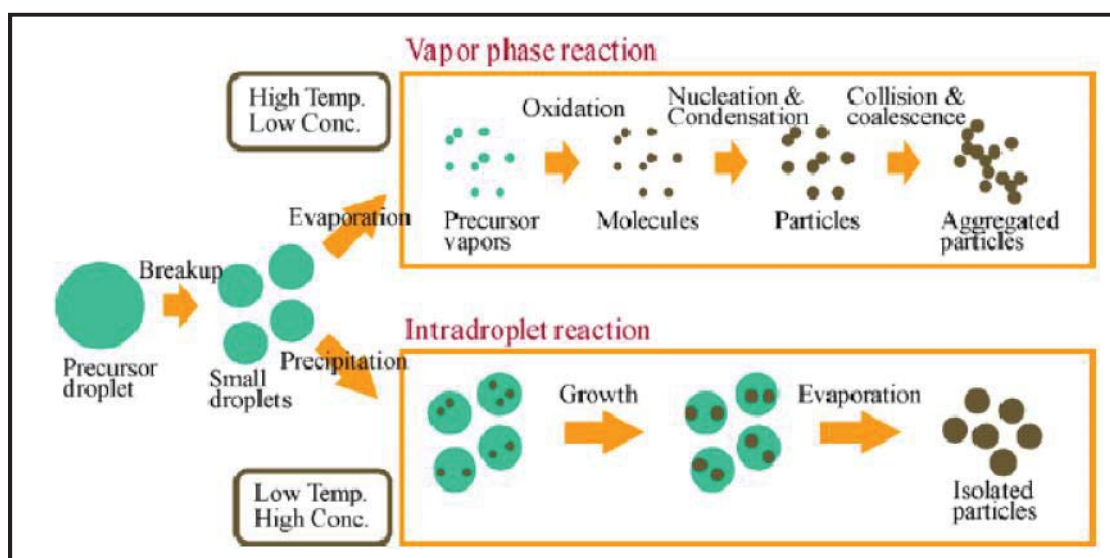
**Table 2.1** Several conditions for TiO<sub>2</sub> synthesis by solvothermal method

Solvent	Temperature (°C)	Holding Time (h)	Surface area (m <sup>2</sup> /g)	Crystallite size (nm)	Photocatalytic application	Ref.
1,4-butadiol	300	5/6	122	20-50	CHCl <sub>3</sub> decomposition	17
1,4-butadiol	300	1	120	30-50	Methanol decomposition	18
Butanol	300, 350	1	96, 102	12, 7	Methyl Orange decomposition	19
1,4-butadiol	300, 350	1	99, 122	8, 6	Methyl Orange decomposition	19
Glycerol	300, 350	1	107, 111	6, 6	Methyl Orange decomposition	19
Ethylene glycol	160-180	120	120	-	H <sub>2</sub> production	19
Ethanol	200	10	140	-	Acetaldehyde decomposition	21
1,4-butadiol	200-300	0-4	100-150	9-15	Ethylene decomposition	22
Toluene	200-300	0-4	143-204	9-13	Ethylene decomposition	22
Toluene	300-350	0.5-8	51-126	9-15	Ethylene decomposition	23
Ethylene glycol	110	48	91	6-24	H <sub>2</sub> production	27
Ethanol + Acetic acid	200	8	-	15	Dye-sensitized solar cell	28
Ethylene glycol + water	180	8	484	<10	Methyl Orange decomposition	72
Ethanol	160	6	420	5	Phenol decomposition	73

## 2.2 TiO<sub>2</sub> preparation by flame spray pyrolysis method

In the past two decades flame aerosol synthesis of novel materials has experienced significant growth in both industry and academia. Recent research is focused on the development of new materials in the nanosized range to be used in various applications, such as catalysis, sensors, bio (orthopaedic, dental and nutritional products), phosphors and electroceramics (fuel cells, batteries, superconductors and ferrites) [32]. Several studies indicate that this scalable synthesis method can result in novel and metastable phases of mixed metal oxides of high purity, which may not be easily accessible by conventional wet- or solid-state processes [36,70]. Especially for photocatalytic applications this synthesis method is emerging as an attractive fast and single-step production route for high surface area materials, often with unprecedented structural and photocatalytic properties. The large variety of possible organometallic precursors especially for the liquid-fed aerosol flame synthesis makes this technique very versatile for photocatalyst synthesis. The main advantage of FSP is the formation of generally homogeneous, nanosized particles through control of the precursor solvent composition [31]. FSP has been used for the synthesis of TiO<sub>2</sub> photocatalysts with different conditions as shown in Table 2.2. Furthermore, they exhibited high photocatalytic activity in the several photocatalytic applications (Table 2.2). However, characteristics of TiO<sub>2</sub> synthesis by FSP depend on conditions such as type of precursor, liquid precursor flow rate, precursor concentration, type of solvent and flow rate of dispersed gas. Increasing the precursor concentration and the feed flow rate as well as the reduction of O<sub>2</sub> dispersing gas during the FSP synthesis would increase the supplied fuel energy to the spray and/or particle concentration so that larger particle size can be obtained, which have been reported by [30,77]. Moreover, H. Chang et al. [76] suggested a mechanism for the generation and growth of TiO<sub>2</sub> nanoparticles in the FSP as shown in Figure 2.1, which exhibited the effect of temperature in flame and concentration of precursor. Nevertheless, the effect of type of organic solvent also influences the physical properties of TiO<sub>2</sub> nanoparticles. G.L. Chiarello et al. [33] reported that the surface area of the FSP synthesised TiO<sub>2</sub> photocatalysts linearly decreases with increasing the combustion heat of the organic solvent/fuel employed. With increasing the combustion heat, the

flame temperature becomes higher, with a consequent increase in the rate of particles growth. Thus, larger particles are obtained, possessing lower specific surface area. The quantitative phase analysis of samples from carboxylic acids solutions, revealed a higher rutile content with increasing the combustion enthalpy of the Ti-precursor solvents, thus for higher flame temperature. However, the use of xylene, the solvent with the highest combustion enthalpy value, led to a higher anatase content in sample. This points to a different TiO<sub>2</sub> formation mechanism in the flame when xylene, an apolar solvent, is used instead of carboxylic acids because, when carboxylic acids are mixed with Ti-isopropoxide the formation of titanium carboxylate and isopropanol can occur, a reaction which is not possible when the same titanium precursor is dissolved in xylene. Therefore, depending on the organic solvent/fuel, TiO<sub>2</sub> synthesis by FSP can start from different titanium precursors, undergoing different oxidation mechanisms in the flame. Furthermore, using xylene as solvent, the sample showed less diffuse scattering with respect to the other FSP samples, indicating a higher crystallinity and a lower content of crystal defects. This may be ascribed to the much higher flame temperature produced by the xylene fuel.



**Figure 2.1** Mechanism for the generation and growth of TiO<sub>2</sub> nanoparticles in the FSP [76]

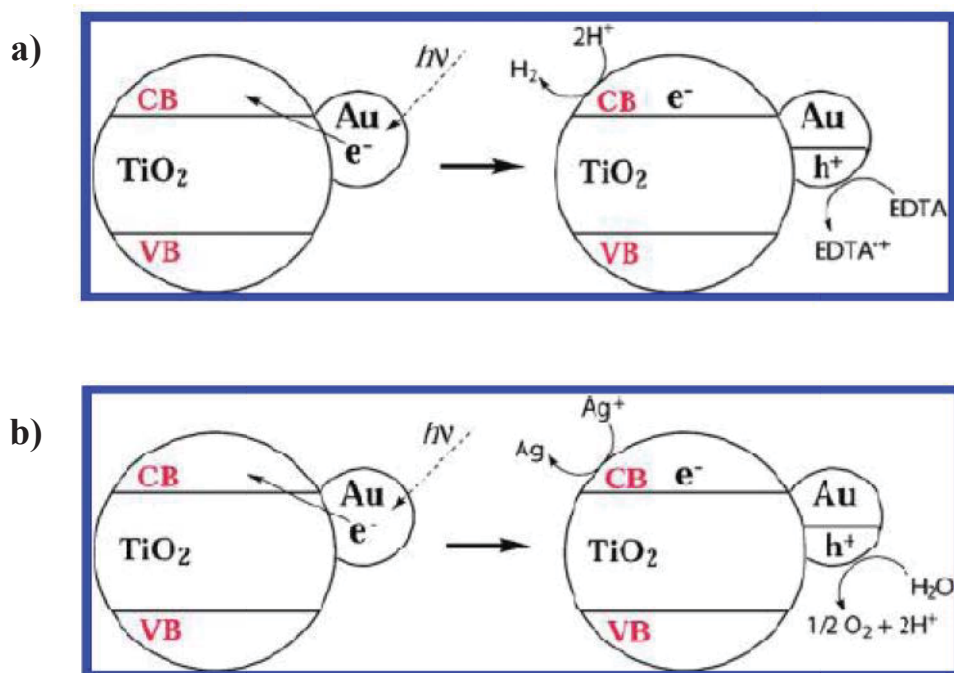
**Table 2.2** Several conditions for TiO<sub>2</sub> synthesis by flame spray pyrolysis method

Solvent	Precursor concentration (mol/l)	precursor flow rate (ml/min)	O <sub>2</sub> dispersed flow rate (l/min)	Surface area (m <sup>2</sup> /g)	Crystallite size (nm)	Photocatalytic application	Ref.
Xylene + Acetonitrile	0.65	3-7	5	-	7-20	Sucrose mineralisation	30
Propionic acid	0.15	3.1	6	66	5-10	H <sub>2</sub> production	33
Propionic acid + Methanol	0.15	3.1	6	68	-	H <sub>2</sub> production	33
Xylene	0.15	3.1	6	54	-	H <sub>2</sub> production	33
Xylene + Pyridine	0.15	3.1	6	106	-	H <sub>2</sub> production	33
Xylene + Acetonitrile	-	4	5	70	10-25	H <sub>2</sub> production	34
Xylene + Acetonitrile	0.65	5	5	89	16	Oxalic acid mineralisation	74
Xylene	0.15	3.1	6	106	5-10	H <sub>2</sub> production	75

### 2.3 Using Au cocatalyst in photocatalytic H<sub>2</sub> production

A. Iwase et al. [62] reported that loading of fine Au particles improved photocatalytic activity for water splitting in some titanate, niobate and tantalate photocatalysts because the fine Au particles play an important role in the creation of active sites for H<sub>2</sub> evolution and the enhancement of charge separation. Moreover, the backward reaction between H<sub>2</sub> and O<sub>2</sub> to produce water on the Au cocatalyst was negligible in comparison with that on a Pt cocatalyst, which is suitable in overall water splitting. Recently, T.Puangpetch et al. [63] presented that Au loaded SrTiO<sub>3</sub> exhibited the highest photocatalytic H<sub>2</sub> production rate when comparison with Ag, Pt, Ni, Fe and Ce under both UV and visible irradiation. They explained that Au has higher electronegativity (EN) and electron affinity (EA) than the other metal. The higher EN of metal cocatalyst, as compared to that of the based photocatalyst, resulting

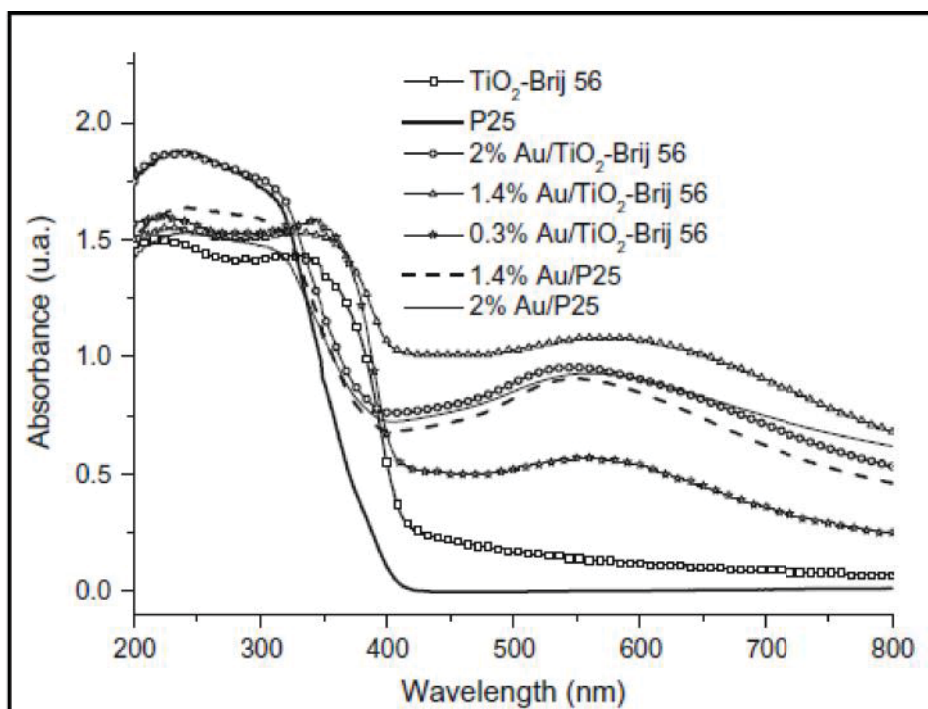
in a more easy photoexcited electron transfer from conduction band of based photocatalyst to the metal cocatalyst. Whereas, high EA promoted the stability of the photogenerated electrons until the proton reduction reaction takes place on the metal cocatalyst surface. Moreover, Au has a high ionic radius, resulting in a high H-OH breaking ability. So that, water can be easily reduced to H<sub>2</sub> on the Au metal surface. Presently, C.G. Silva et al. [64] used Au in modification of TiO<sub>2</sub> for photocatalytic H<sub>2</sub> production under visible light. It can be prepared strongly anchored on the titania surface and it exhibits a characteristic surface plasmon band in the visible region due to the collective excitation of electrons in the gold nanoparticles. They demonstrated that gold can have an additional role as light harvester besides gas evolution center. We have found that, using excitation wave lengths corresponding to gold plasmon band, gold nanoparticles absorb photons and inject electrons into the semiconductor conduction band as shown in Figure 2.2. This photoinduced electron injection into the conduction band of a semiconductor is unusual for a metal, but the nanometric size of the gold particles and the operation of quantum size effects should be responsible for the occurrence of this mechanism. Electrons in the titania conduction band and holes in certain gold nanoparticles have adequate potential to generate hydrogen and oxygen from water, respectively. In addition, O. Rosseler et al. [59] proved that using Au modified TiO<sub>2</sub>, it can reduce the wide band gap of TiO<sub>2</sub> and enhance visible light absorption as shown in Table 2.3 and Figure 2.3. Hence, Au is a promising in modification of wide band gap photocatalyst for response to visible light. However, these properties depend on method in modification of Au, which have been reported by V.R. Gonzalez et al. [78].



**Figure 2.2** Mechanism of the photocatalytic activity of Au/TiO<sub>2</sub> forming H<sub>2</sub> (a) or O<sub>2</sub> (b) upon excitation of the gold surface plasmon band [64]

**Table 2.3** Band gap and cut-off wavelength absorption of the different Au/TiO<sub>2</sub> photocatalyst [59]

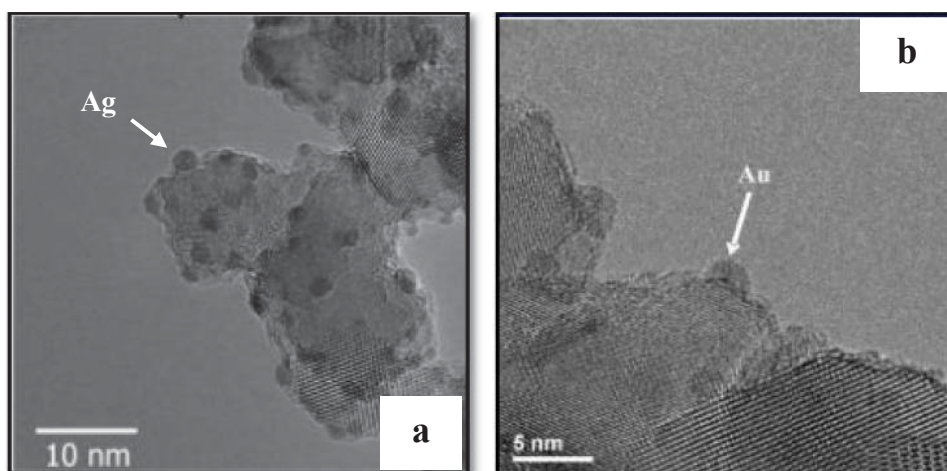
Photocatalyst	Band gap (eV)	Maximum wavelength absorption (nm)
P25	3.23	385
TiO <sub>2</sub> Brij56	3.02	411
1.4 wt.% Au/P25	2.69	461
2 wt.% Au/P25	2.76	450
0.3 wt.% Au/TiO <sub>2</sub> Brij56	2.91	427
1.4 wt.% Au/TiO <sub>2</sub> -Brij56	2.56	485
2 wt.% Au/TiO <sub>2</sub> anatase-Brij56	2.73	455



**Figure 2.3** Light absorption properties of Au/TiO<sub>2</sub> photocatalysts [59]

## 2.4 Metal cocatalyst photodeposition

Metal photodeposition method is photoreducing of metal ions on based photocatalyst surface. G.R. Bamwenda et al. [65] proved that the photodeposition of Au and Pt have higher efficiency in photocatalytic H<sub>2</sub> production than deposition-precipitation, impregnation and physical mixing because Au and Pt particles are well dispersed on TiO<sub>2</sub> and small metal particles in the rang 1-10 nm for Au/TO<sub>2</sub> and in the rang 1-6 for Pt/TiO<sub>2</sub>. In addition, the exposed nanosize or surface area of gold has only a small influence on the rate of hydrogen generation. However, the final Au and Pt loadings obtained during photodeposition depend on the type and concentration of hole scavengers and the illumination time and intensity. In 2005, S.C. Chan and M.A. Barteau [66] prepared Ag and Au on TiO<sub>2</sub> by photodeposition. They found that this technique distinguishes individual Au or Ag nanoparticles with highly uniform metal nanoparticles in the 1-2 nm size range and provides a new route to generate supported metal catalysts with highly uniform sites on the nanoscale, which is not possible with other techniques as shown in Figure 2.4.



**Figure 2.4** TEM image of Ag particles (a) and Au particles (b) on TiO<sub>2</sub> by photodeposition method [66]

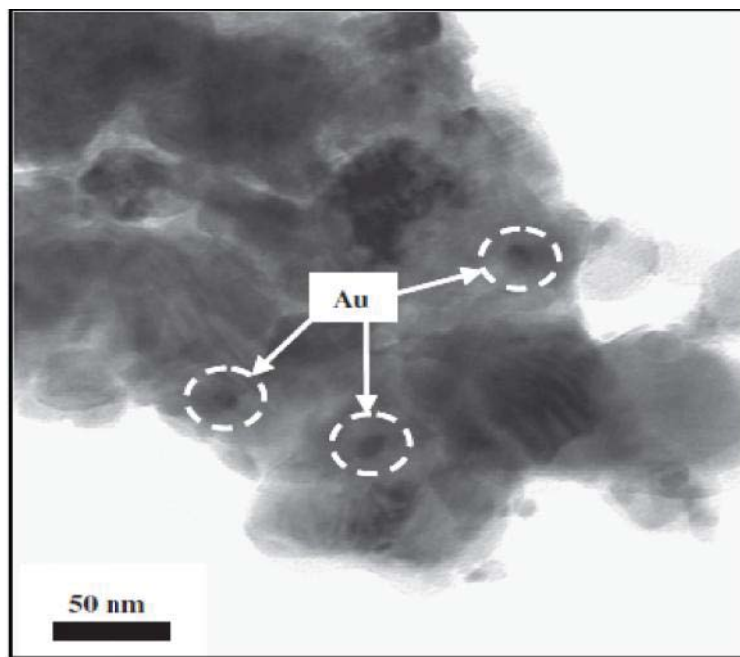
M.A. Behnajady et al. [67] compared Ag loading by photodeposition and liquid impregnation methods for photodegradation of C.I. Acid Red 88. They found that the photocatalytic activity of Ag-photodeposited TiO<sub>2</sub> was much higher than of silver loaded TiO<sub>2</sub> prepared by liquid impregnation method. The difference in the photoactivity of silver doped TiO<sub>2</sub> prepared with different methods can be discussed in terms of the oxidation state of silver on TiO<sub>2</sub> surface. During the preparation process by photodeposition method, Ag<sup>+</sup> ions in the suspension were reduced to Ag, but in the liquid impregnation method silver deposited at TiO<sub>2</sub> surface as Ag<sup>+</sup> ions. In the silver doped TiO<sub>2</sub> with liquid impregnation method (Ag<sup>+</sup>-TiO<sub>2</sub>), the reduction of silver ions to metallic silver consumes electrons, resulting photoactivity decreased than photodeposition. Moreover, an optimum value metal content in photodeposition method less than liquid impregnation method. So that, photodeposition method is a promising for loading expensive metal, especially noble metal. However, photocatalytic activity of metal cocatalyst loading on based photocatalyst by photodeposition method depend on conditions during photodeposition in preparation. M.C. Hidalgo et al. [68] reported that conditions in photodeposited preparation of Au over TiO<sub>2</sub> such as pH, light intensity and deposition time showed to have a high influence on the photodegradation of phenol. Conditions during the photodeposition

process, especially light intensity and deposition time, were proved to have a high influence on the final properties of gold deposits. Photodeposition using illumination at high light intensity appeared as an ineffective method for obtaining Au-TiO<sub>2</sub> photocatalysts for photocatalytic applications as this condition led to very large and heterogeneously distributed gold deposits. On the contrary, when the photodeposition was performed with low light intensity the resulted gold deposits were much smaller obtaining materials with improved photocatalytic activity for phenol degradation. By illumination at low light intensity, amount of gold effectively deposited, aggregation and oxidation state can be controlled by changing the deposition time, enabling a feasible method of tailoring Au-TiO<sub>2</sub> with the appropriate properties for a high photocatalytic activity.

## 2.5 Metal cocatalyst doping

Modification of cocatalyst by doping method are high efficiency in photocatalytic activity because good dispersion of doped cocatalyst in the final product is attained and there appears to be more interaction between based photocatalyst, resulting in excellent photocatalytic performance over conventional methods [63,69]. Moreover, this method is more straightforward method for loading a metal cocatalyst than incipient wetness impregnation. T. Sreethawong et al. [69] prepared Cu, Pd and Au loaded mesoporous TiO<sub>2</sub> photocatalyst by this method for photocatalytic H<sub>2</sub> production. Their XRD and EDS results confirm that the cocatalysts were well dispersed through the mesoporous TiO<sub>2</sub> support via the single-step sol-gel preparation. In 2010, this method was used by T. puangpetch et al. [63] in metal cocatalyst loaded mesoporous SrTiO<sub>3</sub> nanophotocatalyst for photocatalytic H<sub>2</sub> production. From XRD patterns, found that all the loaded metals at low loadings in the range of 0.1-1.5 wt.% do not significantly affect the crystallinity and purity of the synthesized SrTiO<sub>3</sub> photocatalysts. Besides, no crystalline phases of the metals loaded via the single-step sol-gel method were observed in the XRD patterns, probably due to their high dispersion through the mesoporous-assembled structures. XRF results confirm that this method used for loading metals is reliably effective in controlling any desired cocatalyst loading. Moreover, metal loaded based photocatalyst by this method showed small nanoparticle size of metal cocatalysts, resulting in enhancing of

photocatalytic activity. For example, Au cocatalyst loaded mesoporous SrTiO<sub>3</sub> by single-step sol-gel gave small Au particle size in the rang of 10-15 nm [79] as show in Figure 2.5.



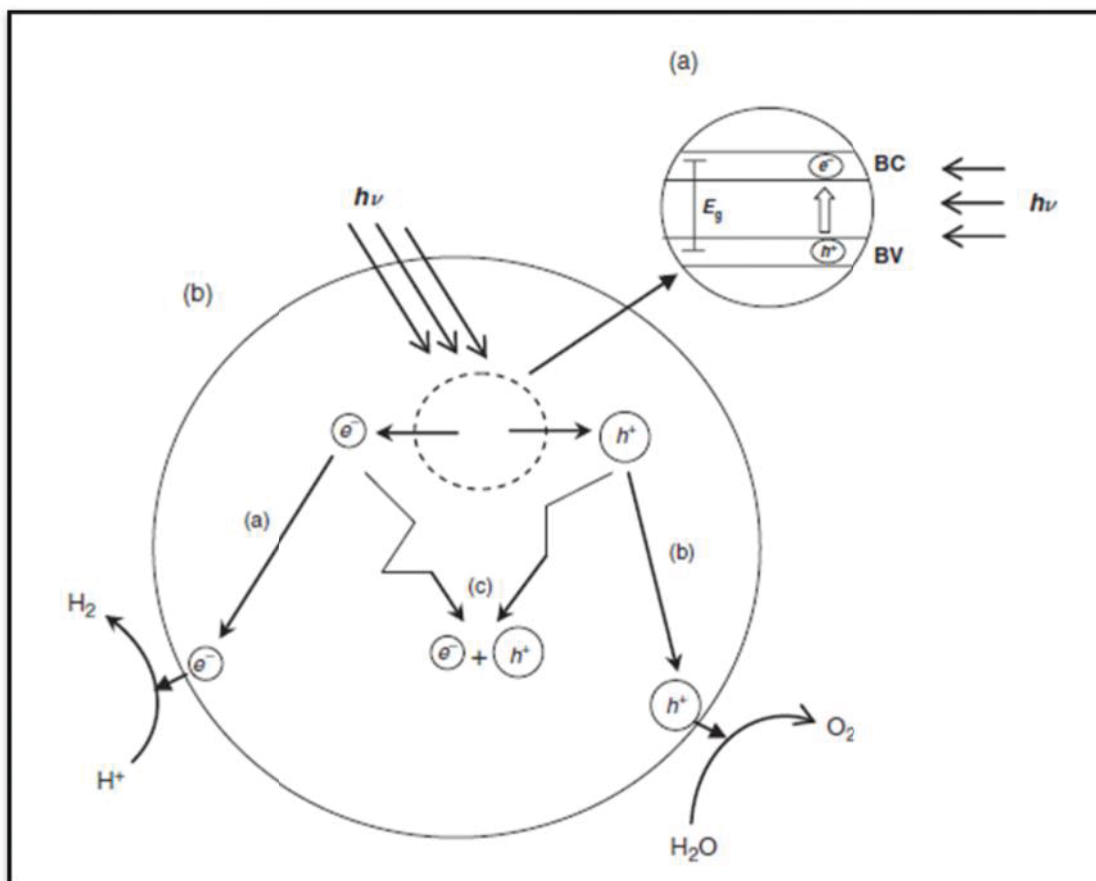
**Figure 2.5** TEM image of the 1 wt.% Au-loaded mesoporous SrTiO<sub>3</sub> photocatalyst [79]

## CHAPTER 3

### THEORY

#### 3.1 Basic principles of photocatalytic H<sub>2</sub> production

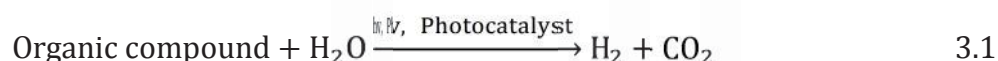
The photocatalytic decomposition of water has been extensively studied on various systems, however, sustained and overall water decomposition into H<sub>2</sub> and O<sub>2</sub> has been accomplished in only a limited number of cases. At the present stage, the quantum efficiency (QE) for overall water splitting is still very low (QE < 2%) under visible light over such a semiconductor particle photocatalyst due to water decomposition is a very difficult and complex reaction because it involves a four-photon process for O<sub>2</sub> evolution and a two-photon process for H<sub>2</sub> evolution. The various intermediate chemical steps represent a kinetic limitation that decreases the efficiency of the reaction and a rapid reverse-reaction between the produced H<sub>2</sub> and O<sub>2</sub> and/ or reaction intermediates on the surface of the small semiconductor particles. Thus, a critical problem to be resolved for an efficient up-hill reaction is to prevent such a thermodynamically-favored reverse-reaction. One possible way to overcome this problem is the use of sacrificial electron donors or hole scavengers (alcohol, organic acid, sulfide ions and others) with a high QE (>10%) because this reaction is down-hill reaction, the photo-energy absorbed by a photocatalyst induces thermodynamically favored reactions, accompanied by a large negative change in the Gibbs free energy ( $\Delta G < 0$ ). Specially, photocatalysis of organic compounds and water into CO<sub>2</sub> and H<sub>2</sub>, if organic compound is organic wastes, not only produce economic H<sub>2</sub> but also solution of enviromental problems. The basic principle of photocatalytic reaction for hydrogen generation using sacrificial electron donor reagents is depicted schematically in Figure 3.1



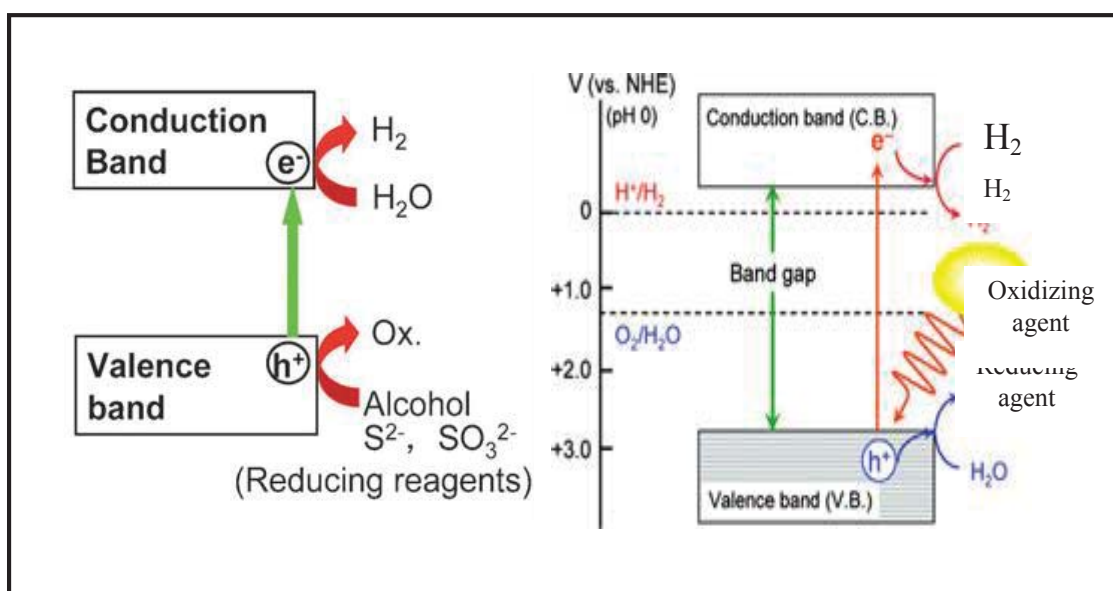
**Figure 3.1** The principle of photocatalytic  $H_2$  production in the presence of electron donor reagent: (A) photoelectronic excitation in the photocatalyst generating electron-hole pairs and (B) processes occurring on photocatalyst particle following photoelectronic excitation [4]

When a photosemiconductor absorbs light photons with energies greater than its band gap energy ( $E_g$ ). This absorption creates excited photoelectrons in the conduction band (CB) and holes in the valence band (VB) of the semiconductor, as schematically depicted in Figure 3.1(A). As indicated in Figure 3.1(B), once the photogenerated electron-hole pairs have been created in the semiconductor bulk, they must separate and migrate to the surface (paths a and b in Figure 3.1(B)) competing effectively with the

electron-hole recombination process (path c in Figure 3.1(B)) that consumes the photocharges generating heat. At the surface of the semiconductor, the photoinduced electrons and holes reduce adsorbed water to produce gaseous hydrogen and oxidize adsorbed organic as reducing reagent to produce carbon dioxide by the following reactions:



Because the photogenerated holes irreversibly oxidize the reducing electron donors instead of  $\text{H}_2\text{O}$ , it enriches electrons in a photocatalyst and if the bottom of the conduction band of the photocatalyst is located at a more negative potential than the water reduction potential, this then facilitates water reduction by the photogenerated electrons in the conduction band as illustrated in Figure 3.2.



**Figure 3.2** Schematic diagram of photocatalytic  $\text{H}_2$  production in the presence of reducing reagent [5]

### 3.2 Evaluation of photocatalytic H<sub>2</sub> production

There are two apparent indicators that should be paid attention in evaluating the hydrogen generation through photocatalysis. One is photocatalytic activity and the other one is photocatalytic stability.

#### 3.2.1 Photocatalytic activity

The efficiency of photocatalytic hydrogen generation from photocatalysis can be measured directly on the amount of hydrogen gas evolution or indirectly on the electrons transferred from semiconductor to water within a certain time period under light irradiation. Different photocatalytic setup configurations, such as inner irradiation type and top irradiation type, and light sources, such as Xe lamp and Hg lamp, are commonly used by different research groups and scientists, which may give different rates of gas evolution when exactly the same photocatalyst is used. This makes it difficult to make direct comparison across the results from different research groups and photocatalytic hydrogen generation systems. Nevertheless, it seems helpful to get approximate correlations between various results if normalize the rates of gas evolution to the amount of photocatalyst employed within a unit of time. Here, using the rate of H<sub>2</sub> gas evolution with units such as  $\mu\text{mol}\cdot\text{h}^{-1}$  and  $\mu\text{mol}\cdot\text{h}^{-1}\cdot\text{g}_{\text{cat}}^{-1}$  to make the measurable comparison between different photocatalysts under similar experimental conditions. The apparent quantum yield, as an extension from the overall quantum yield in a homogeneous photochemical system, becomes important and acceptable to evaluate the photocatalytic activity for water splitting. The overall quantum yield and apparent quantum yield are defined by the following eqs 3.2, 3.3 and 3.4, respectively:

$$\text{Overall quantum yield (\%)} = \frac{\text{Number of reacted electrons}}{\text{Number of absorbed photons}} \times 100 \quad 3.2$$

$$\text{Apparent quantum yield (QY, \%)} = \frac{\text{Number of reacted electrons}}{\text{Number of incident photons}} \times 100 \quad 3.3$$

$$\text{Or for H}_2 \text{ evolution} = \frac{2 \times \text{Number of evolved H}_2 \text{ molecules}}{\text{Number of incident photons}} \times 100 \quad 3.4$$

The apparent quantum yield is estimated to be smaller than the total quantum yield because the number of absorbed photons is usually smaller than that of incident light. In addition to the quantum yield, the solar energy conversion efficiency that is usually used for evaluation of solar cells is also sometimes reported in the literature. It is defined as following eq 3.5:

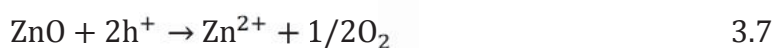
$$\text{Solar energy conversion (\%)} = \frac{\text{Output energy of H}_2 \text{ evolved}}{\text{Energy of incident solar light}} \times 100 \quad 3.5$$

### 3.2.2. Photocatalytic stability

As a good photocatalyst, it should have a good stability for H<sub>2</sub> and/or O<sub>2</sub> production, besides a high photocatalytic activity or quantum yield. To test the photocatalytic stability, a long-time experiment or a repeated experiment is always necessary. Photocorrosion is considered to be the main reason causing the poor stability of photocatalysts, especially the metal sulfide photocatalysts. CdS has frequently been reported to be unstable for photocatalytic H<sub>2</sub> evolution. S<sup>2-</sup> in CdS rather than water is self-oxidized by photoinduced holes in the valence band of CdS. The photocorrosion reaction occurs as following eq 3.6:



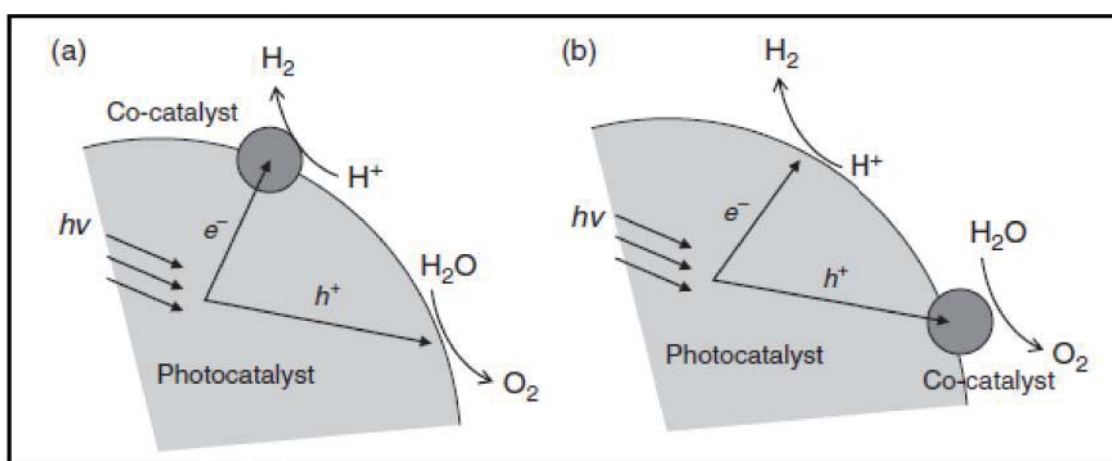
Moreover, ZnO is also photocorroded under band gap excitation even if it is an oxide photocatalyst, which the reaction occurs as following eq 3.7:



## 3.2 Techniques to enhance photocatalytic H<sub>2</sub> production

### 3.3.1 Surface modification by deposition of cocatalysts

The deposition of noble metals (such as Pt, Rh, and Au) or metal oxides (such as NiO and RuO<sub>2</sub>) onto photocatalyst surfaces is an effective way of enhancing photocatalyst activity. The cocatalyst improves the efficiency of photocatalysts, as shown in Figure 3.3, as a result of (i) the capture of CB electrons or VB holes from the photocatalysts, thereby reducing the possibility of electron-hole recombination and (ii) the transference of electrons and holes to surface water molecules, thereby reducing the activation energy for the reduction/oxidation of water. The activity of the cocatalysts is found to be strongly dependent on electrochemical properties, cocatalyst preparation method and the quantity of cocatalysts deposited on the photocatalyst surface. When the amount exceeds a critical limit, the cocatalysts act as electron-hole recombination centers, reducing the efficiency of the host photocatalyst.



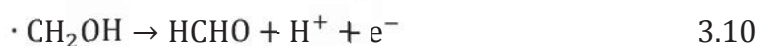
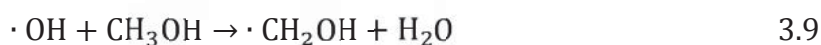
**Figure 3.3** Schematic diagram of photocatalyst surface modification by the addition of cocatalyst to facilitate the hydrogen (a) or oxygen (b) evolution in water splitting [4]

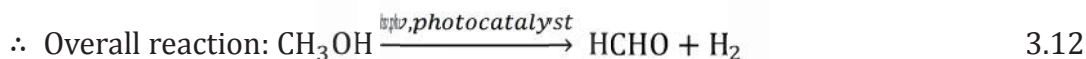
### 3.3.2 Particle size and Surface area

General based on heterogeneous catalysis is that the efficiency of a catalytic reaction increases with increase in surface area of the catalyst. Moreover a low surface photocatalyst recombination rate is an essential condition for carriers reaching interface to react with suitable adsorbed species, whereas a large surface areas, diffusion length of charge carriers was large compared to size of the particles. For very small particles, no internal electric field is necessary to separate photogenerated electron-hole pairs. Therefore, possibility for the charge carriers to reach the interface increased as the size of particles decreased. Nanoparticle was most interested which very small particles and large surface area in order to enhance hydrogen production.

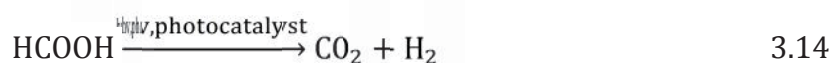
### 3.3.3 Organic sacrificial electron donor reagents for photocatalytic H<sub>2</sub> production

Organic compounds, such as alcohols (methanol, ethanol, isopropanol, etc.), organic acids (formic acid, acetic acid, etc.), and aldehydes (formaldehyde, acetaldehyde, etc.) have all been used as electron donors for photocatalytic hydrogen generation. Among them, methanol was most widely used, and the hydrogen generation process is described as eqs 3.8-3.12:





The product, formaldehyde (HCHO), could be further oxidized to methanoic acid HCOOH and subsequently to  $\text{CO}_2$  together with hydrogen generation via eqs 3.13 and 3.14:



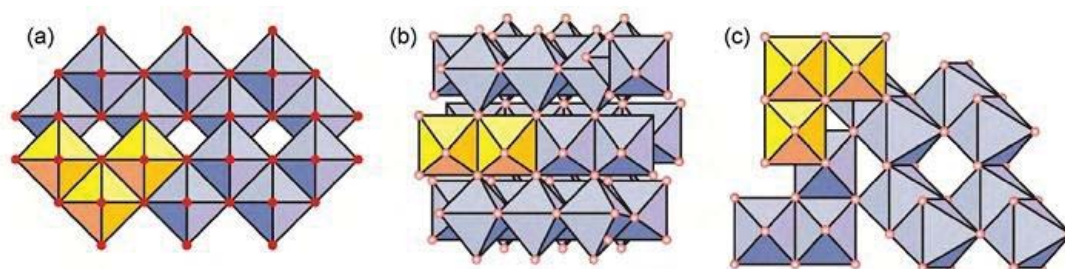
In these photocatalytic systems, organic compounds are oxidized and decomposed by the photogenerated holes. Meanwhile, the remaining photogenerated electrons reduce water to hydrogen. Thus, it can be envisaged that a bifunctional photocatalytic system could be constructed, in which organic pollutants will be used to act as electron donors that achieve photocatalytic production of hydrogen from polluted water and simultaneous degradation of organic pollutants.

### 3.4 Crystal structure and properties of $\text{TiO}_2$ [9-11,14]

Titanium dioxide, also known as titanium (IV) oxide, with molecular weight of  $79.87 \text{ g}\cdot\text{mol}^{-1}$  is the naturally occurring oxide of titanium with the chemical formula  $\text{TiO}_2$ . Titanium dioxide is extracted from a variety of naturally occurring ores that contain ilmenite, rutile, anatase and leucosene, which are mined from deposits throughout the world. Titanium dioxide has a wide range of applications. It is used mostly as a pigment in paints, sunscreens, ointments, and toothpaste since its commercial production in the early twentieth century. Titanium dioxide pigments are inorganic chemical products used for imparting whiteness, brightness and opacity to a diverse range of applications and end-use markets, including coatings, plastics, paper and other industrial and consumer products.  $\text{TiO}_2$  is considered a “quality-of-life” product with demand affected by gross domestic product in various regions of the world.  $\text{TiO}_2$  as a pigment derives value from its whitening properties and opacifying ability (commonly referred to as hiding power). As a result of  $\text{TiO}_2$ 's high refractive

index rating, it can provide more hiding power than any other commercially available white pigment.

Crystals of titanium dioxide can exist in one of the three crystalline forms: rutile, anatase or brookite and they have different properties as shown in Table 3.1. In their structures, the basic building block consists of a titanium atom surrounded by six oxygen atoms in a more or less distorted octahedral configuration. In all the three  $\text{TiO}_2$  structures, the stacking of the octahedra results in three fold coordinated oxygen atoms. The fundamental structural unit in these three  $\text{TiO}_2$  crystals forms from  $\text{TiO}_6$  octahedron units and has different modes of arrangement and links as presented in Figure 3.4. In the rutile form,  $\text{TiO}_6$  octahedra link by sharing an edge along the c-axis to form chains. These chains are then interlinked by sharing corner oxygen atoms to form a three-dimensional framework. Conversely in anatase, the three-dimensional framework is formed only by edge-shared bonding among  $\text{TiO}_6$  octahedrons. It means that octahedra in anatase share four edges and are arranged in zigzag chains along. In brookite, the octahedra share both edges and corners, forming an orthorhombic structure. In coming up with these crystal structures and to estimate the crystal grain size of anatase, rutile and brookite the X-ray diffraction (XRD) experimental method is used. Anatase peaks in X-ray diffraction are occurred at  $\theta = 12.65^\circ$ ,  $18.9^\circ$ , and  $24.054^\circ$ , the rutile peaks are found at  $\theta = 13.75^\circ$ ,  $18.1^\circ$ , and  $27.2^\circ$  while brookite peaks are encountered at  $\theta = 12.65^\circ$ ,  $12.85^\circ$ ,  $15.4^\circ$ , and  $18.1^\circ$ .  $\theta$  represents the X-ray diffraction angle.



**Figure 3.4** Crystalline structure of: (A) anatase, (B) brookite and (C) rutile [14]

Crystal structure	System	Space group	Lattice constants (nm)			
			<i>a</i>	<i>b</i>	<i>c</i>	<i>c/a</i>
Rutile	Tetragonal	D <sub>4h</sub> <sup>14</sup> -P4 <sub>2</sub> /mmm	0.4584	–	0.2953	0.644
Anatase	Tetragonal	D <sub>4h</sub> <sup>19</sup> -I4 <sub>1</sub> /amd	0.3733	–	0.937	2.51
Brookite	Rhombohedral	D <sub>2h</sub> <sup>15</sup> -Pbca	0.5436	0.9166	–	0.944
Density (kg/m <sup>3</sup> )						
Rutile	4240					
Anatase	3830					
Brookite	4170					
Dielectric properties						
	Frequency (Hz)	Temperature (K)	Dielectric constant			
Rutile, perpendicular to optical <i>c</i> -axis	10 <sup>8</sup>	290–295	86			
Rutile, parallel to optical <i>c</i> -axis	–	290–295	170			
Rutile, perpendicular to optical <i>c</i> -axis	10 <sup>4</sup>	298	160			
Rutile, along <i>c</i> -axis	10 <sup>7</sup>	303	100			
Anatase, average	10 <sup>4</sup>	298	55			
Band gap (eV)						
Rutile	3.05					
Anatase	3.26					
Refractive index						
	<i>n<sub>g</sub></i>	<i>n<sub>p</sub></i>				
Rutile	2.9467	2.6506				
Anatase	2.5688	2.6584				
Brookite	2.809	2.677				

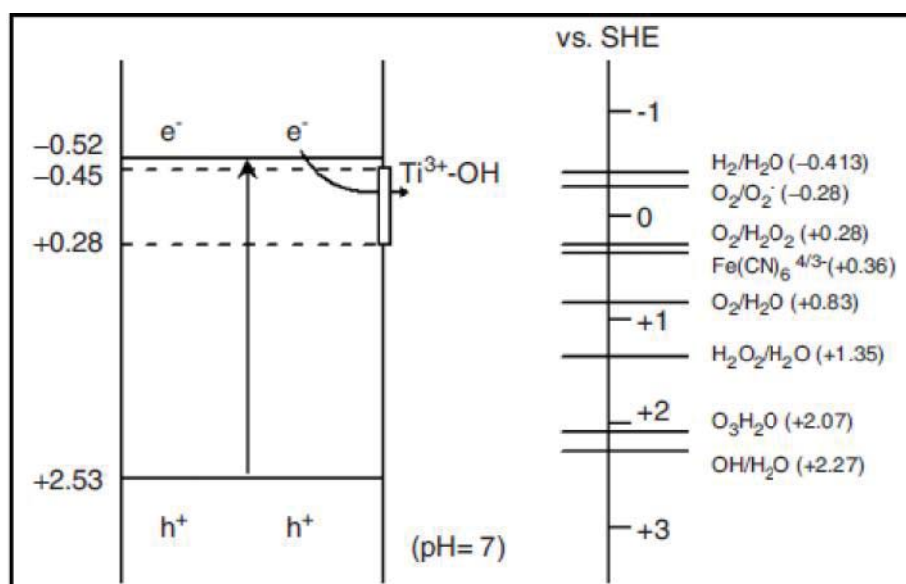
**Table 3.1** Some bulk properties of the three main polymorphs of TiO<sub>2</sub> (anatase, rutile, and brookite) [9]

Thermodynamic calculations based on calorimetric data predict that rutile is the stablest phase at all temperatures and pressures up to 60 kbar. The small differences in the Gibbs free energy (4–20 kJ/mole) between the three phases suggest that the metastable polymorphs are almost as stable as rutile at normal pressures and temperatures. Particle size experiments affirm that the relative phase stability may reverse when particle sizes decrease to sufficiently low values due to surface-energy

effects (surface free energy and surface stress, which depend on particle size). If the particle sizes of the three crystalline phases are equal, anatase is most thermodynamically stable at sizes less than 11 nm, brookite is most stable between 11 and 35 nm, and rutile is most stable at sizes greater than 35 nm. The enthalpy of the anatase  $\rightarrow$  rutile phase transformation is low. A survey of the literature reveals widespread disagreement, with values ranging from -1.3 to  $-6.0 \pm 0.8$  kJ/mol. Kinetically, anatase is stable, i.e., its transformation into rutile at room temperature is so slow that the transformation practically does not occur. At macroscopic scale, the transformation reaches a measurable speed for bulk  $\text{TiO}_2$  at  $T > 600$  °C. During the transformation, anatase pseudo-closed-packed planes of oxygen are retained as rutile closed-packed planes and a co-operative rearrangement of titanium and oxygen ions occurs within this configuration. The proposed mechanism implies at least spatial disturbance of the oxygen ion framework and a minimum breaking of Ti-O bonds as a result of surface nucleation and growth. The nucleation process is very much affected by the interfacial contact in nanocrystalline solids, and once initiated, it quickly spreads out and grain growth occurs. The monotropic anatase  $\rightarrow$  rutile conversion has been studied for both mechanistic and application-driven reasons, because the  $\text{TiO}_2$  phase (i.e., anatase or rutile) is one of the most critical parameters determining the use as a photocatalyst, catalyst, or as ceramic membrane material. This transformation, achieved by increased temperature or pressure.

One of the important properties of the inorganic solid  $\text{TiO}_2$  nanomaterials is its photocatalytic activity, which are largely used as a photocatalyst owing to its beneficial characteristics which include high photocatalytic efficiency, physical and chemical stability, low cost and low toxicity. Moreover,  $\text{TiO}_2$  has suitable redox potential for photocatalytic  $\text{H}_2$  production or organic decomposition as shown in Figure 3.5, the redox potential for photogenerated holes is +2.53V versus the standard hydrogen electrode (SHE) in pH 7 aqueous solution. After reaction with water, these holes can produce hydroxyl radicals, whose redox potential is only slightly decreased and is in fact still more positive than that for ozone. The redox potential for conduction

band electrons  $-0.52$  V, which is negative enough to reduce dioxygen to superoxide or water to hydrogen. In addition to the wide energy band gap,  $\text{TiO}_2$  exhibits many other interesting properties, such as transparency to visible light, high refractive index and a low absorption coefficient. Anatase and rutile, the two principal polymorphs of  $\text{TiO}_2$ , are associated with energy band gap energies of 3.2 and 3.1 eV, respectively. It has been pointed out that the photodegradation reaction rate is much more rapid over anatase than in the case of rutile. This reaction rate is mainly affected by the crystalline state and textural properties such as surface area and particle size of  $\text{TiO}_2$  powder. However, these factors often vary in opposite ways, since a high degree of crystallinity is generally achieved through a high temperature thermal treatment leading to a reduction in the surface area. Thus, optimal conditions for the synthesis  $\text{TiO}_2$  nanomaterials have been sought to obtain materials of high photoactivity. Since photocatalytic reactions are generally studied in aqueous suspensions, problems arise from the formation of hard agglomerates through the diffusion of reactants and products as well as light absorption. The crystal structure of  $\text{TiO}_2$  greatly affects its photocatalytic activity. Amorphous  $\text{TiO}_2$  seldom displays photocatalytic activity due to the presence of nonbridging oxygen atoms in the bulk  $\text{TiO}_2$ , whose Ti-O atomic arrangement defects could act as the recombination centers of the photogenerated electron-hole pairs. The photocatalytic performance of  $\text{TiO}_2$  depends not only on its bulk energy band structure but also, to a large extent, on its surface properties. The larger the surface area per mass, the higher the photocatalytic activity. So that, development of preparation method to obtain high both specific surface area and crystallinity is necessary for high photocatalytic activity.



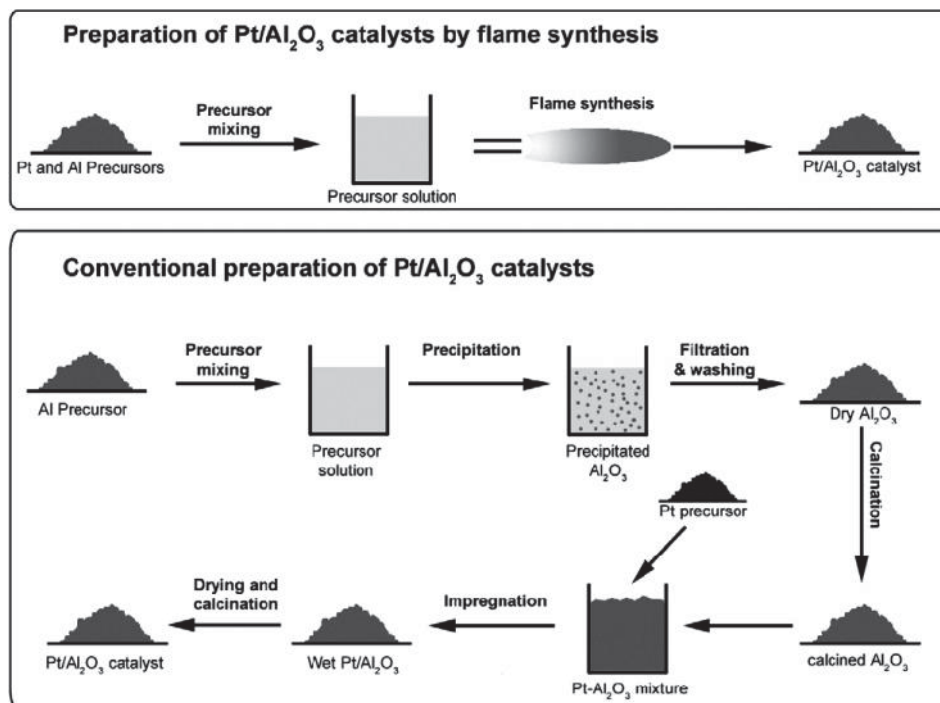
**Figure 3.5** Schematic diagram showing the potentials for various redox processes occurring on the  $\text{TiO}_2$  surface at pH 7 [10]

### 3.5 Flame spray pyrolysis [31,32,36,70]

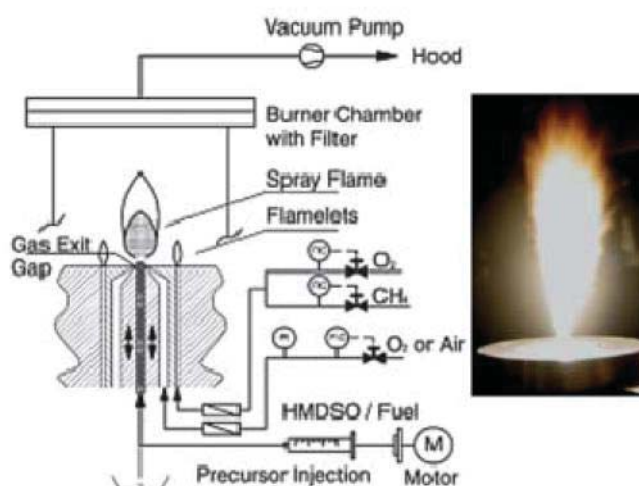
Flame aerosol synthesis of catalytically active nanoparticles can give access to novel structures and materials with closely controlled characteristics such as particle size, Crystal structure, morphology, shape and phase composition, that are not available through conventional techniques. Today, mostly wet-phase techniques are used for the industrial manufacturing of catalysts: incipient wetness impregnation, sol-gel, precipitation, grafting and solid-state reactions, just to name a few, are batch processes requiring several after-treatment steps, such as filtration, drying and calcination. Figure 3.6 shows a schematic of wet and flame processes for the synthesis of  $\text{Pt}/\text{Al}_2\text{O}_3$  catalysts. Moreover, flame technology is a scalable, continuous and well-established method for the production of nanoparticles in large quantities. For decades it has been used for the large-scale manufacture of simple commodities, such as carbon black, pigmentary titania, wave guide preforms, fumed silica and alumina. In presently, depending on the precursor state (aqueous-based, solventbased, vapour) and combustion conditions, flame aerosol syntheses fall into three general categories: (a)

vapour-fedaerosol flame synthesis (VAFS) where a metal precursor is supplied in the form of vapour, (b) flame-assisted spray pyrolysis (FASP) where precursor is supplied in the state of low combustion enthalpy solution (<50% of total combustion energy) usually in aqueous solvent, and because of this, its combustion needs to be assisted by an external hydrogen or hydrocarbon flame and (c) flame spray pyrolysis (FSP) where the precursor is also in liquid form, but with significantly higher combustion enthalpy (>50% of total energy of combustion), usually in an organic solvent. FSP is the youngest of the three processes, has important technological elements such as self sustaining flame, usage of liquid feeds and less volatile precursors, proven scalability, high temperature flames and large temperature gradients. It is also the most heavily explored in recent years for the production of complex and functional nanomaterials. Some of the most notable applications are in the areas of catalysis, optics and photonics, sensors, health care, magnetic materials, electroceramics for fuel cells and composite materials. A key feature in the use of FSP as a convenient tool in synthesising these nanomaterials is the ability to up scale its production, while closely preserving its tailored properties.

In the FSP process, the metal precursor is a combustible liquid that is sprayed and ignited, resulting in produce nanoparticles. The organic precursor solution is dispersed by gas (O<sub>2</sub> or air) convection through a nozzle forming a fine spray which is ignited as show in Figure 3.7.

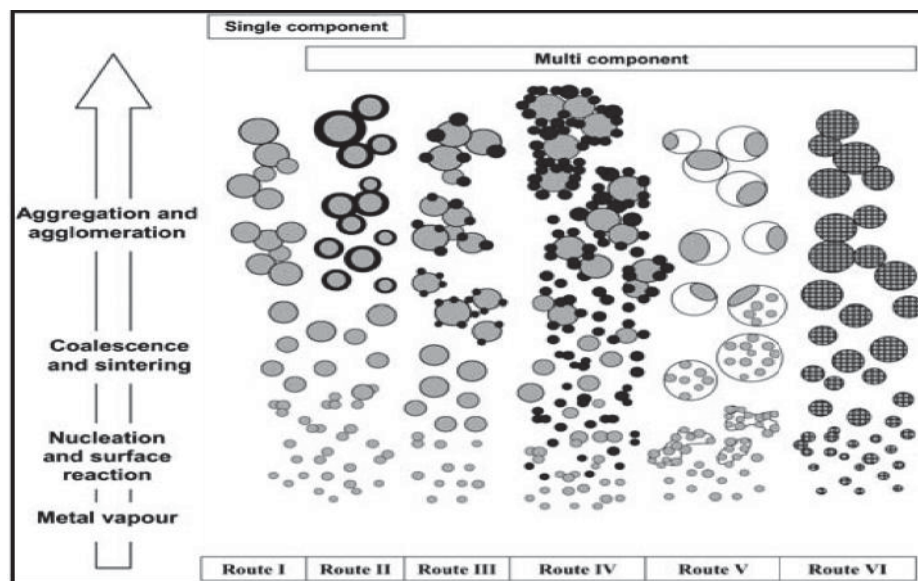


**Figure 3.6** Comparison of conventional wet-phase and flame methods for the synthesis of Pt/Al<sub>2</sub>O<sub>3</sub> catalyst [31]



**Figure 3.7** Schematic of configurations used for the synthesis of catalysts by FSP [36]

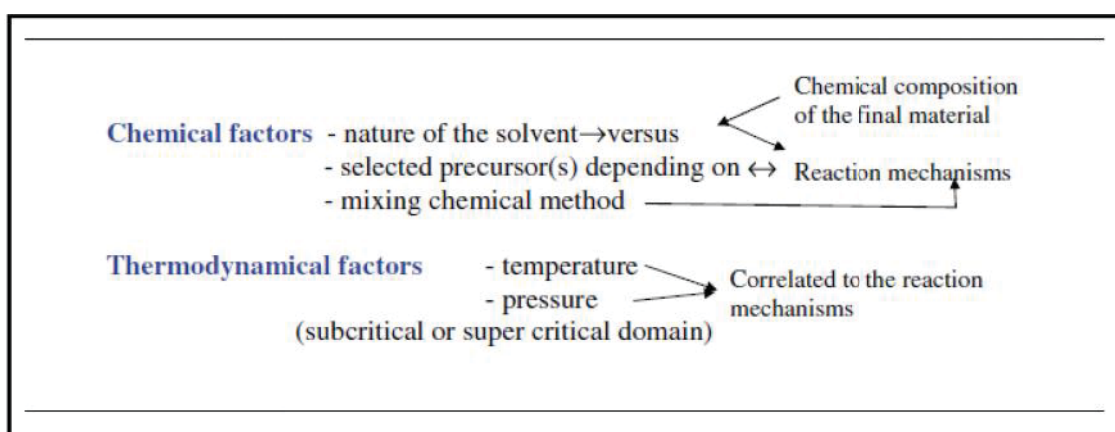
The metal precursors evaporate in this spray flame and are combusted. Particles are then formed by nucleation from the gas phase. The process features short residence times (a few milliseconds) and high maximum process temperatures (up to 3000 K). Afterwards, mention the different categories of particle configurations that may form in the gas-to-particle route in FSP. These particles form in sequential stages of: (1) precursor spray evaporation/decomposition forming metal vapor; (2) nucleation as a result of super saturation; (3) growth by coalescence and sintering; and (4) particles aggregation (forming hard agglomerates by chemical bonds) and agglomeration (forming soft agglomerates by mainly physical bonds) as shown in Figure 3.8. Furthermore, Figure 3.9 shows the different synthesis parameters influencing the particle formation and thus the final characteristics of the material.



**Figure 3.8** The formation of different particle configurations via the gas-to-particle mechanism for single and multi-component systems in FSP process [36]



solvothermal treatment could be used to control grain size, particle morphology, crystalline phase and surface chemistry by regulating sol composition, reaction temperature, pressure, nature of solvent, additives, and aging time. In particular, the particles prepared by this method have larger surface area, smaller particle size, and more stable than those obtained by other methods such as the sol–gel one. Main two types of parameters are involved in solvothermal reactions as show in Figure 3.10.



**Figure 3.10** Main factors governing solvothermal processes [24]

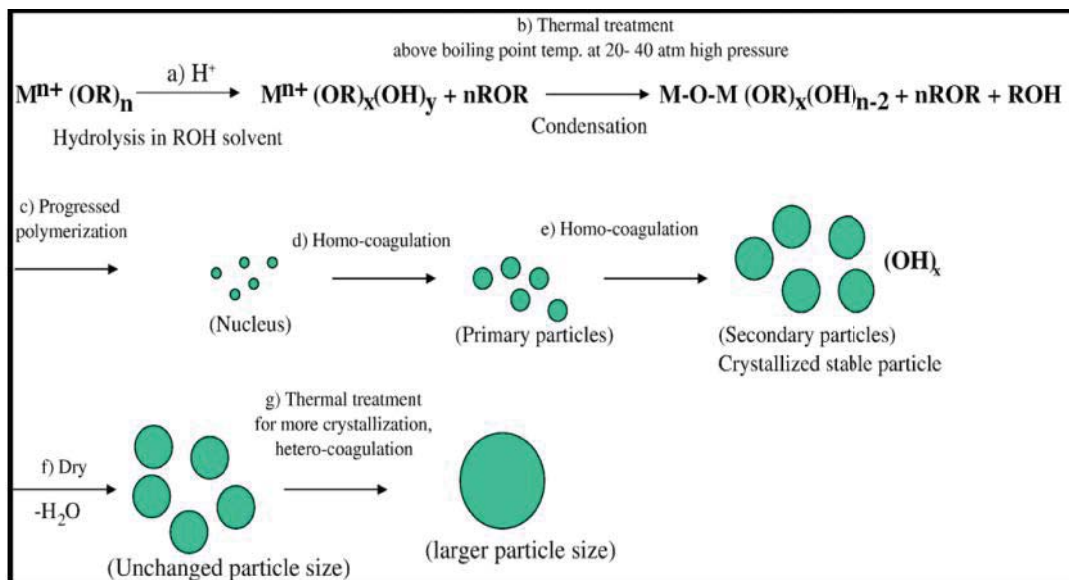
Chemical parameters:

Two different parameters can be taken into account (i) the nature of the reagents and (ii) the nature of the solvent. The chemical composition of the precursors must be appropriated to that of the target-materials. In addition, the concentration of the precursors seems to play a role on the control of the shape of nanocrystallites resulting of a solvothermal process. The interactions between reagents and solvent play an important role in the solvothermal reactions. Consequently the nature of the solvent can act on the reactivity and the morphology of the resulting crystallites. The physicochemical properties of the selected solvent can also play an important role for orienting the structural form of the final material.

The thermodynamical parameters:

These parameters are: temperature, pressure and the reaction time. The solvothermal reactions are mainly developed in mild temperature conditions: ( $T < 400^{\circ}\text{C}$ ). Temperature and pressure improving in the major cases the solubility, the increase of such parameters induces an enhancement of the precursors concentration into the solvent and then favours the growing process (in particular in the preparation of micro- or nanocrystallites). The brief analysis of the main factors governing solvothermal reactions underlines that the nature of the selected solvent plays a key role, in particular for controlling the chemical mechanisms involved in the solvothermal reactions.

This technique was introduced into the field of ceramic materials synthesis, such as  $\text{ZrO}_2$ ,  $\text{Ce}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3$ . This method could be employed as an alternative to calcinations for the promotion of crystallization under mild temperature. The detailed solvothermal method is illustrated in Figure 3.11, and allows for the crystallization of the metal oxide nucleus during thermal treatment at high temperature and pressure (c). The crystallized metal oxide nucleus then develops into the primary particle via homocoagulation (d, e), at which point, the excess solvents partially suppress further crystal growth. As a result, the particle size produced via the solvothermal method is finer than that of the sol-gel method. Finally, the crystallized metaloxide particles are attained without the calcination step (f). To prepare the required structure, the excess thermal treatment steps has to be consistent (g). Unlike the solvothermal method, the sol-gel method moved directly from b) to f) via a heterogeneous coagulation step. This method can control the grain size, particle morphology, crystalline phase and surface chemistry under various sol compositions, reaction temperatures, pressures, solvent species, additives and aging time. In particular, the particles prepared using the solvothermal method have been reported to be more stable, have a larger surface area and smaller particle size compared to those obtained using other methods, such as the sol-gel method.



**Figure 3.11** Expected mechanism for the synthesis of particles using the solvothermal method [71]

## CHAPTER 4

### EXPERIMENTS

#### 4.1 Chemicals

The chemicals were used in the Au modified TiO<sub>2</sub> photocatalyst preparation are all analytical grades as listed in Table 4.1. It is noted that specification of these chemicals about physical properties is exhibited later in Appendix A.

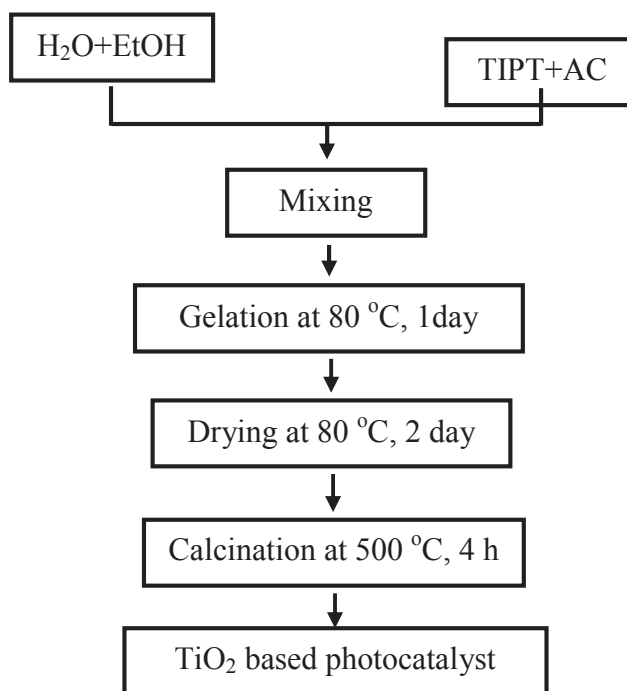
**Table 4.1** The details of chemicals used in the photocatalyst preparation

Chemicals	Formula	Grade	Manufacture
Tetraisopropyl orthotitanate (TIPT)	(C <sub>3</sub> H <sub>7</sub> O) <sub>4</sub> Ti	≥ 98%	Merck Schuchardt OHG, Germany
Hydrogen tetrachloroauratetrihydrate	HAuCl <sub>4</sub> .3H <sub>2</sub> O	99.99%	Sigma-Aldrich Chemie GmbH, Germany
Formic acid	HCOOH	90%	Ajax Finechem Pty Ltd
Methanol	CH <sub>3</sub> OH	99.9%	J.T. Baker
Ethanol	CH <sub>3</sub> CH <sub>2</sub> OH	99.9%	J.T. Baker
Acetylacetone	C <sub>5</sub> H <sub>8</sub> O <sub>2</sub>	99%	Merck Schuchardt OHG, Germany
1-Butanol (BN)	CH <sub>3</sub> (CH <sub>2</sub> ) <sub>3</sub> OH	99.8%	Sigma-Aldrich Chemie GmbH, Germany
Ethylene Glycol (EG)	HOCH <sub>2</sub> CH <sub>2</sub> OH	99%	J.T. Baker
1,4-Butanediol (BD)	HO(CH <sub>2</sub> ) <sub>4</sub> OH	99%	Sigma-Aldrich Chemie GmbH, Germany
<i>n</i> -Pentane (PT)	C <sub>5</sub> H <sub>12</sub>	≥ 99%	Sigma-Aldrich Chemie GmbH, Germany
Xylene (XL)	C <sub>8</sub> H <sub>10</sub>	99.0%	Panreac Guimica S.A.U.

Chemicals	Formula	Grade	Manufacture
<i>n</i> -Cyclohexane (CHX)	C <sub>6</sub> H <sub>12</sub>	99.5%	Sigma-Aldrich Chemie GmbH, Germany
<i>n</i> -Heptane (HT)	C <sub>7</sub> H <sub>16</sub>	99%	Sigma-Aldrich Chemie GmbH, Germany
Toulene (TE)	C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	≥ 99.9%	Merck Schuchardt OHG, Germany
Octane (OT)	C <sub>8</sub> H <sub>18</sub>	≥ 99.5%	Sigma-Aldrich Chemie GmbH, Germany

## 4.2 TiO<sub>2</sub> based photocatalyst preparation

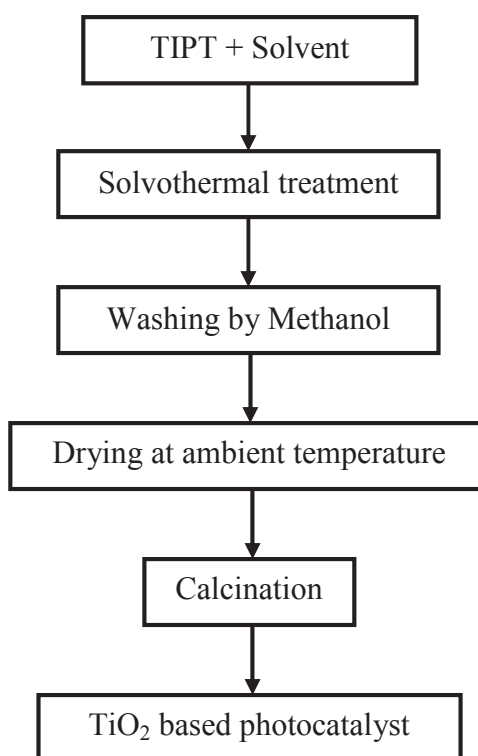
### 4.2.1 TiO<sub>2</sub> preparation by sol-gel method



**Figure 4.1** Schematic of the TiO<sub>2</sub> based photocatalyst synthesis procedure by sol-gel method

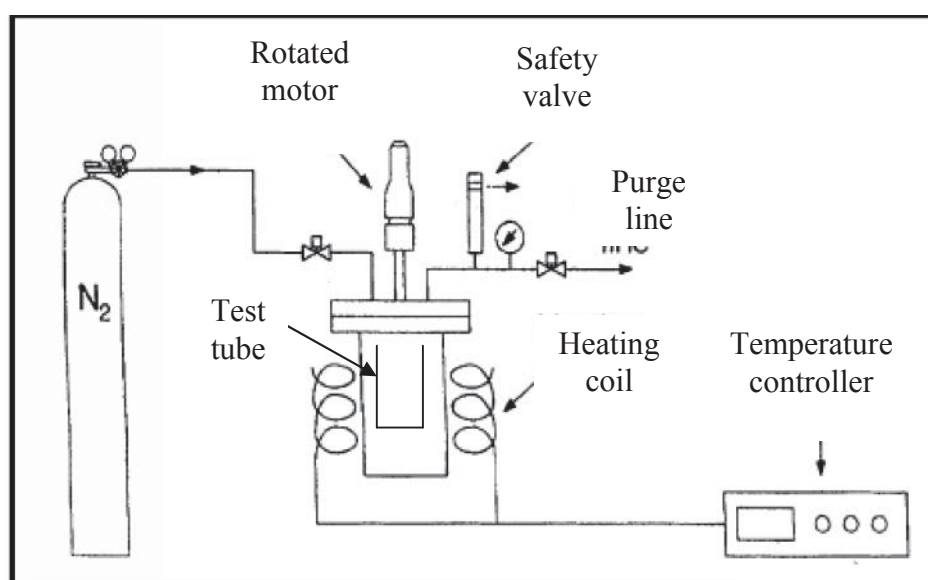
Acetylacetone (ACA) is first added into tetraisopropyl orthotitanate (TIPT) at an equimolar, and the mixed solution is then allowed to cool to room. Afterwards, it is added to solution of water and ethanol with continuously stirring at room temperature to obtain a clear solution. Then, the both solution is mixed to obtain a clear yellow solution while stirring continuously at room temperature. The resulting mixture is kept at 80°C for 1 day to obtain complete gel formation and the resulting gel is dried at 80°C for 2 day. Finally, the obtained zero gel (dried residue) is calcined at 500 ° for 4 h with heating rates of 10 °C/min to remove the impurity to yield the TiO<sub>2</sub> nanocrystal photocatalyst. The schematic diagram of the synthesis procedure is shown in Figure 4.1.

#### 4.2.2 TiO<sub>2</sub> preparation by solvothermal method



**Figure 4.2** Schematic of the TiO<sub>2</sub> based photocatalyst synthesis procedure by solvothermal method

The preparation of the TiO<sub>2</sub> photocatalysts by solvothermal method is shown in Figure 4.2. TIPT is dissolved in organic solvent in a test tube, which was then placed in a 300 cm<sup>3</sup> autoclave as shown in Figure 4.3. The gap between the test tube and the autoclave wall is filled with 30 cm<sup>3</sup> of the same solvent use in the test tube. The autoclave is purged completely by nitrogen before heating up to the desired temperature at a rate of 2.5 °C/min and the vessel is rotated at 300 rpm during the solvothermal reaction. Autogeneous pressure during the reaction gradually increase as the temperature is raised. After the prescribed temperature is reached, the temperature is held constant for desired period of time, and then cool down to room temperature. The resultant product is obtained by centrifugation, washed three times with methanol and dried in air at room temperature. For thermal treatment, the synthesized product is calcined in air with flow rate 30 cm<sup>3</sup>/min and a heating rate of 10 °C/min for 4 h to yield the TiO<sub>2</sub> based photocatalyst. Table 4.2 showed condition in studied parameter for preparation of TiO<sub>2</sub> by this method such as solvent type, temperature of preparation, concentration of TIPT and temperature of calcination.



**Figure 4.3** Autoclave used to synthesis TiO<sub>2</sub>.

**Table 4.2** Condition of studied parameter in TiO<sub>2</sub> prepared by solvothermal

Studied parameter	Condition			
	Solvent type	Solvothermal temperature (°C)	TIPT (TIPT ml:100 ml solvent)	Calcined Temperature (°C)
Solvent type	BN, EG, BD, PT, CHX, HT, TE, OT, XL	300	10	500
Temperature of preparation	CHX	250	10	500
	HT	300		
	TE			
Concentration of Ti	HT	300	5	500
			10	
			15	
			20	
Temperature of calcination	HT	300	10	300
				400
				500
				600

### 4.2.3 TiO<sub>2</sub> preparation by flame spray pyrolysis method

TIPT is used as the feed precursor. It is dissolved in organic solvent to obtain a clear solution. In a typical run, the liquid precursor is fed in the center of a methane/oxygen flame by syringe pump and dispersed by oxygen (Thai Industrial Gas Co., Ltd.) forming a fine spray. The precursor feed rate is 5 ml/min. The pressure drop at the capillary tip is kept constant at 1.5 atm by adjusting the orifice gap area at the nozzle. The photocatalyst powder is collected on a glass microfiber filter (Whatman) with the aid of a vacuum pump.

## 4.3 Au cocatalyst modification

### 4.3.1 Au cocatalyst modification by impregnation

The incipient impregnation procedure are as follows:

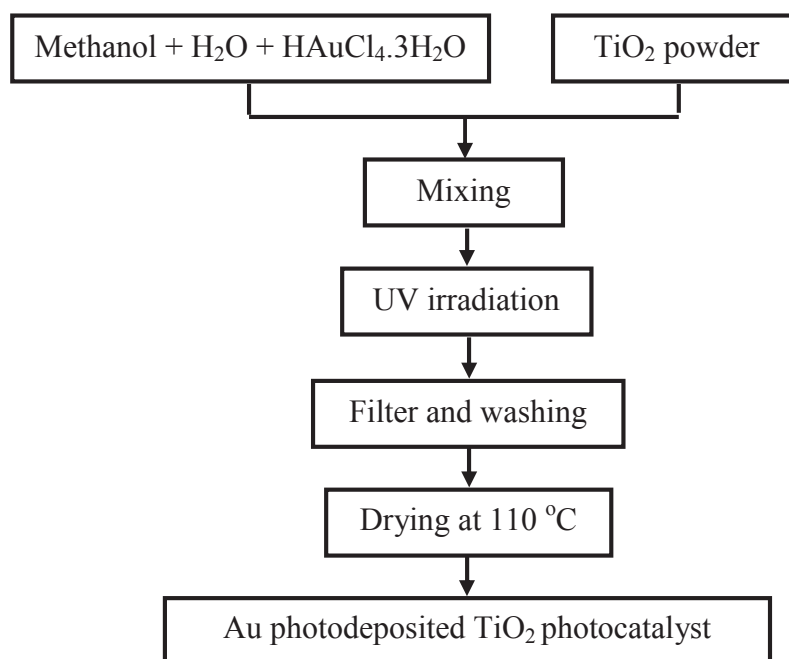
1. Dissolve appropriate amount of H<sub>2</sub>AuCl<sub>4</sub> in distilled water.
2. TiO<sub>2</sub> powder is impregnated with the Au solution.
3. The impregnated sample is kept at room temperature for 6 h.
4. The sample is dried in oven at 110 °C overnight.
5. The dried sample is reduced with H<sub>2</sub> at 200 °C for 4 h.

Finally, the Au modified TiO<sub>2</sub> photocatalyst is obtained.

### 4.3.2 Au cocatalyst modification by photodeposition

In the photodeposition method, Au metal loaded on TiO<sub>2</sub> is prepared by photoreducing Au<sup>3+</sup> ions to Au metal on the TiO<sub>2</sub> surface according to the following steps shown in Figure 4.4. First, TiO<sub>2</sub> powder is suspended in aqueous solution of 0.5 vol.% methanol and the required amount of H<sub>2</sub>AuCl<sub>4</sub>·3H<sub>2</sub>O. The mixture is then

irradiated with UV light (Hg lamp, TUV 11 W PL-S, Phillip), washed with distilled water and then dried at 110 °C for 12 h.



**Figure 4.4** Schematic of synthesis procedure of Au photodeposition over TiO<sub>2</sub>

### 4.3.3 Au cocatalyst modification by doping

In the case of the Au doped TiO<sub>2</sub> based photocatalyst is synthesized by add HAuCl<sub>4</sub> precursor simultaneously TiO<sub>2</sub> based photocatalyst preparation.

## 4.4 Photocatalyst characterization

### 4.4.1 X-Ray diffraction (XRD)

The crystalline size, the structure and purity of a photocatalyst can be analyzed using X-ray diffraction analysis. The refraction or diffraction of the X-rays is monitored at various angles with respect to the primary beam X-ray diffraction analysis using an X-ray refractometer, with Ni-filtered Cu K $\alpha$  radiation in the 2 $\theta$  range of 20 to 80° using the continuous scanning mode at a rate of 2°C min<sup>-1</sup> and operating conditions of 30 kV and 15 mA. The crystallite size is calculated from Scherrer's equation as described by eq 4.1.

$$D = \frac{K\lambda}{\beta \cos\theta} \quad 4.1$$

where  $K$  is the Scherrer constant (0.89),  $\lambda$  is the wavelength of the X-ray radiation (0.15418 nm for CuK $\alpha$ ),  $\beta$  is the full width at half maximum (FWHM) of the diffraction peak measured at 2 $\theta$ , and  $\theta$  is the diffraction angle. Fraction of rutile in the product is calculated according to the following eq 4.2 [22]:

$$\% \text{Rutile} = \frac{1}{((A/R) \times 0.884) + 1} \times 100 \quad 4.2$$

where A and B are the peak area for the major anatase and rutile phase, respectively.

### 4.4.2 N<sub>2</sub> physisorption

The surface area, average pore size diameter and pore size distribution are determined by N<sub>2</sub> physisorption using the BET BELSORP II (surface area and porosity analyzer). The catalyst is firstly pretreated in inert helium gas flow of 50 ml/min at 150 °C for 3 h to remove water bound to the particle surface from air moisture. After cooling down to the ambient temperature, the weight of dried sample is collected. Sample cell is installed to the adsorption part which has liquid nitrogen in dewar. The requisite data are input to the software before the measurement. During the measurement the sample

cell connects to vacuum port is dipped in liquid nitrogen. The volume of N<sub>2</sub> is measured at different partial pressure at of N<sub>2</sub> -196 °C.

#### **4.4.3 Transmission electron microscopy (TEM)**

The crystalline image is determined using transmission electron spectroscopy operates at 80 kV. The sample is dispersed in ethanol to obtain the uniform dispersion of sample. A drop of liquid is deposited onto a copper mesh sample grid that supports a holey carbon support film. The grid is resting on a filter paper and is allowed to dry for several minutes before being moved. The scans are done many times in different areas as much as possible until the good representative image for all areas is obtained.

#### **4.4.4 Inductively coupled plasma (ICP)**

The actual amount of Au in synthesis of photocatalyst are determined by inductively coupled plasma (ICP).

#### **4.4.5 UV-vis diffuse reflectance spectra (UV-vis DRS)**

Diffuse reflectance spectra of the samples are measured at room temperature with a UV-visible spectrophotometer in the range 200-800 nm. Afterwards, the diffuse reflectance spectra are analyzed to estimate the band gap wavelength (E<sub>g</sub>, nm) by using theKabelkae-Munk function (F(R)), as expressed by the following eq 4.3:

$$F(R) = \frac{(1 - R)^2}{2R} \quad 4.3$$

where  $R$  is the ratio of the reflected light intensity to the reflected light intensity of the reference and the band gap energy ( $E_g$ ) was then determined by using the following eq 4.4:

$$E_g = \frac{1240}{\lambda_g} \quad 4.4$$

#### 4.4.6 H<sub>2</sub> Chemisorption

H<sub>2</sub> chemisorption was used to determine a number of gold metal atoms on the photocatalyst surface and overall gold dispersion. The total hydrogen consumption was calculated from the number of injection of a known volume. N<sub>2</sub> and H<sub>2</sub> were used as a carrier gas and a adsorbent gas, respectively. 0.05 g of a photocatalyst sample was placed in a quartz tubular reactor. Under N<sub>2</sub> atmosphere at a flow rate of 30 ml/min, the photocatalyst sample was heated up to 150 °C at a heating rate of 10 °C/min and held for 2 h at this temperature in order to remove adsorbed water on surface. Afterwards, the system was cooled down to room temperature by N<sub>2</sub> at a flow rate of 30 ml/min. At this temperature, the photocatalyst sample was ready to be measure the metal active sites. 20 µl of the purity H<sub>2</sub> gas was injected into the injection port to adsorb on the metal surface of the catalyst sample. Injection of H<sub>2</sub> was continuously repeated until saturation. This situation was occurred when an obtained chromatogram area of any injection, after adsorption of the H<sub>2</sub> pulse in the first injection had proceeded, was kept nearly constant compared with that of the former injection.

#### 4.4.6 Photoluminescence spectroscopy (PL)

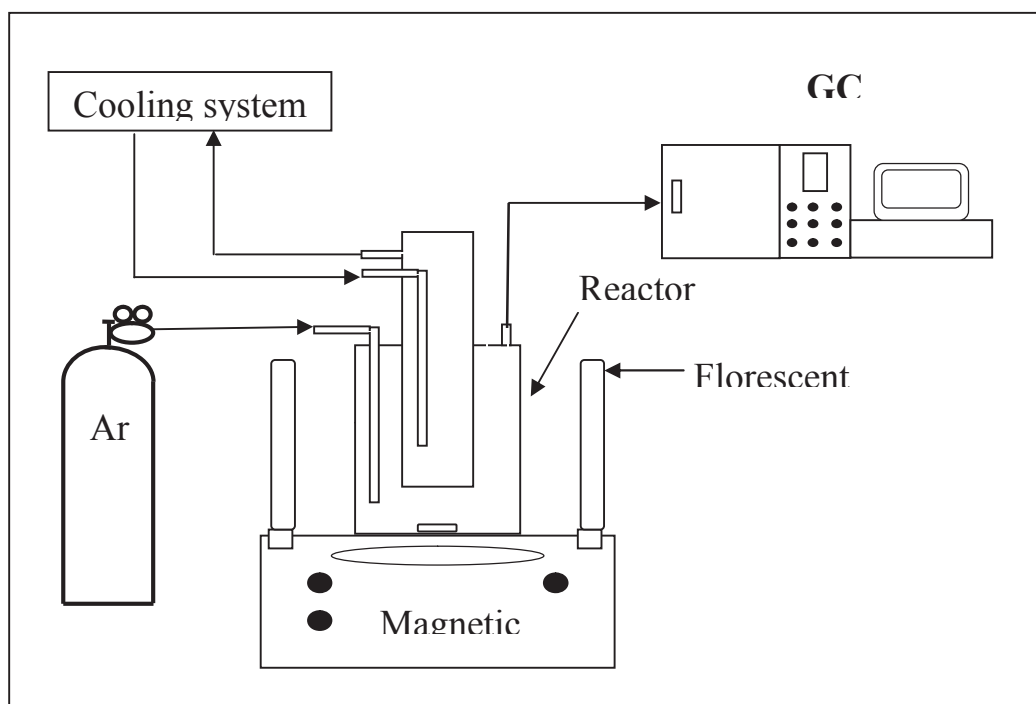
The photoluminescence spectroscopy was used to studied recombination rate of photogenerated e<sup>-</sup>/h<sup>+</sup> pairs. The photoluminescence emission spectra were measured at room temperature in range 350-750 nm with excited at 325 nm.

#### 4.5 Photocatalytic H<sub>2</sub> production testing

The photocatalytic reactions are carried out in a gas circulation system and are performed in an outer-irradiation and air-tight Pyrex glass reactor with a total volume of 750 cm<sup>3</sup>. The reaction temperature is controlled by using a water-cooling system. A set of 176 W fluorescent lamps (16 lamps, 11 W PL-S 2P, Phillip) are employed as simulated sunlight source with total irradiance of about 90 W.m<sup>-2</sup>. Spectrum of the lamp consisted of fluorescent emission predominantly in the visible region along with a UV contribution of about 3% [27]. In a typical experiment, each photocatalyst sample is suspended in 0.1 M formic acid aqueous solution (250 ml) with 0.1 g/l. Prior to the reaction testing, the suspension is left in the dark while simultaneously being thoroughly deaerated by Ar gas (UHP, Thai Industrial Gas Ltd) bubbling for 20 min, and then adjusts flow Ar with 30 cm<sup>3</sup>/min before the suspension is irradiated by turning on the lamps and the reaction temperature is controlled at 30°C. After every 30 min, hydrogen gas is analyzed by an online gas chromatograph equipped with a thermal conductivity detector (TCD), as show in Figure 4.5. The operating conditions for TCD gas chromatograph instrument is shown in the Table 4.3.

**Table 4.3** The operating conditions of TCD gas chromatograph for the photocatalytic H<sub>2</sub> production testing

<b>Gas chromatograph</b>	<b>Shimadzu GC-14B</b>
Detector	TCD
Column	Unibead C
Carrier gas	Ar (UHP)
Carrier gas flow	30 ml/min
Injector temperature	150 °C
Detector temperature	150 °C
Column temperature	40 °C
Analysis gas	H <sub>2</sub> , CO, CO <sub>2</sub>



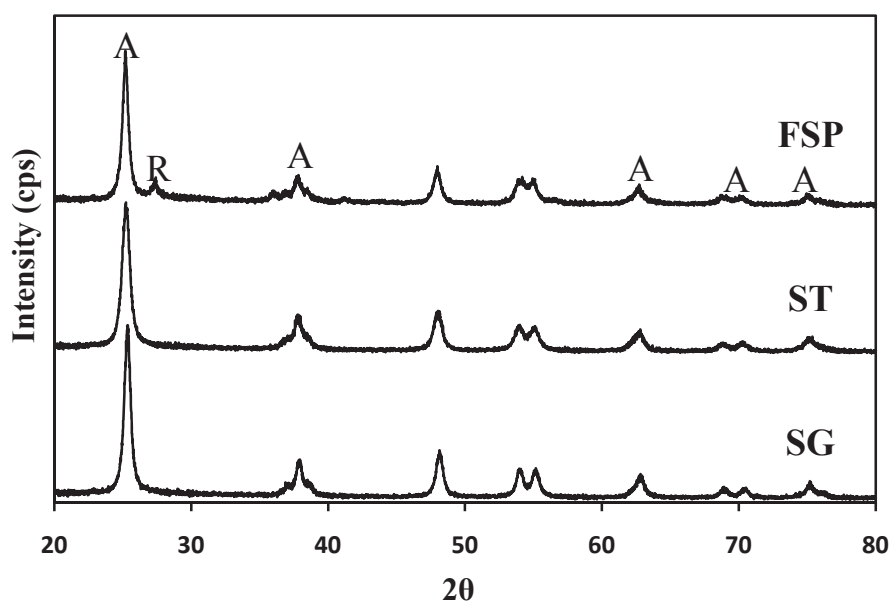
**Figure 4.5** The photocatalytic hydrogen production system used in this study

## CHAPTER 5

### RESULTS AND DISCUSSION

#### 5.1 Photocatalyst characterization

##### 5.1.1 Effect of TiO<sub>2</sub> preparation method



**Figure 5.1** XRD pattern of TiO<sub>2</sub> based photocatalysts prepared by flame spray pyrolysis (FSP), sol-gel (SG) and solvothermal (ST) (A: anatase, R: rutile)

Nanosized TiO<sub>2</sub> particles were successfully prepared by using sol-gel, solvothermal (using 1,4-Butanediol as solvent) and flame spray pyrolysis methods. The

XRD patterns of them, as shown in Figure 5.1. TiO<sub>2</sub> prepared by SG and ST show the dominant peaks at 2θ of about 25.2, 37.9, 48.3, 53.8, 62.7, 68.9 and 75.3, which correspond to the indices of (101), (103), (200), (105), (213), (116) and (107) planes [50], respectively, reveal the crystalline structure of the pure anatase phase. However, TiO<sub>2</sub> prepared by FSP shows two additional very low intense peaks corresponding to rutile phase at 2θ of about 27.5, which correspond to the indices of (110) plane [50] with approximately 5% rutile content, besides that of the major anatase phase.

**Table 5.1** Physical properties of TiO<sub>2</sub> prepared by SG, ST and FSP

Preparation method	Phase <sup>a</sup> content (wt.%)	d <sub>XRD</sub> <sup>b</sup> (nm)	d <sub>TEM</sub> <sup>c</sup> (nm)	Relative <sup>d</sup> crystallinity	S <sub>BET</sub> <sup>e</sup> (m <sup>2</sup> /g)	S <sub>XRD</sub> <sup>f</sup> (m <sup>2</sup> /g)	S <sub>BET</sub> / S <sub>XRD</sub>	Pore <sup>e</sup> diameter (nm)	Pore <sup>e</sup> volume (cm <sup>3</sup> /g)
SG	A (100)	14.4	14.8	1.32	21.8	109.1	0.20	3.8	0.0591
ST	A (100)	11.8	12.1	1.00*	89.3	94.3	0.95	21.7	0.3716
FSP	A (86.8) R (13.2)	16.4 17.0	17.1	1.00	116.9	132.8	0.88	11.8	0.3856
P25	-	-	-	-	61.8	-	-	28.0	0.3626

a) Calculated according to equation proposed by W. Payakgul et al. [22]

b) Base on XRD line broadening

c) Average particle size from TEM

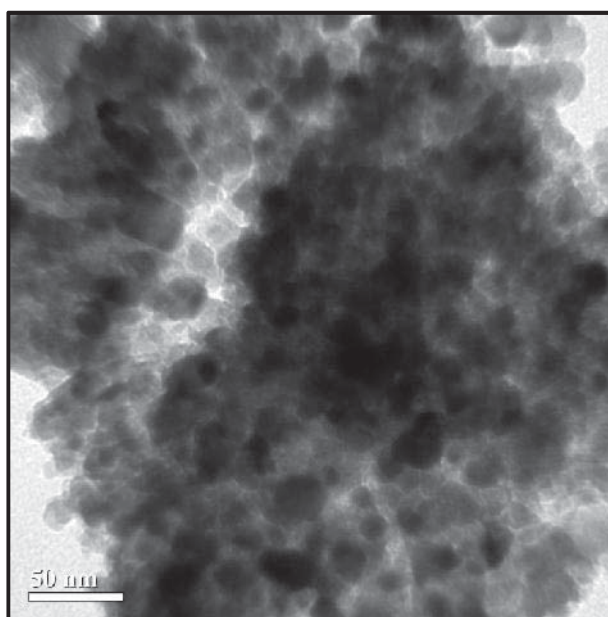
d) Comparison of height main peak of anatase by using ST as reference

e) N<sub>2</sub> physisorption analysis

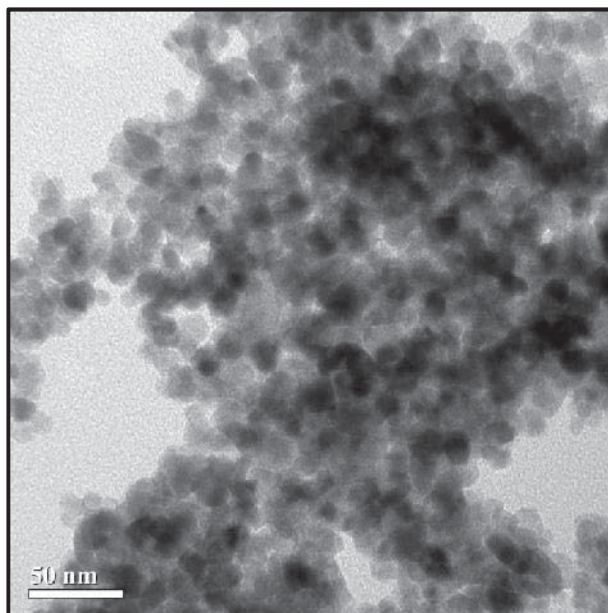
f) Calculated surface area assuming that the particles are nonporous spheres ( $S=6/\rho d_{XRD}$ )

The physical properties of TiO<sub>2</sub> prepared by SG, ST and FSP methods were showed in Table 5.1. It can be seen that the crystallite sizes of TiO<sub>2</sub> particles calculated from the Scherrer equation decreases in the order FSP >SG >ST. However, the

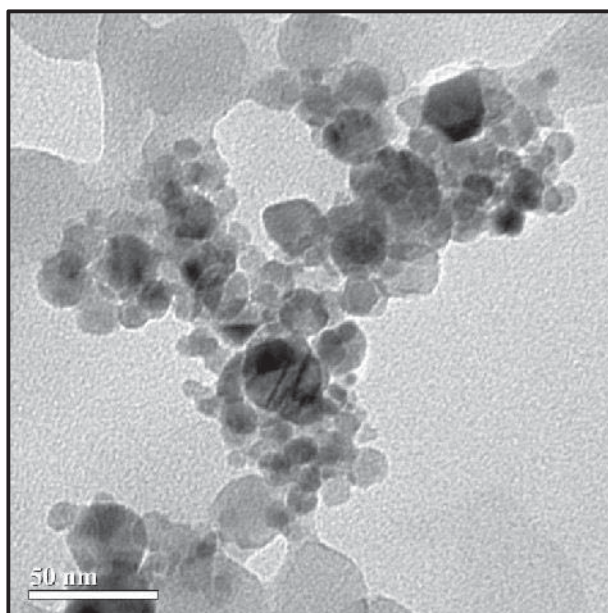
crystallinity of  $\text{TiO}_2$  preparation by SG exhibited higher crystallinity than  $\text{TiO}_2$  preparation by ST and FSP, while both ST and FSP provided same crystallinity. TEM was performed to evaluate the morphology and particle size of  $\text{TiO}_2$  particles. TEM image of  $\text{TiO}_2$  particles prepared by SG, ST and FSP are shown in Figure 5.4-5.6, respectively, they exhibited spherical particles.  $\text{TiO}_2$  prepared by SG and ST exhibit narrow particle size distribution. On the other hand,  $\text{TiO}_2$  prepared by FSP shows wide particle size distribution. Moreover, they can be seen that average particle size from TEM image, which agree with the crystallite sizes of  $\text{TiO}_2$  particles calculated from the Scherrer equation as shown in Table 5.1. Hence, each primary particle observed by TEM is a nanosized single crystal  $\text{TiO}_2$  [22].



**Figure 5.2** TEM image of  $\text{TiO}_2$  preparation by SG



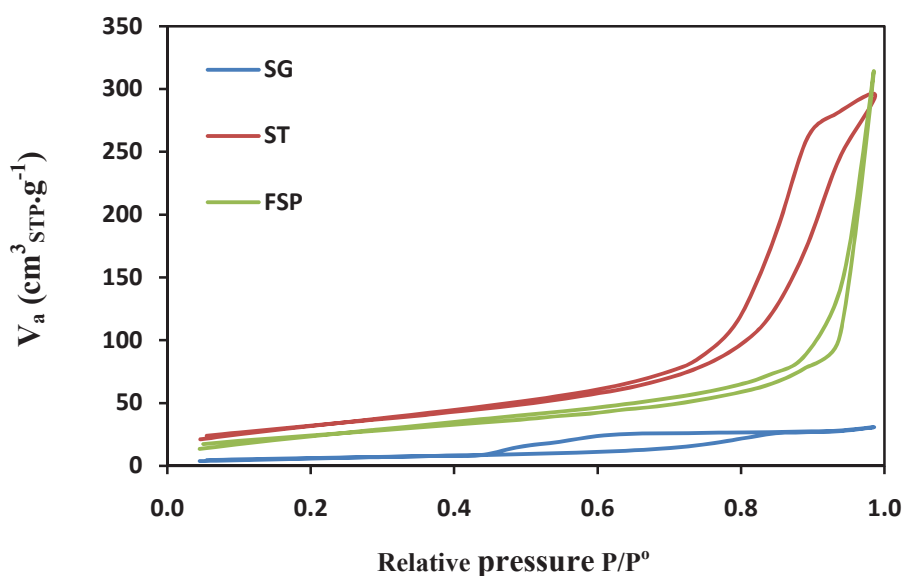
**Figure 5.3** TEM image of TiO<sub>2</sub> preparation by ST



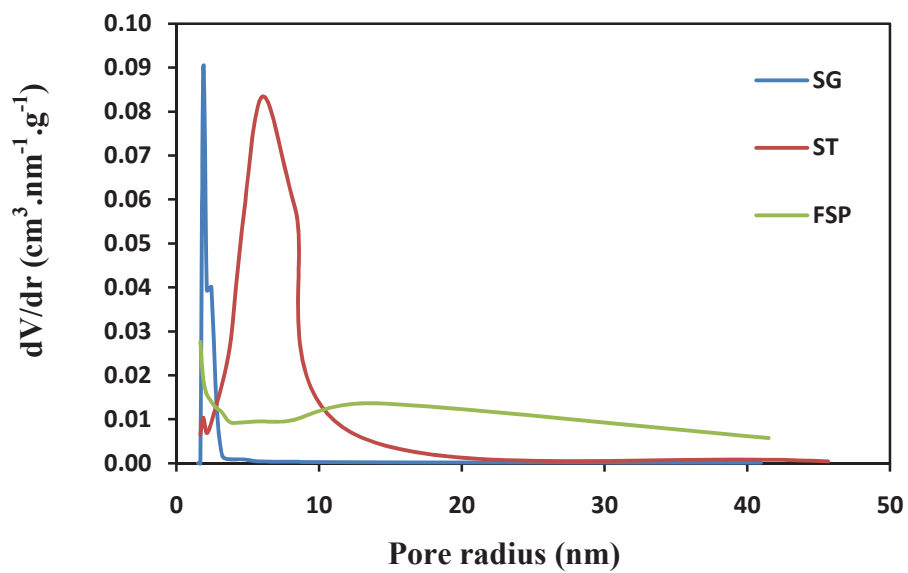
**Figure 5.4** TEM image of TiO<sub>2</sub> preparation by FSP

The BET surface area of all products decreases in the order  $ST > FSP > SG$ . Moreover, Table 5.1 also compares BET surface area ( $S_{BET}$ ) measured by  $N_2$  physisorption and the surface area calculated from a crystallite size ( $S_{XRD}$ ), assume that the crystals are non-porous spheres. It is noticed that  $S_{BET}$  is smaller than  $S_{XRD}$  for all the preparation methods, W. Payakgul et al. [22] proposed that this behavior was the result from the agglomeration of  $TiO_2$  crystals. So that, the agglomeration of crystals increases in the order  $FSP > ST > SG$ , which agree with the TEM observation.  $N_2$  adsorption-desorption isotherm was used to verify the mesoposity of the studied photocatalysts sine the isotherm shape reveals the characteristics of powder structure, which consist of an assembly of numerous particles with large open packing [50]. Figure 5.2 shows  $N_2$  adsorption-desorption isotherm of  $TiO_2$  prepared by SG, ST and FSP, provided information related to the porous texture. The isotherm of  $TiO_2$  prepared by SG and ST reveal the typical IUPAC type IV pattern with the H2 hysteresis loop, characteristic of mesoporous materials (2-50 nm) [42]. A sharp increase in the adsorption volume of  $N_2$  was clearly observed and located in the relative partial pressure rang of 0.5-0.9. This sharp increase can be attributed to the capillary condensation of  $N_2$  inside the mesopores [50], it can be clearly seen from  $TiO_2$  prepared by SG method. However, hysteresis loop  $TiO_2$  prepared by ST method shift at relative high partial pressure than SG because of larger pore size, which according to pore size as shown in Figure 5.3. The isotherm of  $TiO_2$  prepared by FSP gave rise to hysteresis at relative high partial pressure and correspond to the IUPAC type II pattern [42], as shown in Figure 5.3. However, the  $N_2$  adsorption-desorption isotherm for  $TiO_2$  particles prepared by FSP correspond to the IUPAC type II pattern [42], as shown in Figure 5.2. It can be seen that they possess the non-mesoporous characteristic, due to the absence of both a distinct hysteresis loop and an adsorption plateau at very high relative pressure, indicating that there is no capillary condensation of  $N_2$  into the pores. The pore size distributions, as shown in Figure 5.3 are quite broad. This result show that the average pores of  $TiO_2$  obtained by FSP are quite spacious because their pore size distributions are not only present in the mesoporous region (mesopore size between 2 and 50 nm) but also mostly exist in the macroporous region (pore diameter  $>50$  nm), which it is quite typical for nanoparticles

obtained by FSP method that contained only large pore [77]. Furthermore, total pore volume of the TiO<sub>2</sub> products in Table 5.1 increases in the order SG >ST >FSP. This result is attributed to the agglomeration effect and crystallite size [27]. From these characterization results, it is evident that the TiO<sub>2</sub> products prepared by different method have different physical properties.

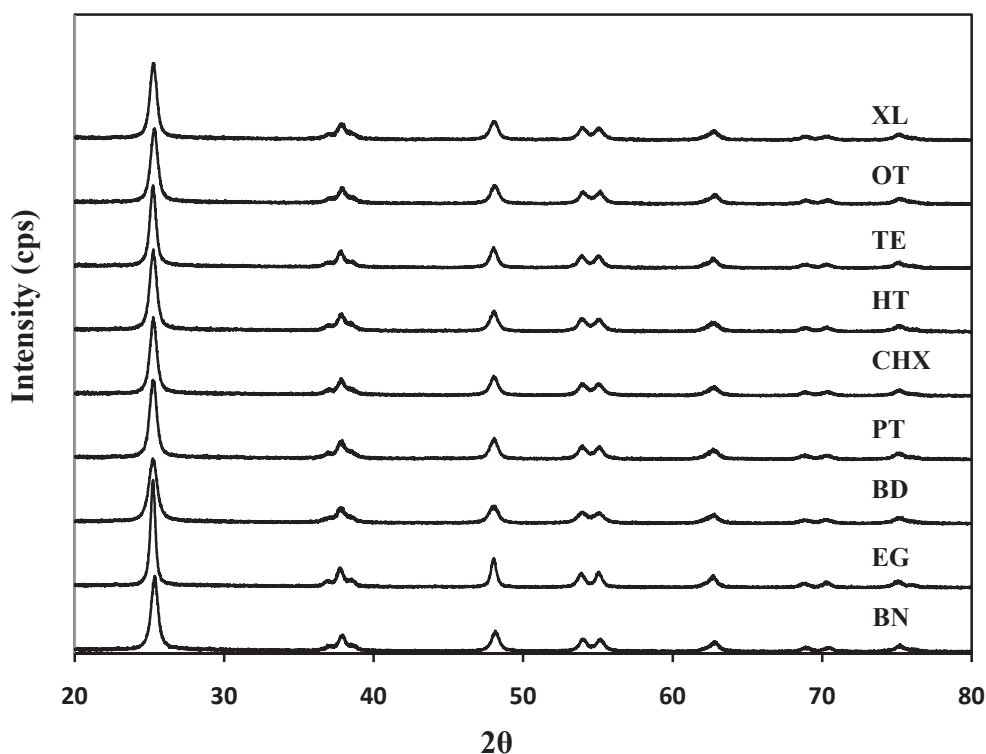


**Figure 5.5** N<sub>2</sub> adsorption/desorption isotherms of TiO<sub>2</sub> preparation by SG, ST and FSP



**Figure 5.6** Pore size distributions of TiO<sub>2</sub> preparation by SG, ST and FSP

### 5.1.2 Effect of solvent type in TiO<sub>2</sub> preparation by solvothermal



**Figure 5.7** XRD pattern of TiO<sub>2</sub> based photocatalysts prepared by ST with using different solvent

The solvents in this research can be divided two main groups, (1) –OH compound solvents, e.g. butanol (BN), ethylene glycol (EG) and 1,4-butanediol (BD) and (2) without –OH compound solvents, e.g. pentane (PT), cyclohexane (CHX), heptane (HT), toluene (TE), octane (OT) and xylene (XL). Generally, type of solvent used in solvothermal for catalyst preparation affect the phase composition extremely during the solvothermal preparation [25]. However, in the this research, all the TiO<sub>2</sub> products prepared by solvothermal method with studied solvents were indentified as anatase phase, as shown in Figure 5.7. Moreover, the effect of solvent type on physical properties of TiO<sub>2</sub> products such as crystallinity, crystallite size, specific surface area, pore size

diameter were shown in Table 5.2. In the polar solvents, the crystallinity increases in the order EG >BN >BD, which agree with polarity of solvent, because nanocrystalline anatase TiO<sub>2</sub> prepared in polar solvent crystallized directly from the solution [22]. Hence, polarity of solvent effect to crystallinity of TiO<sub>2</sub> product, high polarity solvent provided higher crystallinity than lower polarity solvent. On the other hand, the nonpolar solvents provided same crystallinity of TiO<sub>2</sub> products, which agree with polarity of solvent, because nanocrystalline anatase TiO<sub>2</sub> prepared in polar solvent crystallized directly from the solution [22]. Hence, polarity of solvent effect to crystallinity of TiO<sub>2</sub> product, high polarity solvent provided higher crystallinity than lower polarity solvent. On the other hand, crystallinity of TiO<sub>2</sub> prepared in nonpolar solvents were similar crystallinity because of similar polarity. In addition, when nonpolar solvent was used as reaction medium for solvothermal preparation of TiO<sub>2</sub>, amorphous product was initially formed in the solution and later transformed to anatase crystal via solid state reaction, which it opposite reaction in polar solvent.

Figure 5.8 show N<sub>2</sub> adsorption-desorption isotherm of TiO<sub>2</sub> prepared with using BN, EG and BD, provided information related to the porous texture. The isotherm of TiO<sub>2</sub> in using BN, EG and BD reveal characteristic of mesoporous materials with different shap of the hysteresis loop, it mean that this solvent provided shap of pore structure. Moreover, they gave different pore size distribution, BN gave narrow pore size distribution, while EG and BD gave wide pore size distribution as shown in Figure 5.10, because the number of –OH in the moleculer structure might be the factor that affect the TiO<sub>2</sub> formation. The isotherm of TiO<sub>2</sub> prepared using PT, CHX, HT, TE, OT and XL as solvents reveal similar the typical IUPAC type IV pattern as shown in Figure 5.9, since these solvents have no effect of –OH to direct crystalline formation, TiO<sub>2</sub> praticles were prepared by using these solvents may provided same pore size and similar pore size distribution as shown in Figure 5.11. So that, these characterization results, it is evident that the TiO<sub>2</sub> products prepared in different solvent type with solvothermal method have diffent physical properties of TiO<sub>2</sub> product.

**Table 5.2** Physical properties of TiO<sub>2</sub> prepared by ST with different solvent

Sovent type	Phase content <sup>a</sup> (wt.%)	$d_{XRD}^b$ (nm)	Relative <sup>c</sup> crystallinity	$S_{BET}^d$ (m <sup>2</sup> /g)	$S_{XRD}^e$ (m <sup>2</sup> /g)	$S_{BET}/S_{XRD}$	Pore <sup>d</sup> diameter (nm)	Pore <sup>d</sup> volume (cm <sup>3</sup> /g)
BN	A (100)	14.5	1.08	53.2	108.0	0.49	6.4	0.1178
EG	A (100)	20.1	1.66	59.2	77.8	0.76	11.5	0.2085
BD	A (100)	11.8	1.00*	116.9	132.8	0.88	11.8	0.3856
PT	A (100)	14.0	1.24	80.7	112.2	0.72	9.3	0.2483
CHX	A (100)	14.0	1.24	93.2	111.7	0.83	9.2	0.3020
HT	A (100)	14.3	1.27	100.1	109.8	0.90	9.3	0.4027
TE	A (100)	14.6	1.22	104.6	107.2	0.98	9.4	0.3384
OT	A (100)	13.9	1.20	81.6	112.3	0.73	9.4	0.2583
TE	A (100)	14.2	1.22	79.6	100.2	0.72	9.3	0.3408

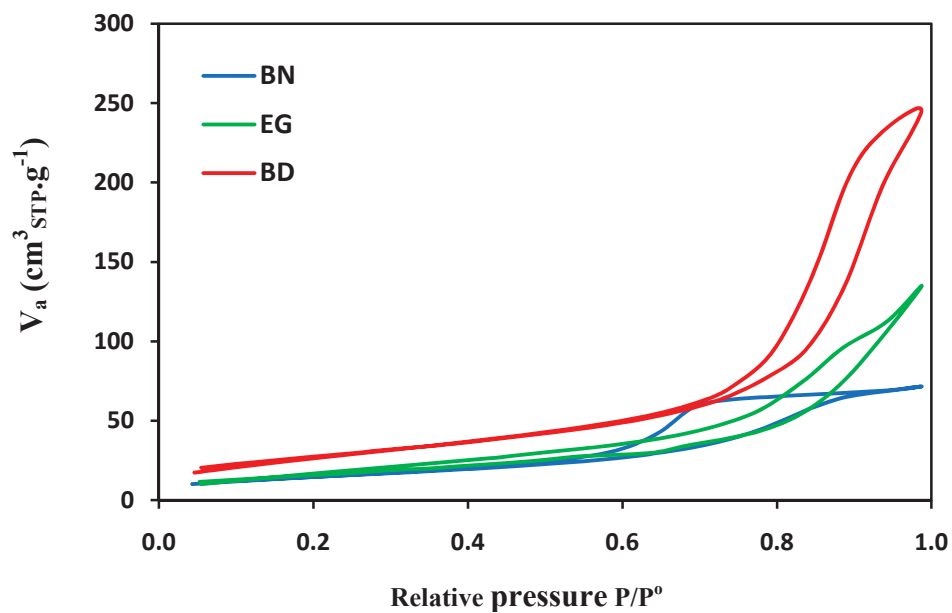
a) Calculated according to equation proposed by W. Payakgul et al. [22]

b) Base on XRD line broadening

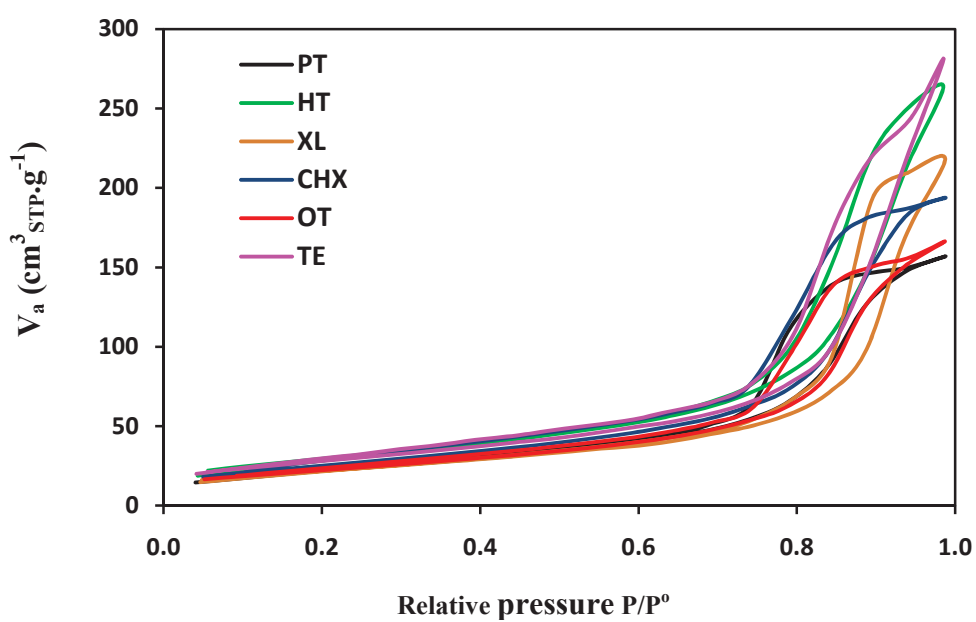
c) Comparison of height main peak of anatase by using ST as reference

d) N<sub>2</sub> physisorption analysis

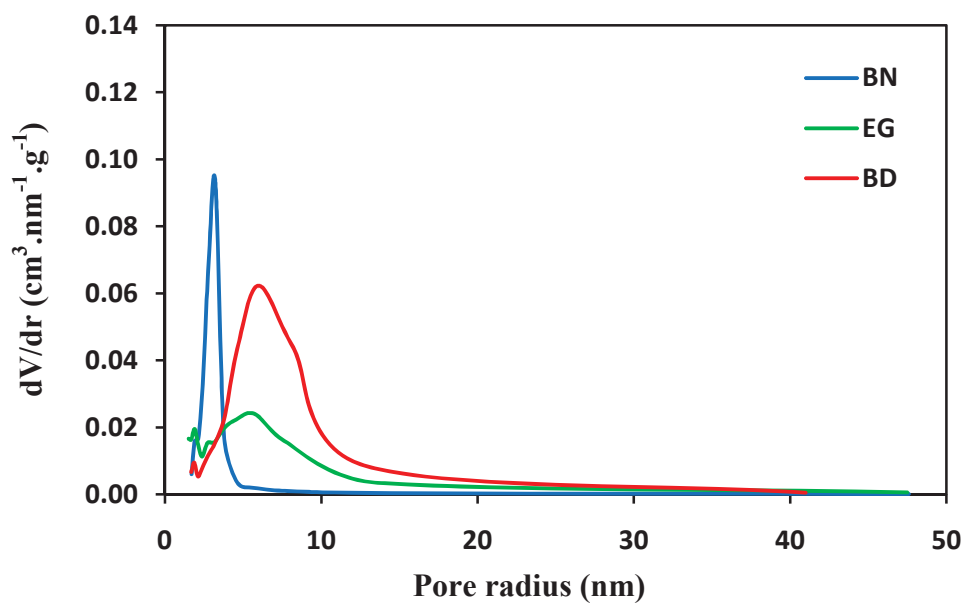
e) Calculated surface area assuming that the particles are nonporous spheres ( $S=6/\rho d_{XRD}$ )



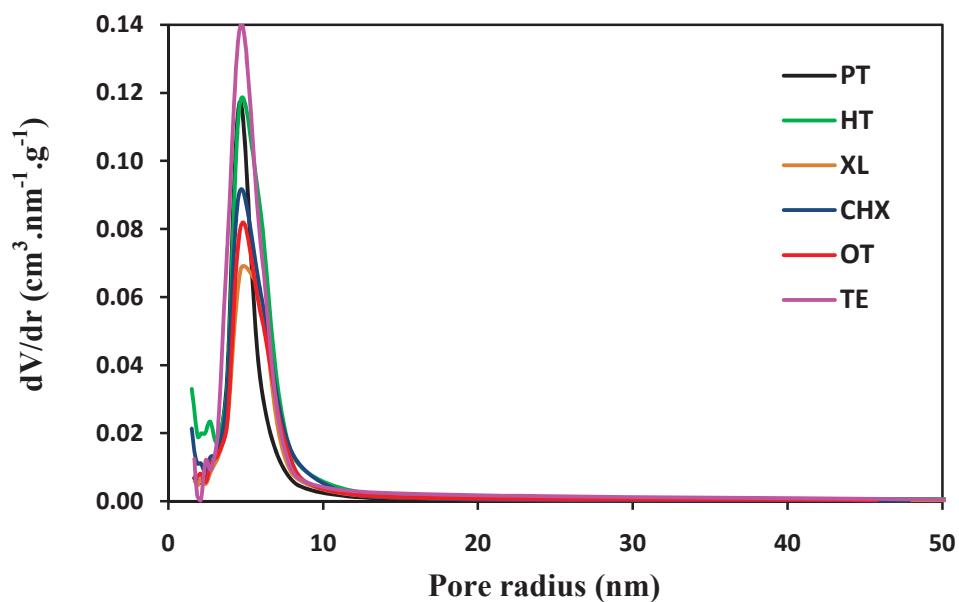
**Figure 5.8** N<sub>2</sub> adsorption/desorption isotherms of TiO<sub>2</sub> preparation by ST with using -OH compound solvent



**Figure 5.9** N<sub>2</sub> adsorption/desorption isotherms of TiO<sub>2</sub> preparation by ST with without -OH compound solvent

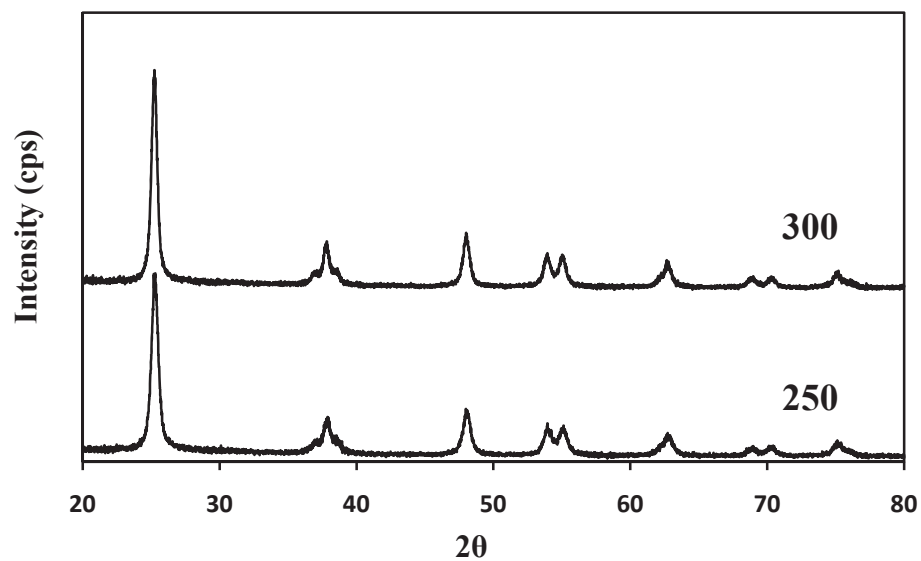


**Figure 5.10** Pore size distribution of TiO<sub>2</sub> preparation by ST with using -OH compound solvent

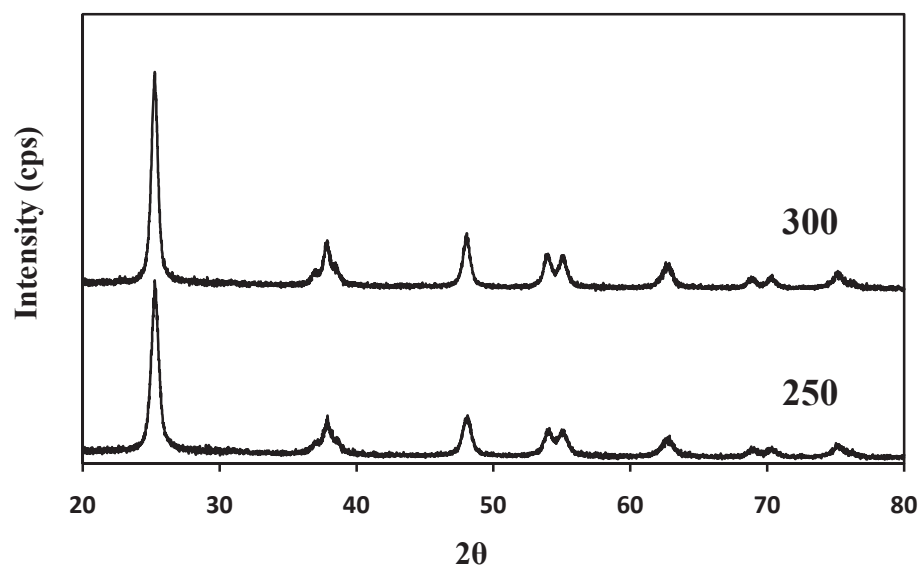


**Figure 5.11** Pore size distribution of TiO<sub>2</sub> preparation by ST with using without -OH compound solvent

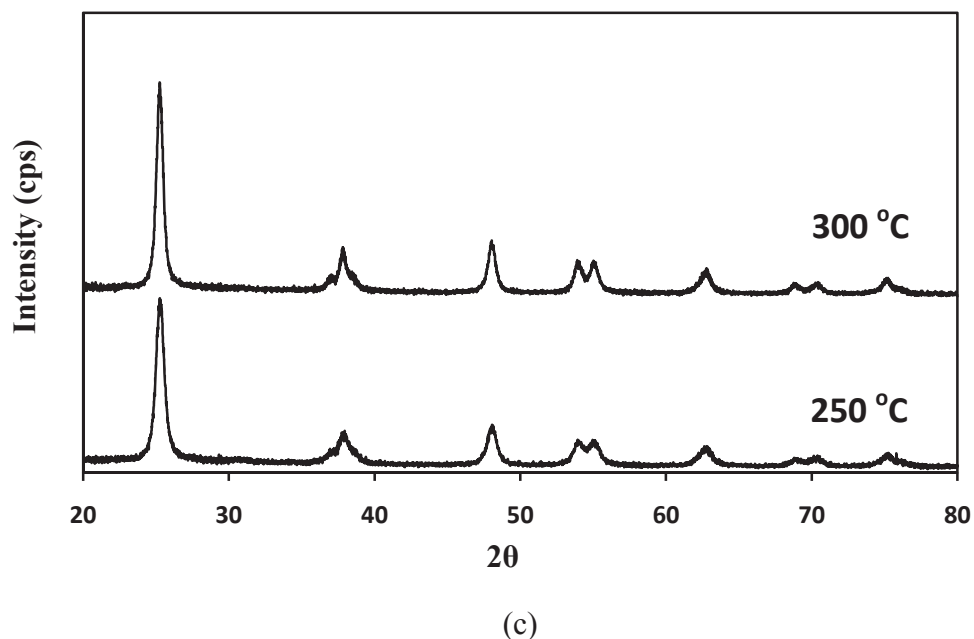
### 5.1.3 Effect of temperature in TiO<sub>2</sub> preparation by solvothermal



(a)



(b)



**Figure 5.12** XRD patterns of TiO<sub>2</sub> based photocatalysts prepared by ST at 250 °C and 300 °C in CHX (a), HT (b) and TE (c) solvent

Further investigation of the solvothermal reaction was conducted by varying the solvothermal temperature at 200, 250 and 300 °C, respectively. It is found that the solvothermal reaction temperature of 200 °C is too low to form any TiO<sub>2</sub> particles for these all studied solvents, such as cyclohexane (CHX), heptane (HT) and toluene (TE). The solvothermal reaction in these solvents is suggested that amorphous product initially precipitates from the solution, then the solid state transformation from the amorphous product to anatase TiO<sub>2</sub> occurring during subsequent heating period [22]. Figure 5.12 depicts the XRD patterns of the TiO<sub>2</sub> powders derived from the solvothermal method at 250 and 300 °C in CHX, HT and TE, respectively. As can be seen, the diffraction peaks of the anatase phase for all products become stronger and sharper upon enhancing the solvothermal temperature, indicating the improved crystallinity of TiO<sub>2</sub> products, it can be seen in Table 5.3.

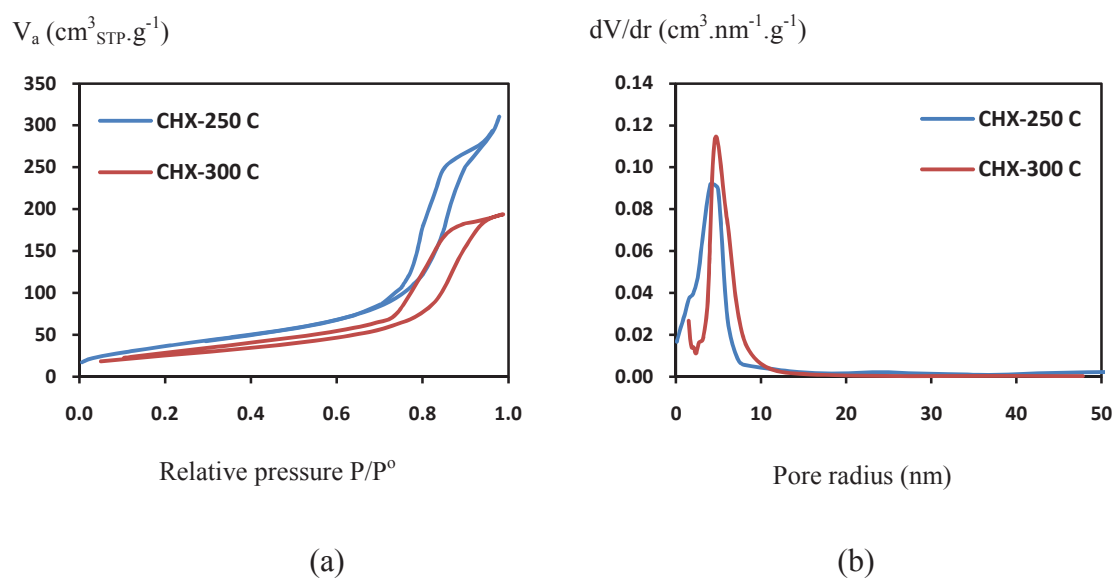
**Table 5.3** Physical properties of TiO<sub>2</sub> prepared by ST with different solvothermal temperature

Temperature (°C)	Solvent type	d <sub>XRD</sub> <sup>b</sup> (nm)	Relative <sup>c</sup> crystallinity	S <sub>BET</sub> <sup>d</sup> (m <sup>2</sup> /g)	S <sub>XRD</sub> <sup>e</sup> (m <sup>2</sup> /g)	S <sub>BET</sub> /S <sub>XRD</sub>	Pore <sup>d</sup> diameter (nm)	Pore <sup>d</sup> volume (cm <sup>3</sup> /g)
200	CHX					No product		
	HT					No product		
	TE					No product		
250	CHX	11.8	1.00	140.5	132.9	1.06	7.1	0.2765
	HT	12.2	1.09	138.3	128.0	1.02	7.9	0.2835
	TE	11.7	0.97	145.7	133.5	1.10	7.0	0.2931
300	CHX	14.1	1.25	93.2	111.7	0.83	9.2	0.3020
	HT	14.0	1.28	100.1	112.2	0.89	9.3	0.4027
	TE	14.6	1.23	103.6	107.2	0.97	9.4	0.3384

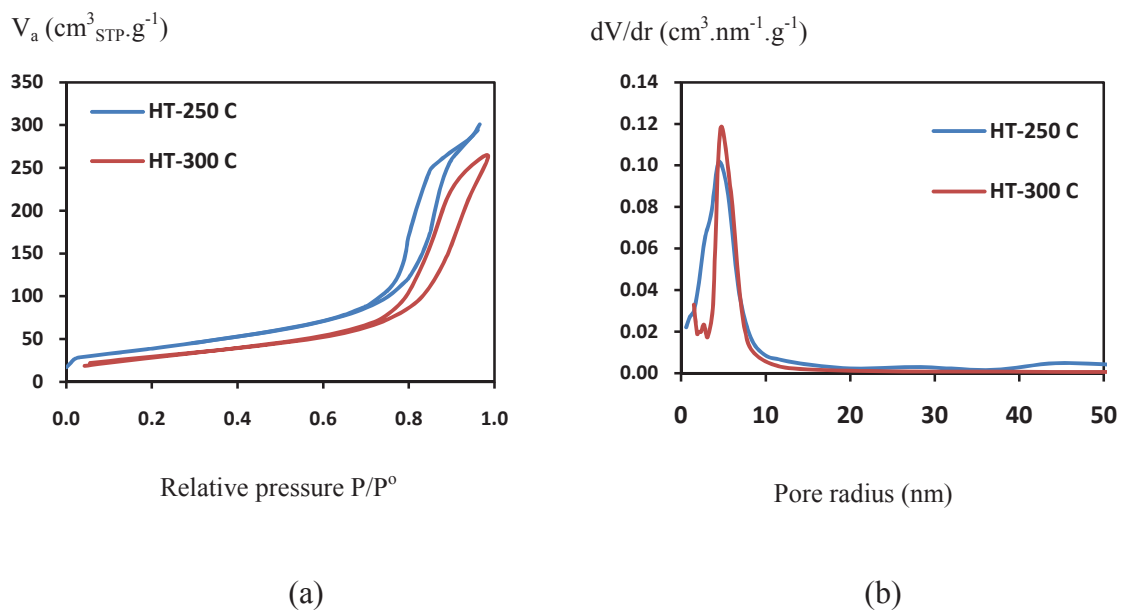
- Base on XRD line broadening
- Comparison of height main peak of anatase by using temperature at 250 °C in CHX as reference
- N<sub>2</sub> physisorption analysis
- Calculated surface area assuming that the particles are nonporous spheres ( $S=6/pd_{XRD}$ )

Moreover, it was found that TiO<sub>2</sub> particles preparation at 300 °C provided larger crystallite size and pore size than preparation at 250 °C as shown in Table 5.3, indicating that high temperature enhanced crystallite size, indicating the TiO<sub>2</sub> particles grow slightly with an increase temperature, resulting increase pore size. Table 5.3 also exhibited that S<sub>BET</sub> determined from N<sub>2</sub> physisorption was higher than S<sub>XRD</sub> calculated based on the crystallite size for all the TiO<sub>2</sub> particle prepared at 250 °C, it was proposed that this behavior was the result of an amorphous-like phase contaminated in the particles of TiO<sub>2</sub>[22]. While ,TiO<sub>2</sub> prepared at 300 °C, it was found that S<sub>BET</sub> was smaller than S<sub>XRD</sub> for all products, indicating that this temperature provide TiO<sub>2</sub> crystalline and agglomerate of TiO<sub>2</sub> crystals [22], resulting increase pore volume of product. Moreover,

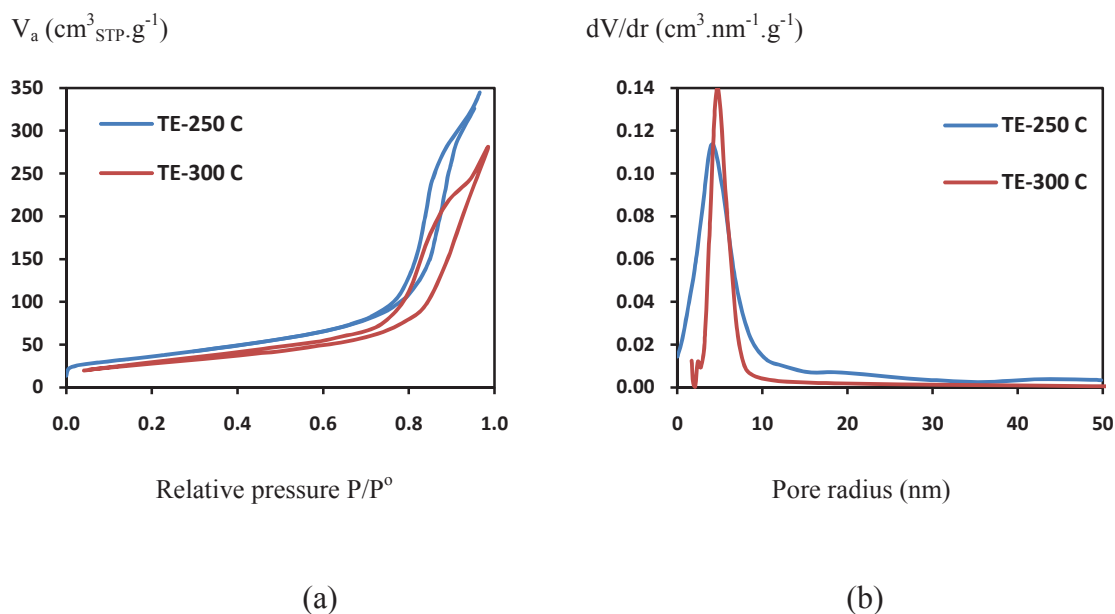
solvothermal temperature effect to porosity, it can be seen in Figure 5.13-5.15. Pore size distribution is narrow at high temperature.



**Figure 5.13**  $\text{N}_2$  adsorption/desorption isotherms (a) and pore size distribution (b) of  $\text{TiO}_2$  prepared by ST in CHX at 250 and 300 °C

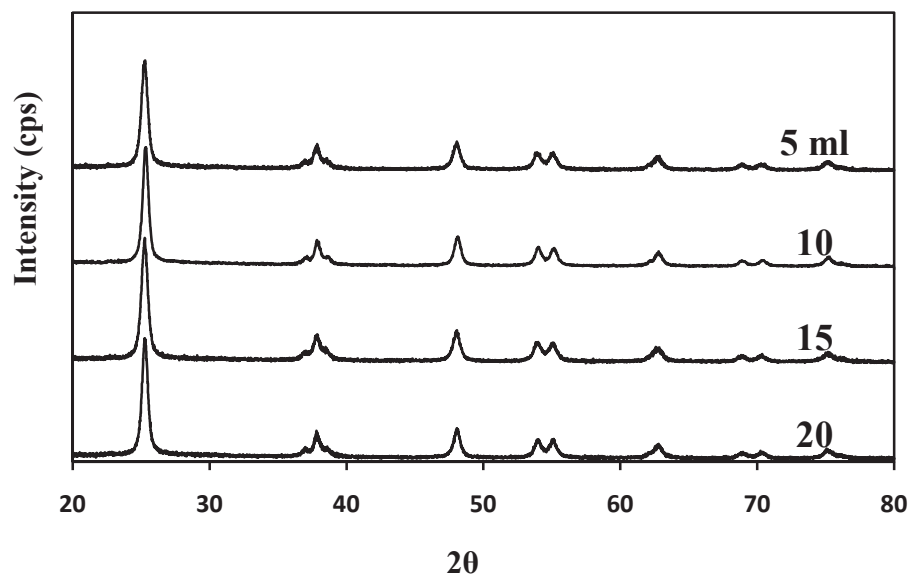


**Figure 5.14**  $N_2$  adsorption/desorption isotherms (a) and pore size distribution (b) of  $TiO_2$  prepared by ST in HT at 250 and 300 °C



**Figure 5.15**  $N_2$  adsorption/desorption isotherms (a) and pore size distribution (b) of  $TiO_2$  prepared by ST in TE at 250 and 300 °C

#### 5.1.4 Effect of Ti concentration in TiO<sub>2</sub> preparation by solvothermal



**Figure 5.16** XRD patterns of TiO<sub>2</sub> based photocatalysts prepared by ST with different TIPT concentration

The effect of amount of Ti was studied by varied TIPT as Ti precursor with 5, 10, 15 and 20 ml in 100 ml of heptane solvent. The XRD patterns of this effect are shown in Figure 5.16. It can be obviously seen that the phase structure of the particles is crystalline and exclusively of anatase phase with similar intensity of peak, indicating that all studied Ti concentration have similar crystallinity. The average crystallite size was calculated according to the Debye-Scherrer equation, as shown in Table 5.4. The average crystallite size of all the samples is about 14 nm. Therefore, it can be concluded that Ti concentration does not change the crystalline phase, crystallite size and crystallinity of products in this studied condition. BET surface areas of all the samples are given in Table 5.4. It can be seen that increasing Ti concentration resulted in decrease in the surface area of TiO<sub>2</sub> product. This result is supported from agglomeration of TiO<sub>2</sub>

particle, indicating that high Ti concentration promote agglomeration of TiO<sub>2</sub> particle, resulting in decrease the surface area. However, concentration of Ti does not effect to porosity of product, which was obtained from N<sub>2</sub> physisorption analysis as shown in Figure 5.17 and 5.18. The products with different Ti concentration are similar of N<sub>2</sub> adsorption-desorption isotherm and pore size distribution.

**Table 5.4** Physical properties of TiO<sub>2</sub> prepared by ST with different Ti concentration

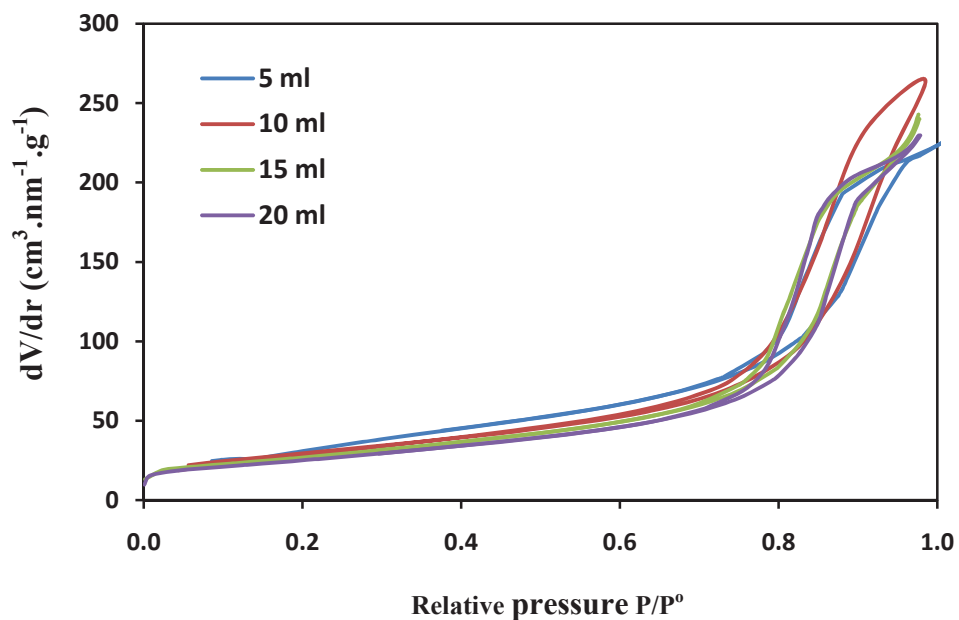
TIPT (ml)	d <sub>XRD</sub> <sup>a</sup> (nm)	Relative <sup>b</sup> crystallinity	S <sub>BET</sub> <sup>c</sup> (m <sup>2</sup> /g)	S <sub>XRD</sub> <sup>d</sup> (m <sup>2</sup> /g)	S <sub>BET</sub> / S <sub>XRD</sub>	Pore <sup>c</sup> diameter (nm)	Pore <sup>c</sup> volume (cm <sup>3</sup> /g)
5	13.8	1.00	112.3	113.4	0.99	9.3	0.2659
10	14.0	1.02	100.1	112.2	0.89	9.4	0.4027
15	14.6	1.05	78.0	107.2	0.73	9.4	0.3348
20	14.3	1.03	64.5	109.8	0.59	9.3	0.2836

a) Base on XRD line broadening

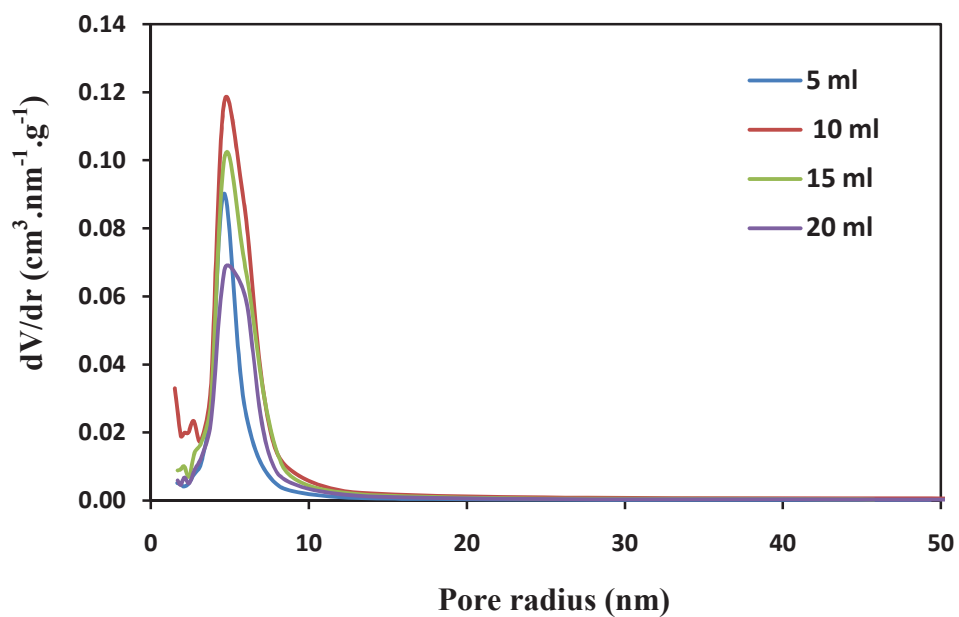
b) Comparison of height main peak of anatase by using 5 ml of TIPT as reference

c) N<sub>2</sub> physisorption analysis

d) Calculated surface area assuming that the particles are nonporous spheres ( $S=6/\rho d_{XRD}$ )

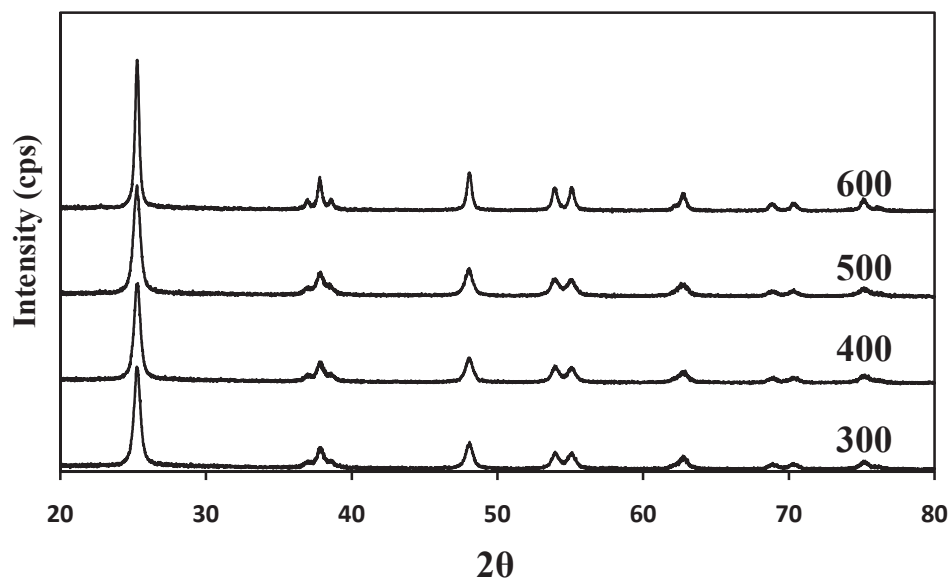


**Figure 5.17**  $N_2$  adsorption/desorption isotherms of  $TiO_2$  prepared by ST in HT with different amount of TIPT



**Figure 5.18** Pore size distribution of  $TiO_2$  prepared by ST in HT with different amount of TIPT

### 5.1.5 Effect of calcined temperature



**Figure 5.19** XRD patterns of TiO<sub>2</sub> based photocatalysts prepared by ST with different calcined temperature

Generally, calcination of synthesized TiO<sub>2</sub> particles in order to remove impurity, enhancing crystallinity and phase transformation of TiO<sub>2</sub>. Temperature calcination of this research was varied at 300, 400, 500 and 600 °C, respectively. However, the result of calcination in this work is found that at 300-600 °C does not change phase structure, all samples are anatase phase as shown in Figure 5.19. TiO<sub>2</sub> prepared by sol-gel method consisted small rutile phase at calcination temperature of 600 °C [50]. So that, TiO<sub>2</sub> prepared by solvothermal method provide stability of anatase phase, which according to W. Payakgul et al. [22], they prepared TiO<sub>2</sub> particles by solvothermal method in toluene. Moreover, in the range of 300-500 °C was also found that crystallinity and crystallite size are unchanged, indicating that increasing temperature do not effect in increasing crystallinity and crystallite size, it is explained that crystallinity

and crystallite size are carried out in preparation of TiO<sub>2</sub> by solvothermal step. On the other hand, at 600 °C clearly enhance crystallinity and crystallite size. This result indicates that the temperature effect on enhancing of crystallinity and crystallite size of TiO<sub>2</sub> crystals because temperature of calcination rearrang in TiO<sub>2</sub> crystals and promote sintering of TiO<sub>2</sub> crystal, resulting in improving of crystallinity and crystallite size, repectively as shown in Table 5.5. The BET surface area and porosity of TiO<sub>2</sub> products with calcination at 300-600 °C are given in Table 5.5. It can be seen that surface area and pore size increases in the order at 300 °C until 500 °C because of impurity removing. Calcinnation at 600 °C carried out sintering of TiO<sub>2</sub> crystals, resulting of surface area decreasing. However, N<sub>2</sub> adsorption-desorption isotherm in Figure 5.20 and pore size distribution in figure 5.21 of all samples show similar feature, indicating that the pore structure is similar in different temperature of calcination.

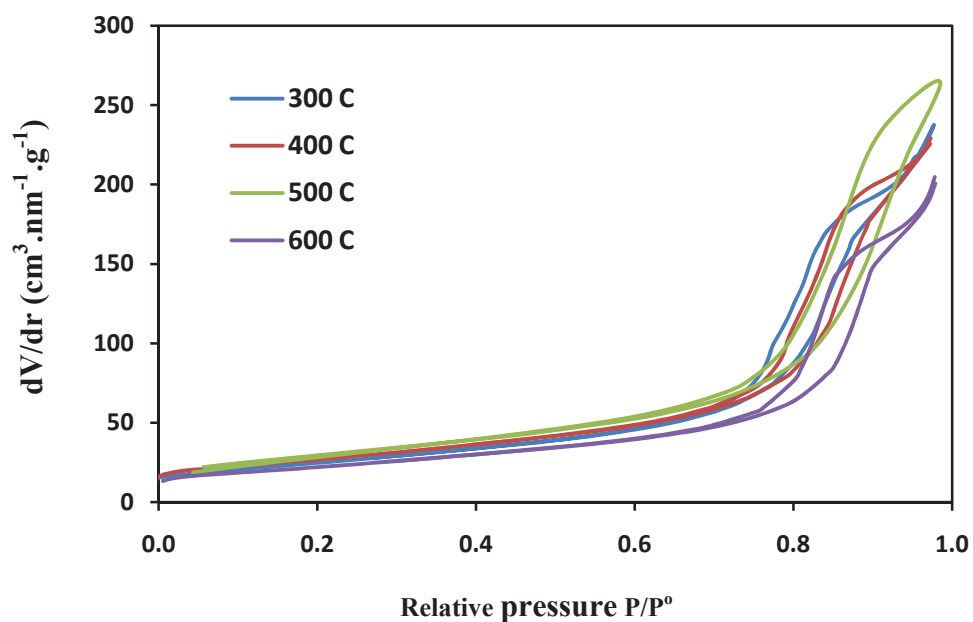
**Table 5.5** Physical properties of TiO<sub>2</sub> prepared by ST with different calcined temperature

Temperature (°C)	d <sub>XRD</sub> <sup>a</sup> (nm)	Relative <sup>b</sup> crystallinity	S <sub>BET</sub> <sup>c</sup> (m <sup>2</sup> /g)	Pore <sup>c</sup> diameter (nm)	Pore <sup>c</sup> volume (cm <sup>3</sup> /g)
300	14.1	1.00	79.8	6.7	0.3255
400	14.2	0.99	87.6	7.8	0.3632
500	14.0	1.05	100.1	9.4	0.4027
600	24.2	1.52	62.2	16.0	0.2877

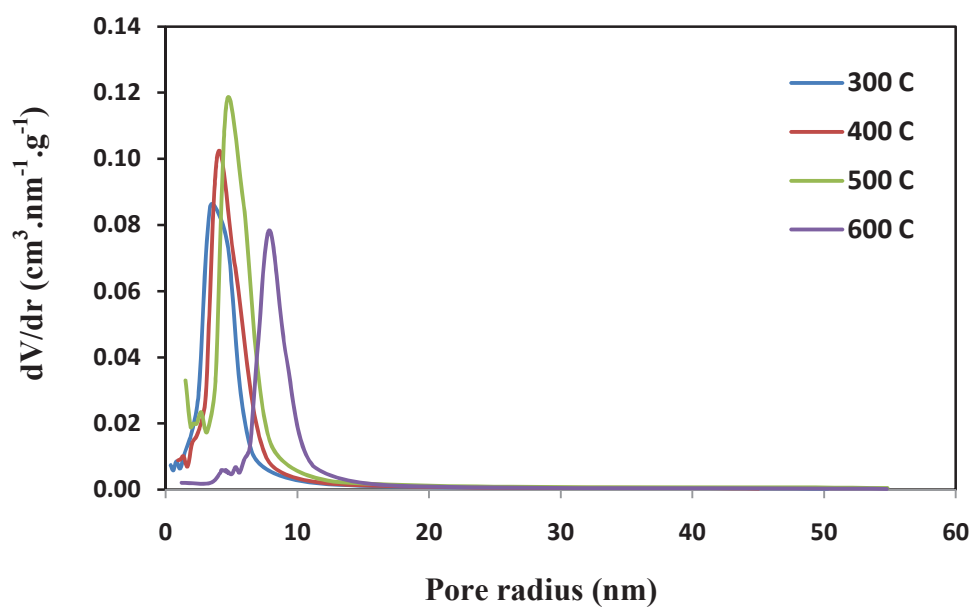
a) Base on XRD line broadening

b) Comparison of height main peak of anatase by using 300 °C of calcined temperature as reference

c) N<sub>2</sub> physisorption analysis

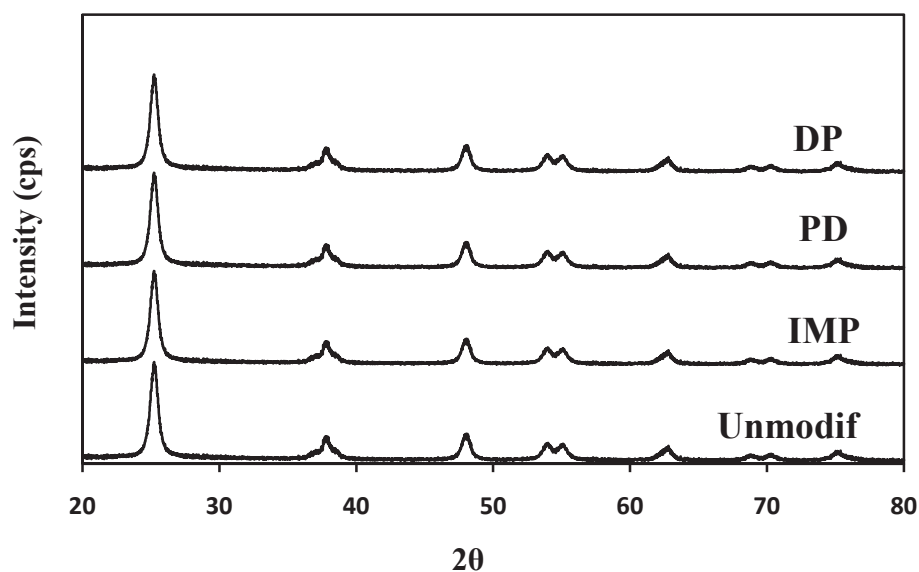


**Figure 5.20** N<sub>2</sub> adsorption/desorption isotherms of TiO<sub>2</sub> prepared by ST in HT with different calcined temperatures



**Figure 5.21** Pore size distribution of TiO<sub>2</sub> prepared by ST in HT with different calcined temperatures

### 5.1.6 Effect of Au modified TiO<sub>2</sub> method



**Figure 5.22** XRD patterns of Au modified TiO<sub>2</sub> by PD, DP and IMP

From XRD patterns of Au modified TiO<sub>2</sub> based photocatalyst by photodeposition (PD), impregnation (IMP), and doping (DP), when TiO<sub>2</sub> based photocatalyst prepared by ST in BD at 300 °C show in Figure 5.22, the diffractograms mainly exhibit the crystalline structure of the anatase phase, which is similar to that of the unmodified TiO<sub>2</sub>. From the XRD results, the indistinguishable presence of the diffraction peak of Au at 44.0 [68] indicates that the loaded Au particles are in very high dispersion. As the minimum detection limit of the XRD technique for any crystalline materials is around 5 nm, it is inferred that the crystallite sizes of the Au particles may be approximately equal to or below this value. In addition, the loaded Au content was relatively low [49]. Moreover, all the methods do not change physical properties from unmodified TiO<sub>2</sub> such as crystallite size, BET surface area and porosity as shown in Table 5.6 and Figure 5.23 and 5.24. The actual metal loadings of the Au modified TiO<sub>2</sub>

photocatalysts obtained from ICP were not significantly different from the nominal Au loadings for DP and IMP method, while PD differently provide between actual and nominal Au loading as shown in Table 5.6. This implies that the IMP and DP methods used for Au modified TiO<sub>2</sub> is reliably effective in controlling any desired cocatalyst loading than PD method. From results of H<sub>2</sub> chemisorption in Table 5.6 is found that active site of Au particle modified TiO<sub>2</sub> by PD and DP are clearly higher than IMP because of high dispersion of Au particles.

**Table 5.6** Physical properties of Au modified TiO<sub>2</sub> by IMP, PD and DP

<b>Au modified method</b>	<b>Actual Au loading<sup>a</sup> (wt.%)</b>	<b>d<sub>XRD</sub><sup>b</sup> (nm)</b>	<b>S<sub>BET</sub><sup>c</sup> (m<sup>2</sup>/g)</b>	<b>Pore<sup>c</sup> diameter (nm)</b>	<b>E<sub>g</sub><sup>d</sup> (eV)</b>	<b>H<sub>2</sub> Chemisorption<sup>e</sup> (μmol/g)</b>	<b>Au Dispersion<sup>e</sup> (%)</b>
<b>Unmodified</b>	-	11.8	116.9	11.8	3.26	n.d.	-
<b>PD</b>	0.26	11.7	101.2	11.3	3.18	12.1	36.67
<b>IMP</b>	0.25	11.7	112.5	12.2	3.10	7.9	23.94
<b>DP</b>	0.26	12.1	115.2	12.1	3.10	10.8	32.73

n.d. = not detected

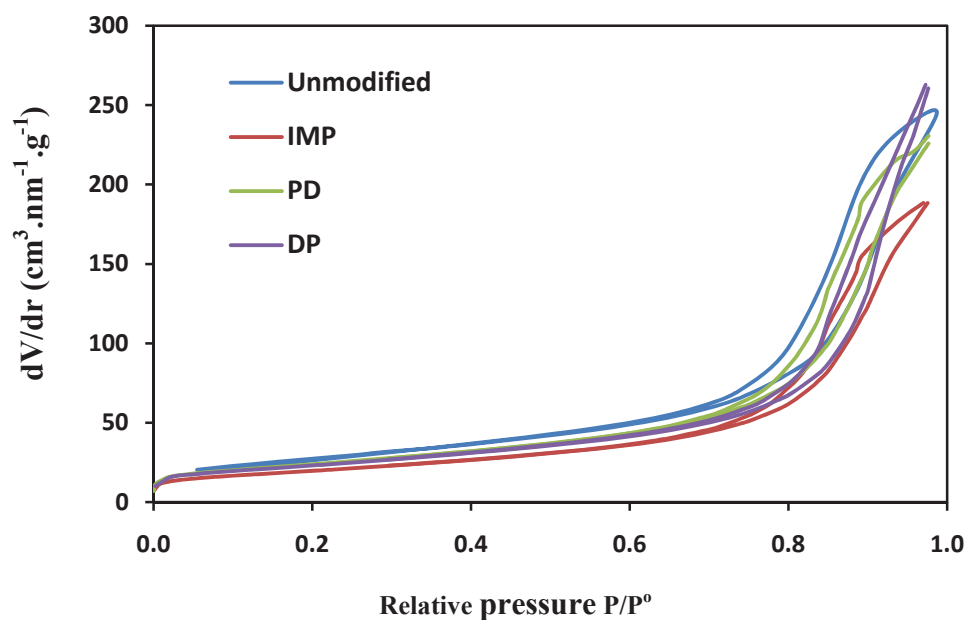
a) ICP analysis (Nominal Au loading : 1.00, 0.26 and 0.26 wt.% of PD, DP and IMP, respectively)

b) XRD analysis

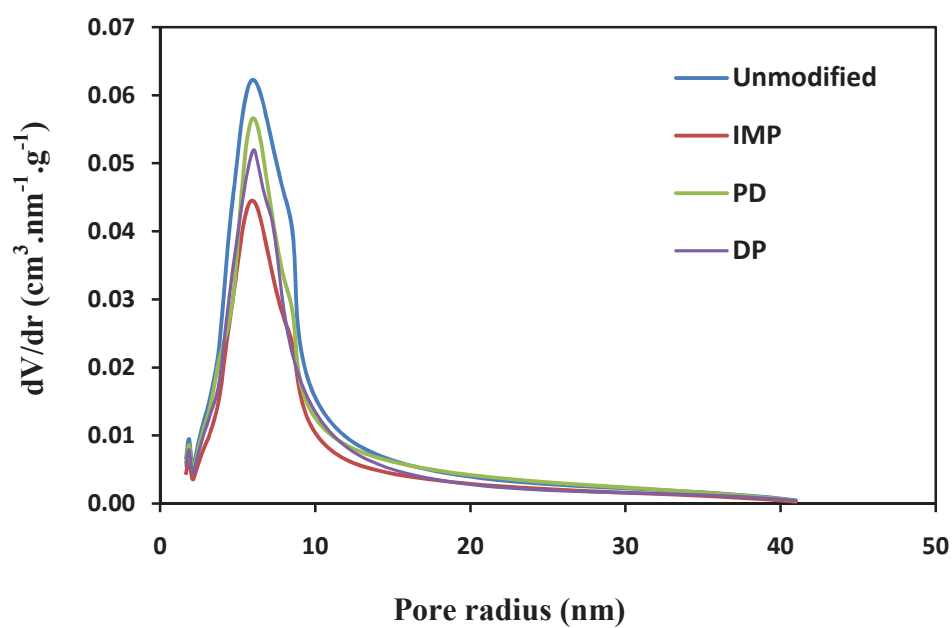
c) N<sub>2</sub> physisorption analysis

d) UV-visible spectroscopy analysis

e) H<sub>2</sub> chemisorption analysis



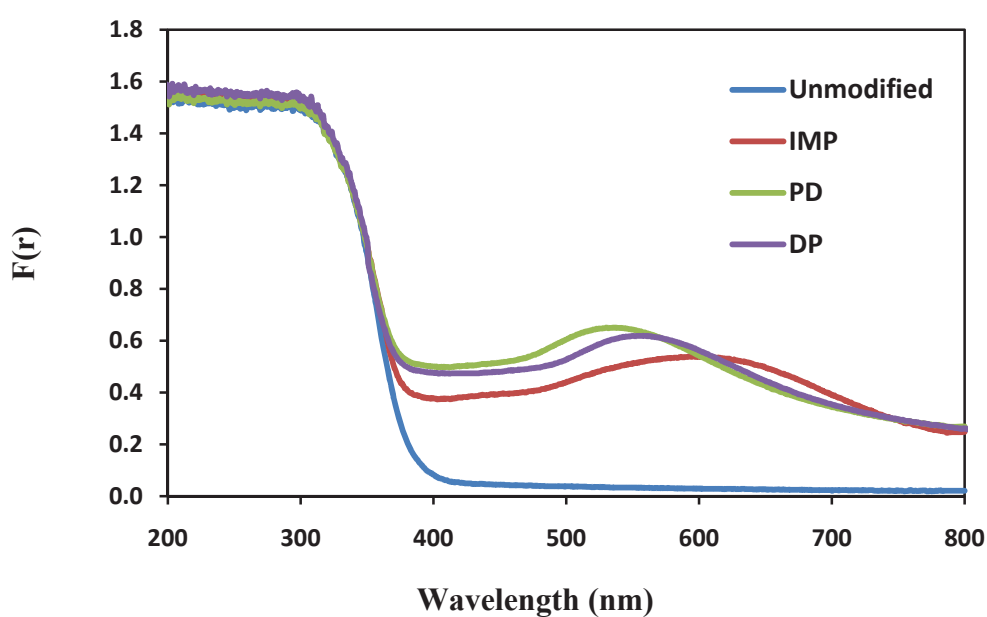
**Figure 5.23**  $N_2$  adsorption/desorption isotherms of Au modified  $TiO_2$  by IMP, PD and DP



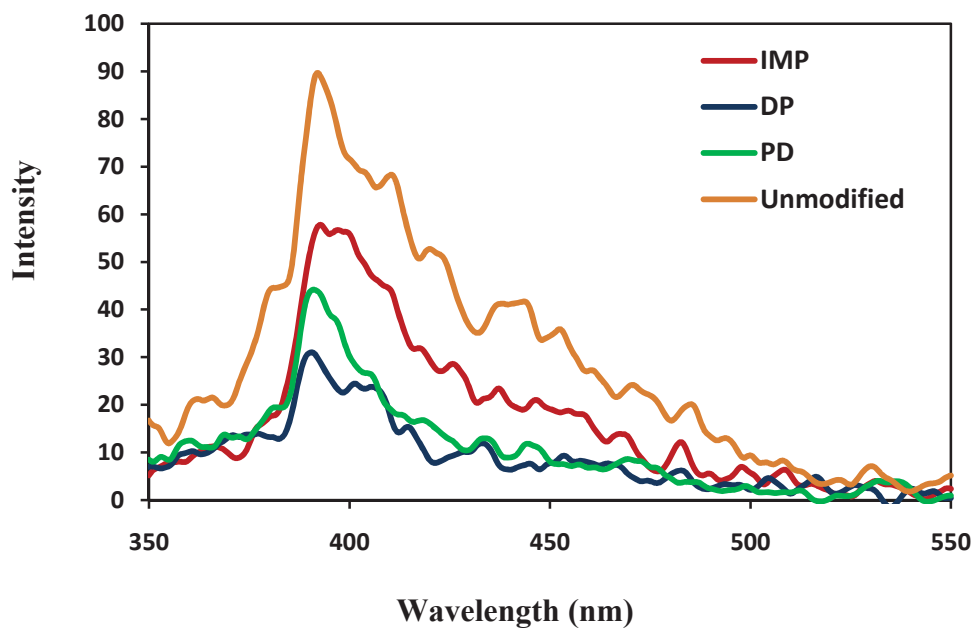
**Figure 5.24** Pore size distribution of Au modified  $TiO_2$  by IMP, PD and DP

The light-harvesting ability of all the Au modified methods were determined from their UV-vis DRS in the range from 200 to 800 nm. The UV part of the spectra was very similar for all the samples, presenting the characteristic absorption threshold around 400 nm, i.e. very close to that of pure anatase. Band gap energies were found that Au modified TiO<sub>2</sub> with these methods hardly change main band gap energy when comparing to unmodified TiO<sub>2</sub> (see Table 5.6). However, all the Au modified methods also show that the presence of Au greatly contributes to the increase in the light-harvesting ability within the visible region ( $\lambda > 400$  nm), which it significantly enhanced the visible light-harvesting ability up to a wavelength of 800 nm, as shown in Figure 5.25. In the visible part of the spectra the surface plasmon band of metallic gold could be observed for the Au modified TiO<sub>2</sub> by PD, DP and IMP around 540, 550 and 600 nm, respectively. For gold nanoparticles a strong dependence between particle size and plasmon bandwidth and position has been reported [68]. The bandwidth of the surface plasmon absorption (SPA) grows upon increasing the mean particle size for gold deposits larger than 25 nm [68]. Thus, the difference of bandwidths in the samples prepared with PD,IMP and DP would confirm the larger size of the gold deposits obtained IMP. The position of the absorption maximum of the SPA also depends on the particle size, with red-shifts when increasing the particle diameters for gold particles larger than 25 nm and both red- and blue-shifts for smaller metal particles [68]. For this reason, considering that in our case the difference in the position of the SPA between the PD and DP is just about 10 nm, the position of the SPA does not ensure any valid indication about the size of the deposits. The PL emission spectra can be used to disclose the efficiency of charge carrier trapping, immigration, transfer and to understand the fate of photo-induced electrons and holes in semiconductor [80]. It is known that the PL spectrum is the result of the recombination of excited electrons and holes, the lower PL intensity may indicate the lower recombination rate of electrons-holes under light irradiation [80]. Figure 5.26 shows the PL spectra of Au modified TiO<sub>2</sub> photocatalyst. The PL intensities vary in the following order: DP > PD > IMP > Unmodified TiO<sub>2</sub>. This result can be concluded that an Au can reduce the recombination rate of photoinduced electrons and holes in Au modified TiO<sub>2</sub> and the recombination rate also depends Au modified method. Au

modified TiO<sub>2</sub> by is least recombination rate of charges, it may contribute decreasing recombination in both bulk and surface photocatalyst. In addition, this also shows that the PL curve does not shifted to the right (the longer wavelength) in Au modified TiO<sub>2</sub> compared to unmodified TiO<sub>2</sub>. This result means that the band gap of TiO<sub>2</sub> anatase was not changed to low energy [21], which according to the result from UV-vis DRS.



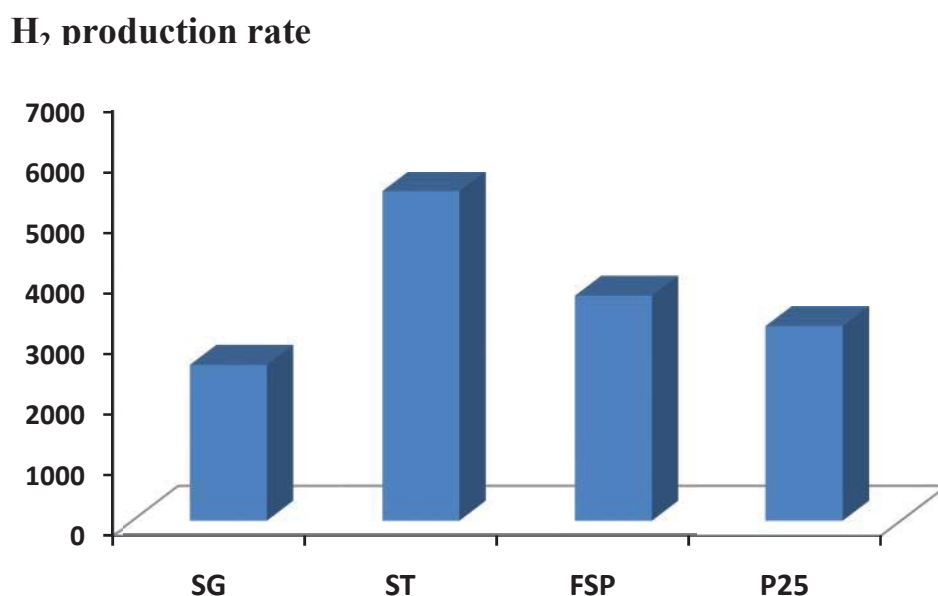
**Figure 5.25** UV-vis DRS of Au modified TiO<sub>2</sub> by IMP, PD and DP



**Figure 5.26** The PL emission spectra of Au modified TiO<sub>2</sub> by IMP, PD and DP

## 5.2 Photocatalytic H<sub>2</sub> production

### 5.2.1 Effect of TiO<sub>2</sub> preparation method



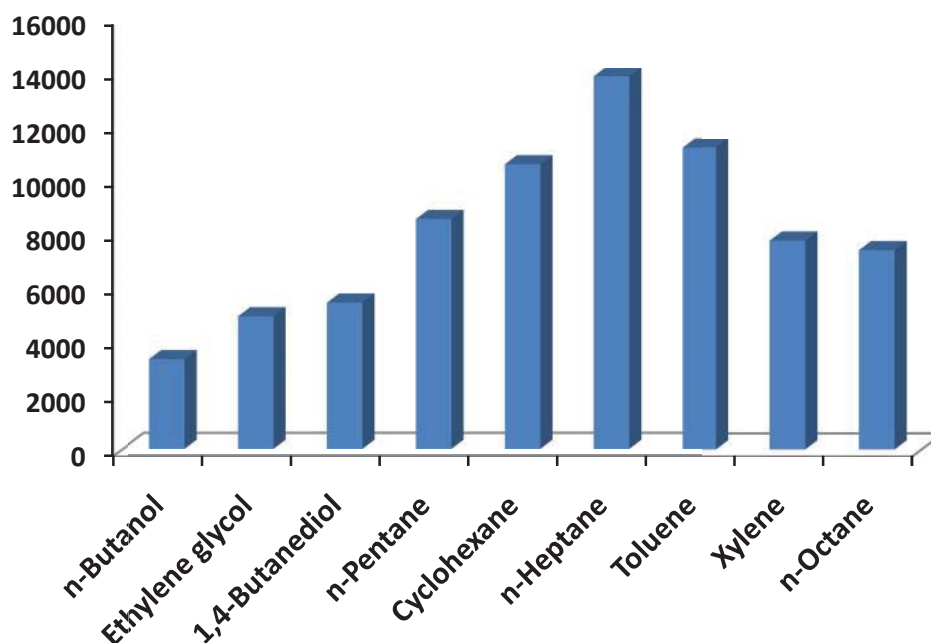
**Figure 5.27** Effect of preparation method of TiO<sub>2</sub> particles on photocatalytic H<sub>2</sub> production rate

The photocatalytic activity of TiO<sub>2</sub> particles prepared by SG, ST and FSP with comparing to P25 as commercial TiO<sub>2</sub> were examined by measurement of the photocatalytic H<sub>2</sub> production rate from aqueous formic acid solution with 0.26wt.% of Au loading by photodeposition under simulated solar light. As shown in Figure 5.12, the photocatalytic H<sub>2</sub> production rate of TiO<sub>2</sub> prepared by ST is highest in among of the studied methods because this method provided highest specific surfacarea and smallest nanocrystallite size of TiO<sub>2</sub>. It well known that high surface area and small crystallite

size promote active site and fast transference of  $e^-/h^+$  onto the surface of  $TiO_2$ . In addition, this method provided suitable pore size in mesoporous rang. The mesopore have been proved increasing of photocatalytic activity of photocatalysts. From the result of photocatalytic  $H_2$  production with different preparation method, it can said that the preparation method of  $TiO_2$  photocatalyst highly affected physical properties of  $TiO_2$  particles and their photocatalytic activity. So that, ST method was selected in preparation of  $TiO_2$  particles for photocatalytic  $H_2$  production and it was determined suitable condition for preparation of  $TiO_2$  with high photocatalytic activity.

### 5.2.2 Effect of solvent type in $TiO_2$ preparation by solvothermal

#### $H_2$ production rate



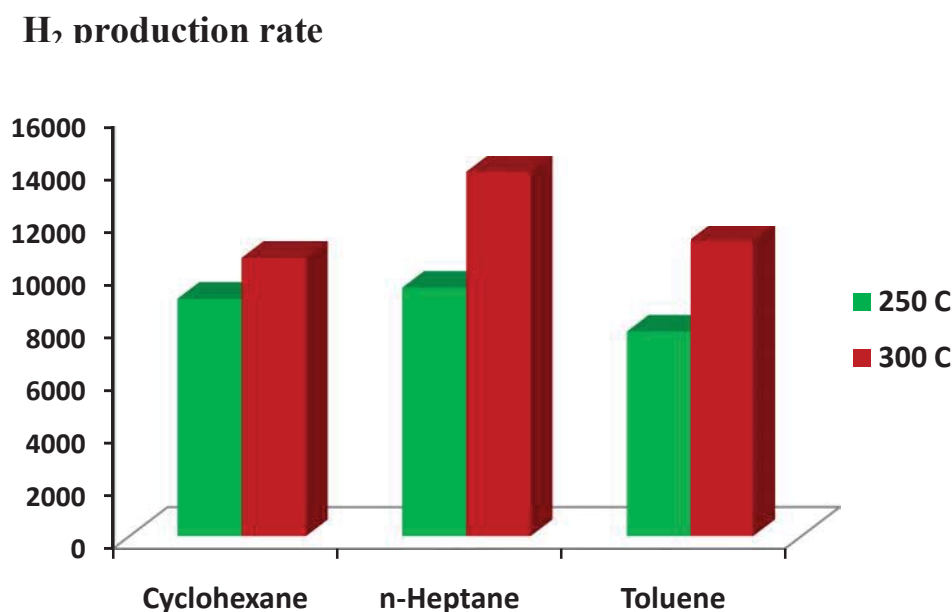
**Figure 5.28** Effect of solvent type of  $TiO_2$  preparation by ST on photocatalytic  $H_2$  production rate

Generally, solvent extremely affect physical and chemical properties of photocatalyst and their photocatalytic activity for photocatalyst preparation by solvothermal method [24], so that, the type of solvent were firstly varied in the TiO<sub>2</sub> prepared by this method. Figure 5.13 show the photocatalytic H<sub>2</sub> production rate of TiO<sub>2</sub> preparation by solvothermal method with using different solvents. Usually, photocatalytic H<sub>2</sub> production rate related specific surface area, high surface area provided high active size, hence, high photocatalytic activity. Although TiO<sub>2</sub> prepared in 1,4 butanediol provided highest surface area but provided low crystallinity, which crystallinity affect charge transference, hence, the photocatalytic H<sub>2</sub> production rate of them were lower than other studied solvent with lower specific surface area. On the other hand, TiO<sub>2</sub> prepared in heptane and toluene provided similar surface area, but heptane was higher H<sub>2</sub> production rate than toluene, because it was higher agglomeration of crystallite TiO<sub>2</sub> than in toluene. The agglomeration of TiO<sub>2</sub> crystals decrease recombination rate of e<sup>-</sup>/h<sup>+</sup> pair, increasing photocatalytic activity.

### 5.2.3 Effect of temperature in TiO<sub>2</sub> preparation by solvothermal

Figure 5.29 shows effect of solvothermal temperature in preparation of TiO<sub>2</sub> powders on photocatalytic H<sub>2</sub> production in aqueous formic acid solution with 0.26 wt.% of Au loading by photodeposition under simulated solar light. It can be seen that preparation at 300 °C is higher than 250 °C for all studied solvents because solvothermal temperature at 300 °C of TiO<sub>2</sub> preparation provide high crystallinity and consists of anatase crystals without contamination of amorphous phase in the TiO<sub>2</sub> particles even if smaller surface area and crystallite size. Although high surface area and small nanocrystallite size provide high active size and fast transference of charges to surface of photocatalyst, respectively. This indicates that crystallinity has effect to photocatalytic activity, it is well known that high crystallinity contributes easy mobility of charges in

the bulk photocatalyst while amorphous  $\text{TiO}_2$  does not active in photocatalytic reaction [5,14].



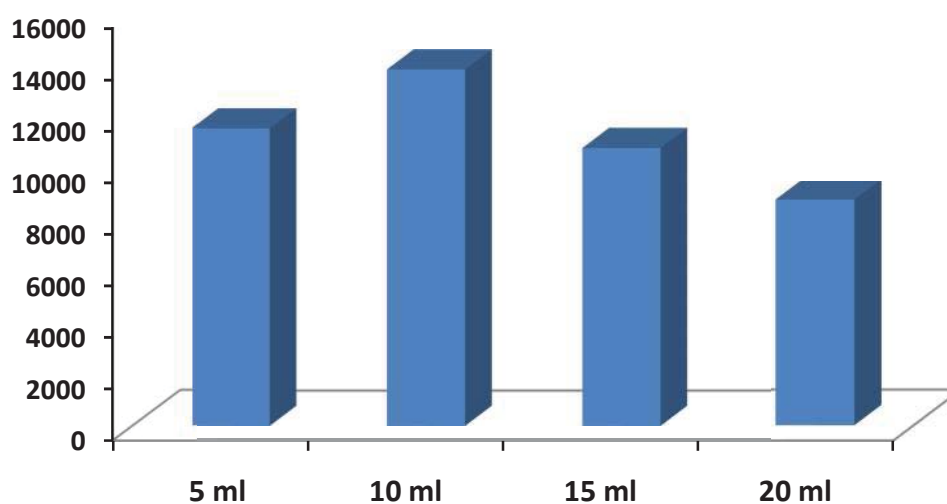
**Figure 5.29** Effect of temperature in  $\text{TiO}_2$  preparation by ST on photocatalytic  $\text{H}_2$  production rate

#### 5.2.4 Effect of Ti concentration in $\text{TiO}_2$ preparation by solvothermal

The photocatalytic  $\text{H}_2$  production was examined to studied the effect of Ti concentration in  $\text{TiO}_2$  preparation by solvothermal method. This result is shown in Figure 5.30. It was found that TIPT-to-solvent volume ration is 10/100 gave optimum concentration for providing  $\text{TiO}_2$  with highest  $\text{H}_2$  production rate. The  $\text{H}_2$  production rate increased with increasing TIPT until 10 ml of TIPT, after that the  $\text{H}_2$  production rate decreased with increasing TIPT. This result was explained that  $\text{TiO}_2$  particles preparation with 5 ml of TIPT hardly agglomerated although highest surface area. Generally, agglomeration of  $\text{TiO}_2$  particles contribute decreasing of charge recombination rate, resulting in increase photocatalytic activity. While the higher TIPT than 10 ml,  $\text{TiO}_2$

particles significantly agglomerated, resulting in decreased surface area. Therefore, photocatalytic H<sub>2</sub> production rate decreased when increasing TIPT.

### H<sub>2</sub> production rate

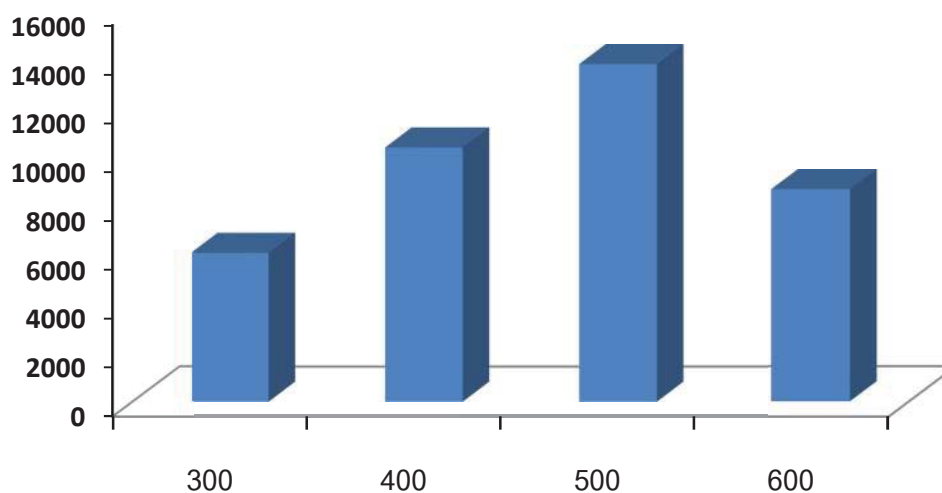


**Figure 5.30** Effect of TIPT concentration in TiO<sub>2</sub> preparation by ST on photocatalytic H<sub>2</sub> production rate

### 5.2.5 Effect of calcined temperature

The effect of calcine temperature of synthesized TiO<sub>2</sub> by solvothermal is shown in Figure 5.31. It was found that photocatalytic H<sub>2</sub> production rate increased with increasing temperature of calcination, after that the H<sub>2</sub> production rate decreased at 600 °C of calcined temperature. This result was explained that at lower calcined temperature at 500 °C provided low surface area because the TiO<sub>2</sub> particle contaminated impurity, while the higher temperature of calcination at 500 °C carried out significant sintering of TiO<sub>2</sub> particle to large particle size, resulting in decreased surface area of surface reaction even if high crystallinity. Therefore, photocatalytic H<sub>2</sub> production rate is highest at 500 °C of temperature of calcination.

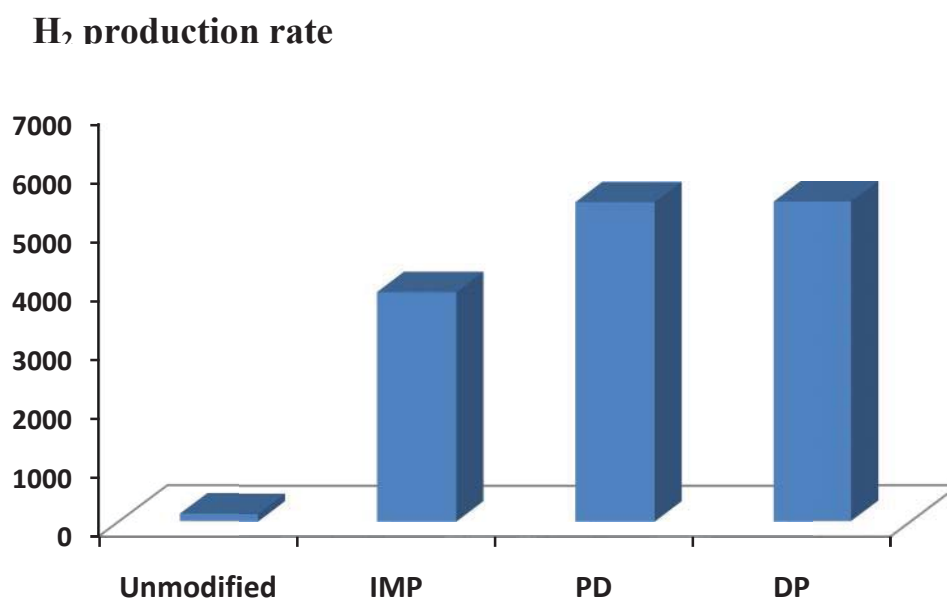
### H<sub>2</sub> production rate



**Figure 5.31** Effect of calcined temperature on photocatalytic H<sub>2</sub> production rate

#### 5.2.6 Effect of Au cocatalyst modified method

The photocatalytic H<sub>2</sub> production rate in Figure 5.32 is exhibited the effect of Au modified TiO<sub>2</sub> with photodeposition (PD), impregnation (IMP) and doping (DP) compared to unmodified TiO<sub>2</sub>. It was found that TiO<sub>2</sub> was modified by Au greatly enhanced photocatalytic activity. This result was explained the roles of Au seem to involve the attraction and trapping of photogenerated electrons, the reduction of protons and the formation and desorption of H<sub>2</sub> [65]. The H<sub>2</sub> production rate of DP and PD method exhibited higher than IMP because these method provided high absorption of visible light, small nanoparticle size of Au, high active sites of Au and low charges recombination rate, resulting photocatalytic activity of them are higher than IMP method [63,64]. However, DP and PD method show the same photocatalytic H<sub>2</sub> rate. Although the Au active sites of DP are smaller than PD, but charges recombination rate in DP is smaller than in PD. So that, the both method showed same high efficiency of cocatalyst modification for photocatalysis.



**Figure 5.32** Effect of Au modified method on photocatalytic H<sub>2</sub> production rate

## CHAPTER 6

### CONCLUSIONS AND RECOMMENDATION

The physical properties such as surface area, crystallinity and porosity of TiO<sub>2</sub> particles can be modified by using different preparation method or different condition. The balance of surface area, crystallinity, porosity and pore structure were found to be responsible for the activity of the photocatalytic H<sub>2</sub> production, these properties were obtained from selecting suitable preparation method and suitable condition. The suitable method is the solvothermal method with preparation condition of heptane as solvent, synthesized temperature of 300 °C, TIPT-to-heptane volume ratio of 10:100 and calcination temperature of 500 °C.

Due to the H<sub>2</sub> production results, the loaded Au particles can significantly increased the photocatalytic activity of TiO<sub>2</sub> under simulated solar light. Photodeposition and doping methods were found to be the suitable method for the TiO<sub>2</sub> modification with Au. The best Au modified TiO<sub>2</sub> exhibited the H<sub>2</sub> production rate of 13,786 μmol.h<sup>-1</sup>.g<sub>cat</sub><sup>-1</sup>.

The recommendations for further study were suggested as follows:

1. The Au modified TiO<sub>2</sub> should be developed to decreased band gap energy by using cation or anion doping and to enhanced oxidation reaction on photocatalyst surface by loading oxidation site such as RuO<sub>2</sub> or IrO<sub>2</sub>.
2. The optimal amount of Au loading should be investigated to enhanced the photocatalytic H<sub>2</sub> production activity of the TiO<sub>2</sub> based photocatalyst.

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## **APPENDIX**

## APPENDIX A

### CALCULATION FOR PHOTOCATALYST PREPARATION

**Table A.1** Chemical Properties

Chemicals	Molecular weight	Purity (wt.%)	Density (g/cm <sup>3</sup> )
TiO <sub>2</sub>	79.87	100	3.83
Au	196.97	100	-
TIPT	284.25	98	0.96
HAuCl <sub>4</sub> .3H <sub>2</sub> O	393.83	49 (Au Basis)	-

#### *A.1 Calculation of Au modified by incipient impregnation*

Preparation of Au modified by incipient impregnation method is shown as follows:

Reagent: Au  
Support: TiO<sub>2</sub>

**Example:** Calculation for the preparation of 0.26Au/TiO<sub>2</sub> photocatalyst with HAuCl<sub>4</sub>.3H<sub>2</sub>O as Au precursor

For 2 g of TiO<sub>2</sub> based photocatalyst

$$\text{Au required} = 2 \times (0.26/100) = 5.2 \times 10^{-3} \text{ g}$$

Thus, Au 5.2 x 10<sup>-3</sup> g was prepared from HAuCl<sub>4</sub>.3H<sub>2</sub>O

$$\text{Au metal} \quad 49 \text{ g} \quad \text{in} \quad \text{HAuCl}_4 \cdot 3\text{H}_2\text{O} \quad 100 \text{ g}$$

For 5.2 x 10<sup>-3</sup> g of Au metal

$$\text{HAuCl}_4 \cdot 3\text{H}_2\text{O} = 5.2 \times 10^{-3} \times (100/49) = 0.0106 \text{ g}$$

### ***A.2 Calculation of TiO<sub>2</sub> based photocatalyst prepared by flame spray pyrolysis***

0.3 M solution was used as precursor for TiO<sub>2</sub> preparation by flame spray pyrolysis is shown as follows:

**Example:** Calculation for the preparation of the TiO<sub>2</sub> photocatalysts, TIPT were used as precursor and diluted with xylene to a 0.3 M solution.

*Based on 0.3 M solution of Ti concentration will be as follows:*

*Basis 500 ml precursor solution 0.3 M:*

$$\text{mol Ti} = 500 \text{ ml} \times \frac{0.3 \text{ mol Ti}}{1000 \text{ ml}} = 0.15 \text{ mol Ti}$$

$$\text{TIPT} = 0.15 \text{ mol Ti} \times \frac{1 \text{ mol TIPT}}{1 \text{ mol Ti}} \times \frac{284.25 \text{ g TIPT}}{1 \text{ mol TIPT}} \times \frac{1 \text{ ml TIPT}}{0.96 \text{ g TIPT}} = 44.41 \text{ ml TIPT}$$

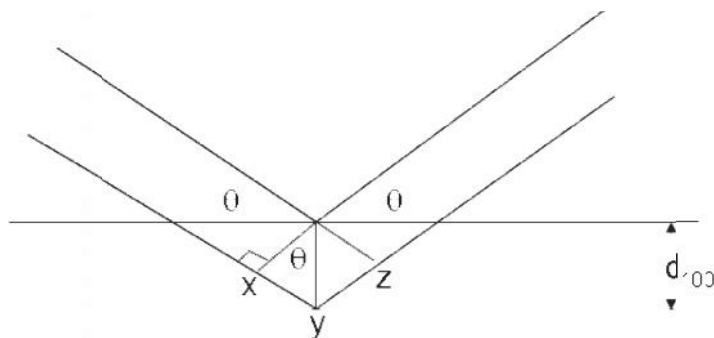
## **APPENDIX B**

## APPENDIX B

### CALCULATION OF THE CRYSTALLITE SIZE

#### *Calculation of the crystallite size by Debye-Scherrer equation*

The crystallite size was calculated from the half-height width of the diffraction peak of XRD pattern using the Debye-Scherrer equation.



**Figure B.1** Derivation of Bragg's Law for X-ray diffraction

$$xy = yz = d \sin \theta$$

Thus

$$xyz = 2d \sin \theta$$

But

$$xyz = n\lambda$$

Therefore

$$2d \sin \theta = n\lambda$$

*Bragg's Law*

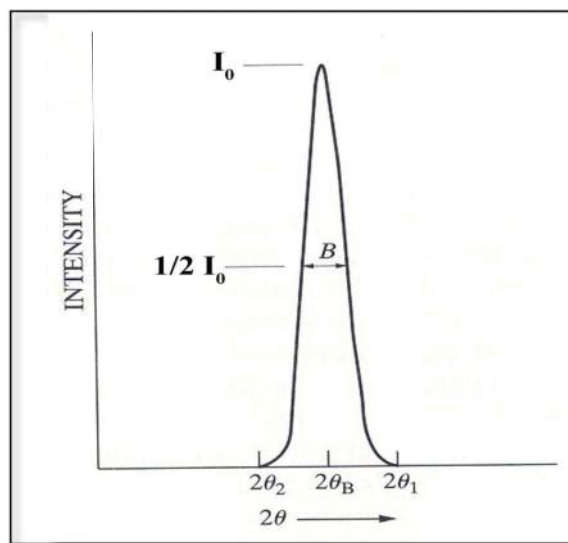
$$d = \frac{n\lambda}{2 \sin \theta}$$

The Bragg's Law was derived to B.1

From Scherrer equation:

$$D = \frac{K\lambda}{\beta \cos \theta}$$

Where  $D$  = Crystallite size,  $\text{\AA}$   
 $K$  = Crystallite-shape factor = 0.89  
 $\lambda$  = X-ray wavelength,  $1.5418 \text{ \AA}$  for  $\text{CuK}\alpha$   
 $\theta$  = Observed peak angle, degree  
 $\beta$  = Full-Width at Half-Maximum (FWHM), radian



**Figure B.2** The determining of the FWHM value of XRD line broadening

## **APPENDIX C**

## APPENDIX C

### CALCULATION FOR TOTAL H<sub>2</sub> CHEMISORPTION AND DISPERSION

Calculation of the total H<sub>2</sub> chemisorption and metal dispersion of the catalyst, a stoichiometry of H<sub>2</sub> : Au = 1 : 2, is assumed. The calculation procedure is as follows:

Let the weight of photocatalyst used	=	W	g
Let the wt% of Au in photocatalyst used	=	X	g
Integral area of H <sub>2</sub> peak after adsorption	=	A	unit
Integral area of 100 $\mu$ l of standard H <sub>2</sub> peak	=	B	unit
Amounts of H <sub>2</sub> adsorbed on photocatalyst	=	B-A	unit
Concentration of Au	=	0.26	wt. %
Volume of H <sub>2</sub> adsorbed on photocatalyst	=	100 $\times$ [(B-A)/B]	$\mu$ l
Volume of 1 $\mu$ mole of H <sub>2</sub> at 30 $^{\circ}$ C	=	24.88	$\mu$ l
Mole of H <sub>2</sub> adsorbed on photocatalyst	=	[(B-A)/B] $\times$ [100/24.88]	$\mu$ mole
Total hydrogen chemisorption	=	[(B-A)/B] $\times$ [100/24.88] $\times$ [1/W]	$\mu$ mole /g <sub>catalyst</sub>
	=	N	$\mu$ mole /g <sub>catalyst</sub>

$$\% \text{Au dispersion} = \frac{\text{The amount of Au equivalent to H}_2 \text{ adsorption}}{\text{Total amount of Au loading}}$$

$$\begin{aligned} \text{Molecular weight of Au} &= 196.97 \text{ g.mol}^{-1} \\ \text{Metal dispersion (\%)} &= \frac{2 \times N \times 10^{-6} \times 100}{(X \times W) / 196.97} \\ &= \frac{(3.94 \times 10^{-2}) N}{X \times W} \end{aligned}$$

## **APPENDIX D**

## APPENDIX D

### CALCULATION OF PHOTOCATALYTIC H<sub>2</sub> PRODUCTION RATE

The photocatalytic performance was evaluated in terms of photocatalytic H<sub>2</sub> production rate.

Photocatalytic H<sub>2</sub> production rate was calculated as follows:

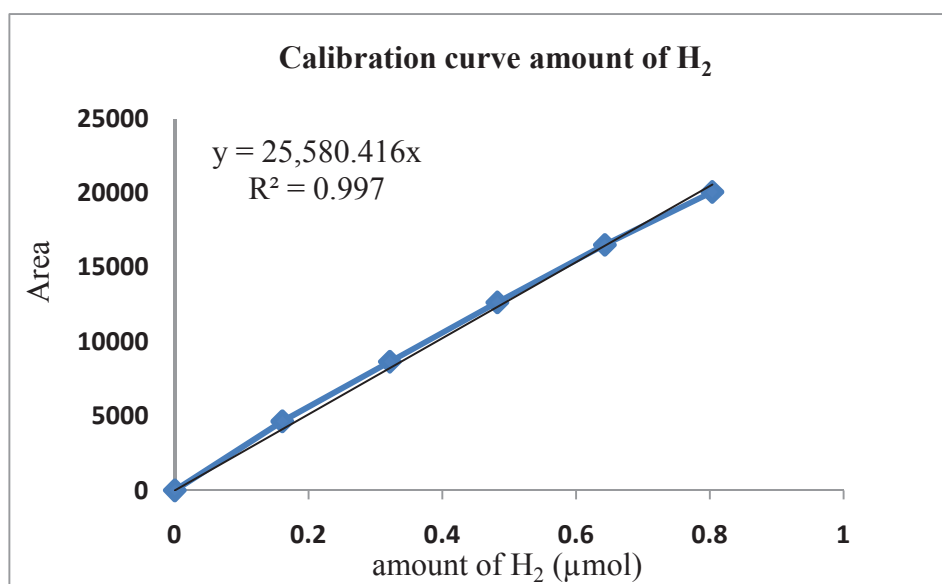
Let the weight of photocatalyst used =  $W$  g  
 Flow rate of Ar carrier = 30 ml/min  
 Volume of sample gas = 5 ml  
 Amount of H<sub>2</sub> was determined from calibration curve in figure D.1 =  $A$   $\mu\text{mol}$

Which area of H<sub>2</sub> obtained from computer program based plot on TCD (GC-14B).

$\therefore$  H<sub>2</sub> production rate ( $\mu\text{mol} / \text{h} \cdot \text{g}$  of catalyst )

$$= \frac{A \mu\text{mol}}{W \text{ g}_{\text{catalyst}}} \times \frac{30 \text{ ml} \cdot \text{min}^{-1}}{5 \text{ ml}} \times \frac{60 \text{ min}}{1 \text{ h}}$$

$$= \frac{360 \times A}{W} \mu\text{mol H}_2 \cdot \text{h}^{-1} \cdot \text{g}_{\text{catalyst}}^{-1}$$



**Figure D.1** Calibration curve of amount of H<sub>2</sub>

## **APPENDIX E**

## **APPENDIX E**

### **INTERNATIONAL PROCEEDING**

Karnanpus Dangsakol and Tarawipa Puangpetch

“Preparation method and characterization of Au modified TiO<sub>2</sub> for photocatalytic H<sub>2</sub> production with simulated solar energy”, Paccon 2012, Pure and Applied Chemistry International Conference, Thailand, 11-13 Jan, 2012 (poster presentation)

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Special Interest Nanoparticle /Heterogeneous Catalysis/Renewable Energy